

Banner appropriate to article type will appear here in typeset article

Exploring the nexus among roughness function, apparent slip velocity and upscaling coefficients for turbulence over porous/textured walls

Essam Nabil Ahmed^{1†} and Alessandro Bottaro¹

¹DICCA, Università degli Studi di Genova, via Montallegro 1, 16145 Genova, Italy

(Received xx; revised xx; accepted xx)

The interaction between a turbulent flow and a porous boundary is analyzed with focus on the sensitivity of the roughness function, ΔU^+ , to the upscaled coefficients characterizing the wall. The study is aimed at (i) demonstrating that imposing *effective* velocity boundary conditions at a *virtual* plane boundary, next to the physical one, can efficiently simplify the direct numerical simulations (DNSs); and (ii) pursuing correlations to estimate ΔU^+ *a priori*, once the upscaled coefficients are calculated. The homogenization approach employed incorporates near-interface advection via an *Oseen*-like linearization, and the macroscopic coefficients thus depend on both the micro-structural details of the wall and a slip-velocity-based Reynolds number, Re_{slip} . A set of homogenization-simplified DNSs is run to study the channel flow over transversely isotropic porous beds, testing values of the grains' pitch within $0 < \ell^+ < 40$. Reduction of the skin-friction drag is attainable exclusively over streamwise-aligned inclusions for ℓ^+ values up to 20–30. The drag increase over spanwise-aligned inclusions (or streamwise-aligned ones at large ℓ^+) is accompanied by enhanced turbulence levels, including intensified sweep and ejection events. The r.m.s. fluctuations of the transpiration velocity at the virtual plane, \tilde{V}_{rms} , is the key control parameter of ΔU^+ ; our analysis shows that, provided $\tilde{V}_{rms} \lesssim 0.25$, then \tilde{V}_{rms} is strongly correlated to a single macroscopic quantity, Ψ , which comprises the Navier-slip and interface/intrinsic permeability coefficients. Fitting relationships for ΔU^+ are proposed, and their applicability is confirmed against reference results for the turbulent flow over impermeable walls roughened with three-dimensional protrusions or different geometries of riblets.

Key words: To be chosen during online submission.

1. Introduction

Turbulent channel flows are characterized by substantially large skin-friction drag, compared to laminar ones, and this can have severe consequences on the performance of fluid transport systems, in terms of efficiency, running costs, and the reduction of emissions. There is a vast literature on turbulence in smooth channels (Kim *et al.* 1987; Mansour *et al.* 1988; Bernard *et al.* 1993; Jeong *et al.* 1997; Jiménez & Pinelli 1999; Vreman & Kuerten 2014), which has focused, for instance, on the behaviors of the primary turbulent fluctuations and the

† Email address for correspondence: essameldin.abdo@edu.unige.it

35 higher-order statistics, on the role of *ejection* and *sweep* events in the generation of Reynolds
 36 stresses, on nonlinear recurrent patterns, or on the autonomous regeneration cycle responsible
 37 for maintaining near-wall turbulence. Since the seminal work by [Nikuradse \(1933\)](#), the study
 38 of turbulent flow in channels delimited by rough boundaries has become a major focus of
 39 research, whether the goal is (i) to explore how given surface topographies can alter the near-
 40 wall turbulence and the skin-friction drag ([Orlandi *et al.* 2006](#); [Orlandi & Leonardi 2006](#),
 41 [2008](#); [Wang *et al.* 2021](#); [Monti *et al.* 2022](#); [Hao & García-Mayoral 2024](#)), (ii) to propose
 42 and test simplified models for numerical analysis ([Bottaro 2019](#); [Lācis *et al.* 2020](#); [Ahmed
 43 *et al.* 2022b](#)) or even predictive correlations ([Forooghi *et al.* 2017](#); [Flack *et al.* 2020](#)), or (iii)
 44 to optimize and assess the feasibility of wall-based energy-saving control strategies of either
 45 active ([Antonia *et al.* 1995](#); [Kang & Choi 2000](#); [Choi 2002](#); [Wise & Ricco 2014](#); [Cheng
 46 *et al.* 2021](#)) or passive nature ([Walsh & Lindemann 1984](#); [Bechert *et al.* 1997](#); [Rastegari &
 47 Akhavan 2015](#); [Rosti *et al.* 2018](#); [Endrikat *et al.* 2021b](#)). This introductory section centers
 48 around these important aspects.

49 Passive drag reduction techniques (i.e., micro-textured surfaces, permeable substrates, etc.
 50 able, with no energy input, to favorably manipulate the turbulent boundary layer with a
 51 view to reducing the turbulent skin-friction drag compared to the smooth surface case) have
 52 been the subject of intense research activities. Properly designed superhydrophobic surfaces
 53 (SHS) and liquid-infused surfaces (LIS), permitting large effective slip thanks to air (or liquid
 54 lubricant, respectively) being trapped within grooves/cavities/micro-grates formed on them,
 55 can yield substantial drag reduction in turbulent channel flows ([Park *et al.* 2013](#); [Rastegari
 56 & Akhavan 2015](#); [Fu *et al.* 2017](#); [Chang *et al.* 2019](#)). Riblets (longitudinal surface grooves)
 57 have proved to mitigate the velocity fluctuations near the wall, resulting in a more uniform
 58 flow field ([Bechert & Bartenwerfer 1989](#)). The skin-friction drag over surfaces altered with
 59 riblets is crucially sensitive to their geometry and to the Reynolds number of the flow in their
 60 vicinity (characterized, for instance, by the lateral spacing of riblets measured in wall units,
 61 ℓ^+) as found by many investigators ([Walsh & Lindemann 1984](#); [Bechert *et al.* 1997](#); [El-Samni
 62 *et al.* 2007](#); [Gatti *et al.* 2020](#); [Endrikat *et al.* 2021a,b](#); [von Deyn *et al.* 2022](#)). For example,
 63 the experiments by [Bechert *et al.* \(1997\)](#) on different configurations of riblets revealed that
 64 an optimized drag reduction of almost 10% can be attained, in particular with longitudinal
 65 blade ribs having depth and thickness equal to, respectively, 0.5 and 0.02 times the lateral rib
 66 spacing and with $\ell^+ \approx 17$. It should be noted that drag reduction ceases when ℓ^+ exceeds a
 67 value of about 30, and this is associated with the occurrence of inertial-flow mechanisms such
 68 as a Kelvin–Helmholtz instability ([García-Mayoral & Jimenez 2011](#); [Endrikat *et al.* 2021a](#)).
 69 Manipulating the turbulent boundary layer and achieving skin-friction reduction by means
 70 of properly engineered permeable substrates have recently caught the attention of many
 71 researchers. The porous medium permeability coefficients ($\hat{\mathcal{K}}_{ij}$) and the Navier slip lengths
 72 ($\hat{\lambda}_i$) are the main parameters whose role has been examined in a number of investigations, with
 73 different micro-structures of the substrate, sizes of the solid inclusions, porosities (θ), and
 74 flow conditions. Throughout this paper, \hat{x} , \hat{y} and \hat{z} refer to, respectively, the streamwise, wall-
 75 normal and spanwise directions. Among the configurations studied, transversely isotropic
 76 porous beds of streamwise-preferential permeability $\hat{\mathcal{K}}_{xx} \gg \hat{\mathcal{K}}_{yy} = \hat{\mathcal{K}}_{zz}$, for instance those
 77 constructed with cylindrical inclusions elongated in the direction of the mean flow, are
 78 repeatedly reported to potentially reduce drag in turbulent channel flows; the underpinning
 79 of their function, analogous to that of riblets, has been explained by [Abderrahaman-
 80 Elena & García-Mayoral \(2017\)](#), [Gómez-de-Segura *et al.* \(2018a\)](#), [Gómez-de-Segura &
 81 García-Mayoral \(2019\)](#), and [Chavarin *et al.* \(2021\)](#). These authors have found that, at
 82 relatively large values of the wall-normal permeability, Kelvin-Helmholtz-like rollers are
 83 generated near the porous/free-fluid interface, and this adversely affects the drag-reducing

84 mechanism. Streamwise-preferential porous substrates characterized by relatively large
 85 $\sqrt{\mathcal{K}_{yy}^+}$ (considerably beyond the threshold identified by Gómez-de-Segura & García-Mayoral
 86 (2019) for the emergence of Kelvin–Helmholtz vortices) were considered, among other
 87 configurations, in the scale-resolving direct numerical simulations by Khorasani *et al.* (2024)
 88 and the experiments by Vijay & Luhar (2024), and drag increase was confirmed. For a
 89 complete picture, it is also useful to cite the experiments by Morimoto *et al.* (2024) where
 90 drag either remained unchanged or was found to increase (with respect to smooth wall) for the
 91 case of streamwise-preferential permeable beds under conditions that were expected, on the
 92 basis of the numerical findings in Gómez-de-Segura & García-Mayoral (2019), to yield drag
 93 reduction instead. Morimoto *et al.* (2024) commented that it is difficult in practice (unlike in
 94 numerical work) to maintain the large uniform porosity and streamwise permeability when
 95 the substrate/channel interface is approached, and this adversely affects slippage. Several
 96 other studies of turbulence over porous substrates were conducted. Among the most relevant
 97 ones, we cite those conducted by Suga’s group (Suga *et al.* 2013, 2018; Suga 2016; Kuwata
 98 & Suga 2017), and those by Breugem *et al.* (2006), Manes *et al.* (2011), Rosti *et al.* (2015,
 99 2018), Wang *et al.* (2021, 2022), Esteban *et al.* (2022), and Hao & García-Mayoral (2024).

100 Investigating how the microscale features of the surface (e.g. roughness, porosity, superhy-
 101 drophobicity, etc.) can alter the characteristics of the turbulent motion above it, and thus skin-
 102 friction drag or heat/mass transfer effectiveness, is important in several applications for both
 103 predictive and optimization purposes. The numerical complexity and the high computational
 104 cost associated with resolving turbulent fields near and across surface micro-details represent
 105 a challenge, because of the large variety of surface topographies encountered in practice, the
 106 computational costs required to carry out well-resolved direct numerical simulation (DNS) or
 107 large eddy simulations of the motion, and the uncertainties/errors related with the numerical
 108 representation of the rough surface or of the grain shape and distributions for the case of
 109 a porous bed. Despite the recent computational advances which have permitted numerical
 110 investigations with unprecedented levels of accuracy (Chung *et al.* 2021), the aforementioned
 111 factors represent a major hurdle when optimization of the surface is the ultimate goal. In this
 112 respect, characterizing a surfaces by key parameters available *a priori* and exhibiting a strong
 113 relation with the roughness function, for example, can be very beneficial. However, this is a
 114 complex undertaking, and the quantities widely investigated throughout the literature are, in
 115 principle, available only *a posteriori* (i.e., after conducting the numerical/experimental study
 116 of the turbulent flow over the surface) and, hence, of limited use for prediction purposes.
 117 For example, we mention here (i) the equivalent sand-grain size, k_s , first introduced by
 118 Schlichting (1937) and later used as a classifier for rough surfaces in a large body of studies
 119 (refer to the limitations and drawbacks highlighted by Jiménez (2004) and Abderrahaman-
 120 Elena *et al.* (2019)); and (ii) the virtual origins of mean flow and turbulence (Luchini *et al.*
 121 1991; Jiménez 1994; Luchini 1996), with successive efforts devoted, in recent years, to the
 122 exploration of the statistical quantities whose near-wall behavior defines the virtual origin
 123 of turbulence (Gómez-de-Segura *et al.* 2018b; Abderrahaman-Elena *et al.* 2019; Bernardini
 124 *et al.* 2021; Ibrahim *et al.* 2021; Khorasani *et al.* 2022; Wong *et al.* 2024). On the positive
 125 side, predictive models based on the aforementioned concepts, albeit not yet generalized,
 126 are beginning to emerge (Flack & Schultz 2010; Yang & Meneveau 2016; Yang *et al.* 2016;
 127 Foroughi *et al.* 2017; Flack *et al.* 2020; Khorasani *et al.* 2022). It is also worth referring
 128 to the recent work on machine-learning-based predictive methods by, for example, Jouybari
 129 *et al.* (2021), Lee *et al.* (2022), Yang *et al.* (2023, 2024), and Shi *et al.* (2024).

130 The development of accurate macroscopic models for the fluid-wall interaction has become
 131 a very active field of research in the last decade or so. These are viable tools capable
 132 of simplifying the numerical analysis while maintaining an acceptable level of accuracy.
 133 The asymptotic, multiscale homogenization theory (Babuška 1976; Mei & Vernescu 2010)

134 is a theoretical framework through which the rapidly varying properties characterizing a
135 heterogeneous surface (irregular, rough, lubricant-infused, or porous, *inter alia*) can be
136 replaced by homogeneous upscaled parameters such as the Navier's slip lengths or the
137 interface permeability coefficients (Jiménez Bolaños & Vernescu 2017; Lācis *et al.* 2017;
138 Bottaro 2019; Zampogna *et al.* 2019a; Lācis *et al.* 2020). The latter are necessary for the
139 formulation of *effective* boundary conditions, free of empirical coefficients, to be imposed at
140 a fictitious plane interface next to the physical textured boundary; the macroscale behavior
141 of the channel flow is then studied numerically, eschewing the numerical resolution of flow
142 details between/in close vicinity of the solid protrusions/grains and, consequently, alleviating
143 mesh requirements and computational costs. The validity of the asymptotic homogenization
144 approach is contingent on the presence of well-separated scales, for instance a microscopic
145 length scale ($\tilde{\ell}$) related to the surface texture and a macroscopic one ($\mathcal{L} \gg \tilde{\ell}$) related to the
146 large-scale flow structures in the channel, such that we are able to define the small parameter
147 $\epsilon = \tilde{\ell}/\mathcal{L} \ll 1$ and seek a solution of the problem up to the required order of accuracy in
148 terms of ϵ . Jiménez Bolaños & Vernescu (2017) provided a robust homogenization-based
149 method for the evaluation of the slip coefficient, contributing to the classical order-one slip
150 condition over a textured surface, first proposed by Navier (1823) on the basis of empirical
151 considerations. High-order effective boundary conditions were derived by Bottaro & Naqvi
152 (2020) and Ahmed *et al.* (2022a) for the flow over a rough surface and by Lācis *et al.* (2020),
153 Sudhakar *et al.* (2021), Naqvi & Bottaro (2021) and Ahmed *et al.* (2022b) for the flow over a
154 porous bed. Definitions of the three velocity components at the fictitious interface, valid up
155 to second-order in ϵ , are now available; this is crucial under turbulent flow conditions since
156 turbulent fluctuations along directions both tangent and normal to the fictitious interface
157 considerably affect the behavior of the turbulent boundary layer and, therefore, the skin-
158 friction drag (Orlandi *et al.* 2006; Orlandi & Leonardi 2006, 2008; Bottaro 2019; Lācis *et al.*
159 2020). The near-wall advection was incorporated into the analysis by means of an Oseen's
160 approximation in the studies by Buda (2021) and Ahmed & Bottaro (2024), and this permitted
161 to widen considerably the applicability range of the model.

162 The present work is aimed at investigating the hydrodynamic interaction between a
163 porous/rough boundary and a fluid under turbulent flow conditions, with the aid of a
164 homogenization framework. The main focus is on exploring the relationship between the
165 roughness function ΔU^+ (i.e., the shift in the intercept of the logarithmic velocity profile)
166 and the macroscopic coefficients (i.e., the Navier-slip coefficients and the interface/intrinsic
167 permeabilities) contributing to the effective boundary conditions at the wall. Throughout
168 the work, it is assumed that the roughness elements do not protrude significantly into the
169 free-fluid turbulent region, for outer layer similarity to hold (Townsend 1976). The study is
170 twofold. First, turbulent channel flows over permeable boundaries of different geometries are
171 considered, and high-order *effective* boundary conditions of the three velocity components,
172 defined at a *fictitious* plane boundary tangent to the grains, are formulated (Section 2),
173 validated (Section 3.1), and employed to simplify a set of direct numerical simulations
174 (Section 3.2); the mean velocity profiles are obtained and the main turbulence statistics near
175 the porous/free-fluid interface are analyzed to interpret the drag-reducing/increasing effects
176 of the porous patterns. Second, in order to estimate the roughness function *a priori*, without
177 the need for running direct numerical simulations, the available results are fitted to generate
178 an explicit expression linking ΔU^+ to the upscaled coefficients of interest (Section 3.3); the
179 generality of the fitting correlation(s) is confirmed via validation against results from the
180 literature for the turbulent flow over rough, impermeable walls (Section 3.4). A discussion
181 on the applicability range of the model is provided in Section 4, and general conclusions are
182 given in Section 5.

2. Problem statement and upscaling approach

2.1. Governing equations and domain decomposition

Let us consider the turbulent flow of a viscous, incompressible, Newtonian fluid in a channel delimited from one side (at $\hat{y} = 2H$) by a smooth, impermeable wall and from the other side (at $\hat{y} \leq 0$) by a permeable substrate constructed with spanwise-elongated (\hat{z} -aligned) solid inclusions, regularly arranged with given periodicity ℓ in the streamwise and wall-normal directions (\hat{x} and \hat{y} , respectively); refer to figure 1. The velocity components ($\hat{u}_1 = \hat{u}$, $\hat{u}_2 = \hat{v}$, $\hat{u}_3 = \hat{w}$) and the pressure \hat{p} are the dependent variables, to be evaluated over space ($\hat{x}_1 = \hat{x}$, $\hat{x}_2 = \hat{y}$, $\hat{x}_3 = \hat{z}$) and time \hat{t} . The conservation equations governing the flow can be expressed as follows:

$$\frac{\partial \hat{u}_i}{\partial \hat{x}_i} = 0, \quad \rho \left(\frac{\partial \hat{u}_i}{\partial \hat{t}} + \hat{u}_j \frac{\partial \hat{u}_i}{\partial \hat{x}_j} \right) = -\frac{\partial \hat{p}}{\partial \hat{x}_i} + \mu \frac{\partial^2 \hat{u}_i}{\partial \hat{x}_j^2}, \quad (2.1)$$

with ρ and μ the fluid density and dynamic viscosity, respectively.

We identify two characteristic length scales: a microscopic one, $\tilde{\ell}$, characterizing the porous bed, and a macroscopic one, \mathcal{L} , related to the large-scale motion in the channel. Provided that the two length scales are well-separated, i.e. $\tilde{\ell} \ll \mathcal{L}$, it is possible to manipulate the microscale problem by means of an asymptotic analysis in terms of a small parameter $\epsilon = \tilde{\ell}/\mathcal{L} \ll 1$. As illustrated in figure 1, the flow domain is decomposed into three distinct sub-domains: a channel-flow region away from the porous/free-fluid interface (superscript “C”), an interfacial region (superscript “I”) and a region within the porous layer away from boundaries, governed by Darcy’s law (superscript “P”). Correspondingly, the following three sets of normalized variables are proposed:

$$X_i = \frac{\hat{x}_i}{\mathcal{L}}, \quad U_i^C = \frac{\hat{u}}{\mathcal{U}}, \quad P^C = \frac{\hat{p}}{\rho \mathcal{U}^2}, \quad (2.2a)$$

$$x_i = \frac{\hat{x}_i}{\tilde{\ell}}, \quad U_i^I = \frac{\hat{u}}{\epsilon \mathcal{U}}, \quad P^I = \frac{\hat{p}}{\mu \mathcal{U} / \mathcal{L}}, \quad (2.2b)$$

$$x_i = \frac{\hat{x}_i}{\tilde{\ell}}, \quad U_i^P = \frac{\hat{u}}{\epsilon^2 \mathcal{U}}, \quad P^P = \frac{\hat{p}}{\mu \mathcal{U} / \mathcal{L}}, \quad (2.2c)$$

where \mathcal{U} is a suitable macroscopic velocity scale; a discussion on the proper selection of scales is provided later. Based on the normalization above, the governing equations (2.1) can be recast into the following dimensionless forms in the \bullet^C , \bullet^I , and \bullet^P regions, respectively;

$$\frac{\partial U_i^C}{\partial X_i} = 0, \quad \frac{\partial U_i^C}{\partial t} + U_j^C \frac{\partial U_i^C}{\partial X_j} = -\frac{\partial P^C}{\partial X_i} + \frac{1}{Re} \frac{\partial^2 U_i^C}{\partial X_j^2}, \quad (2.3a)$$

$$\frac{\partial U_i^I}{\partial x_i} = 0, \quad \epsilon^2 Re \left(\frac{\partial U_i^I}{\partial t} + U_j^I \frac{\partial U_i^I}{\partial x_j} \right) = -\frac{\partial P^I}{\partial x_i} + \frac{\partial^2 U_i^I}{\partial x_j^2}, \quad (2.3b)$$

$$\epsilon \frac{\partial U_i^P}{\partial x_i} = 0, \quad \epsilon^4 Re U_j^P \frac{\partial U_i^P}{\partial x_j} = -\frac{\partial P^P}{\partial x_i} + \epsilon \frac{\partial^2 U_i^P}{\partial x_j^2}, \quad (2.3c)$$

with $Re = \rho \mathcal{U} \mathcal{L} / \mu$. Note that the time scale is the same in the interface and free-fluid region ($t = \hat{t} \mathcal{U} / \mathcal{L}$) and that in the bulk of the porous domain the motion is assumed steady. In the intermediate and porous regions, the dependent variables are function of both the fast (microscopic) and the slow (macroscopic) coordinates (x_i , X_i respectively), whilst in the channel-flow region, the dependent variables vary spatially with the macroscopic coordinates,

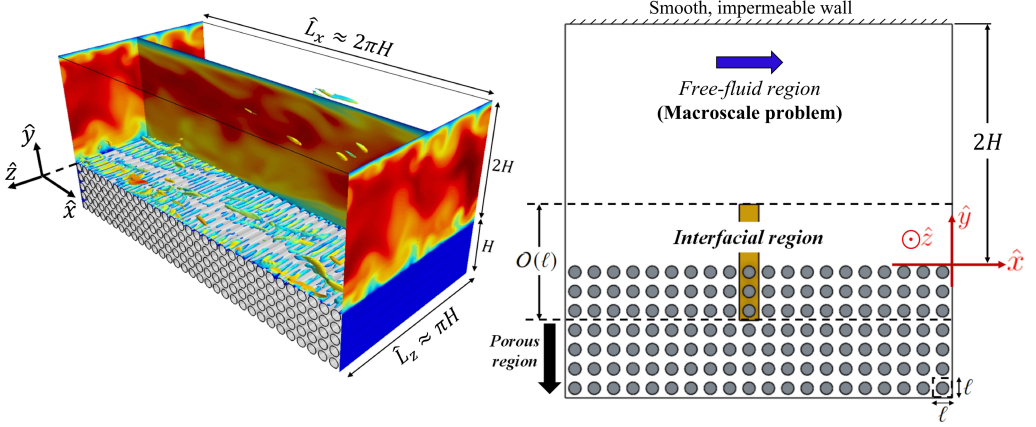


Figure 1: Sketch of the full domain for the case of a channel delimited from the top by a smooth, impermeable wall and from the bottom by a porous bed formed by spanwise-elongated cylindrical grains. The right frame illustrates in a constant \hat{z} -section the decomposition of the domain into three distinct sub-regions; the brown volume represents the horizontally periodic elementary cell of the microscopic problem.

222 X_i , only. A fictitious dividing surface between the channel-flow region and the interfacial
 223 layer is defined at $\hat{x}_2 = \hat{y}_\infty$, and continuity of the velocity and the traction vectors is applied
 224 there. With $y_\infty = \hat{y}_\infty/\tilde{\ell}$ and $\mathcal{Y}_\infty = \hat{y}_\infty/\mathcal{L} = \epsilon y_\infty$ the microscopic and the macroscopic vertical
 225 coordinates of this interface, respectively, the matching conditions can be written as follows:

$$226 \quad \lim_{x_2 \rightarrow y_\infty} U_i^I = \frac{1}{\epsilon} \lim_{X_2 \rightarrow \mathcal{Y}_\infty} U_i^C, \quad (2.4a)$$

227

$$228 \quad \lim_{x_2 \rightarrow y_\infty} \left(-P^I \delta_{i2} + \frac{\partial V^I}{\partial x_i} + \frac{\partial U_i^I}{\partial y} \right) = \lim_{X_2 \rightarrow \mathcal{Y}_\infty} \left(-Re P^C \delta_{i2} + \frac{\partial V^C}{\partial X_i} + \frac{\partial U_i^C}{\partial Y} \right), \quad (2.4b)$$

229 with δ_{ij} the Kronecker index. For the conditions above to be valid, y_∞ must be sufficiently
 230 large such that the \bullet^I variables become uniform in x and z at the virtual interface.

231

2.2. Asymptotic analysis of the microscale problem

232 The dependent variables in the interfacial and the porous sub-domains are expanded in terms
 233 of ϵ as

$$234 \quad U_i^I = U_i^{I(0)} + \epsilon U_i^{I(1)} + \epsilon^2 U_i^{I(2)} + \dots, \quad P^I = P^{I(0)} + \epsilon P^{I(1)} + \epsilon^2 P^{I(2)} + \dots,$$

235

$$236 \quad U_i^P = U_i^{P(0)} + \epsilon U_i^{P(1)} + \epsilon^2 U_i^{P(2)} + \dots, \quad P^P = P^{P(0)} + \epsilon P^{P(1)} + \epsilon^2 P^{P(2)} + \dots$$

237 Furthermore, the gradients are recast using the chain rule ($\frac{\partial}{\partial x_i} \rightarrow \frac{\partial}{\partial x_i} + \epsilon \frac{\partial}{\partial X_i}$). The asymp-
 238 totic expressions are substituted into the equations governing the flow in the microscopic
 239 regions, for the microscale problems to be reconstructed at different orders of ϵ . It has been
 240 shown (Naqvi & Bottaro 2021) that the resulting systems of equations for the interfacial and
 241 the porous regions can be combined by defining a composite description of the asymptotic
 242 expansions, that is

$$243 \quad u_i = u_i^{(0)} + \epsilon u_i^{(1)} + \mathcal{O}(\epsilon^2), \quad p = p^{(0)} + \epsilon p^{(1)} + \mathcal{O}(\epsilon^2), \quad (2.5a)$$

244 with

$$245 \quad u_i^{(0)} = \begin{cases} U_i^{\mathcal{I}(0)}, & y \in \mathcal{I} \\ \epsilon U_i^{\mathcal{P}(0)}, & y \in \mathcal{P} \end{cases}, \quad u_i^{(1)} = \begin{cases} U_i^{\mathcal{I}(1)}, & y \in \mathcal{I} \\ \epsilon U_i^{\mathcal{P}(1)}, & y \in \mathcal{P} \end{cases}, \quad (2.5b)$$

246 and

$$247 \quad p^{(0)} = \begin{cases} P^{\mathcal{I}(0)}, & y \in \mathcal{I} \\ P^{\mathcal{P}(0)} + \epsilon P^{\mathcal{P}(1)}, & y \in \mathcal{P} \end{cases}, \quad p^{(1)} = \begin{cases} P^{\mathcal{I}(1)}, & y \in \mathcal{I} \\ \epsilon P^{\mathcal{P}(2)}, & y \in \mathcal{P} \end{cases}. \quad (2.5c)$$

248 The following composite system, valid over the whole region below the dividing interface
249 (i.e., $x_2 < y_\infty$), is thus obtained:

$$250 \quad \begin{cases} \partial_i u_i = -\epsilon \partial'_i u_i^{(0)} + \mathcal{O}(\epsilon^2) \\ -\partial_i p + \partial_j^2 u_i = \mathcal{R} u_j \partial_j u_i + \epsilon \left[\partial'_i p^{(0)} - 2\partial_j \partial'_j u_i^{(0)} + \mathcal{R} u_j^{(0)} \partial'_j u_i^{(0)} \right] + \mathcal{O}(\epsilon^2) \end{cases} \quad (2.6)$$

251 with $\mathcal{R} = \epsilon^2 Re$ a microscopic Reynolds number and with derivatives indicated by $\partial_i = \frac{\partial}{\partial x_i}$

252 and $\partial'_i = \frac{\partial}{\partial X_i}$.

253 In order to treat the problem above, we first simplify it by linearising the convective
254 terms applying an Oseen approximation. In particular, a constant value is assigned to the
255 streamwise velocity component, u_1 , near the interface, chosen as the surface-averaged slip

256 velocity $u_{slip} = \frac{\hat{u}_{slip}}{\epsilon \mathcal{U}}$ (with \hat{u}_{slip} the dimensional slip velocity at the plane $\hat{y} = 0$), i.e.

257 $u_j^{(0)} \simeq (u_{slip}, 0, 0)^\dagger$. Thus, the advection term in (2.6) simplifies as $\mathcal{R} u_{slip} \partial_1 u_i$, with

$$258 \quad \mathcal{R} u_{slip} = \frac{\rho \hat{u}_{slip} \tilde{\ell}}{\mu} = Re_{slip}. \quad (2.7)$$

259 The quantity Re_{slip} is a slip-velocity Reynolds number, based on the microscopic length
260 scale $\tilde{\ell}$; as we will see later, its value is not necessarily small. The composite system (2.6) is
261 now approximated as

$$262 \quad \begin{cases} \partial_i u_i = -\epsilon \partial'_i u_i^{(0)} + \mathcal{O}(\epsilon^2) \\ -\partial_i p + \partial_j^2 u_i = Re_{slip} \partial_1 u_i + \epsilon \left[\partial'_i p^{(0)} - 2\partial_j \partial'_j u_i^{(0)} + Re_{slip} \partial'_1 u_i^{(0)} \right] + \mathcal{O}(\epsilon^2) \end{cases} \quad (2.8)$$

263 The leading-order problem reads:

$$264 \quad \mathcal{O}(1) : \begin{cases} \partial_i u_i^{(0)} = 0, \\ -\partial_i p^{(0)} + \partial_j^2 u_i^{(0)} = Re_{slip} \partial_1 u_i^{(0)}, \\ \left(-p^{(0)} \delta_{i_2} + \partial_2 u_i^{(0)} + \partial_i u_2^{(0)} \right)_{x_2=y_\infty} = S_{i_2}^C, \end{cases} \quad (2.9)$$

265 with $S_{i_2}^C$ the macroscopic traction vector evaluated at $X_2 = \mathcal{Y}_\infty$, i.e.

$$266 \quad S_{i_2}^C = \boldsymbol{\sigma}^C \cdot \mathbf{e}_2|_{X_2=\mathcal{Y}_\infty} = \left(\frac{\partial U^C}{\partial Y} + \frac{\partial V^C}{\partial X}, -RePC + 2\frac{\partial V^C}{\partial Y}, \frac{\partial W^C}{\partial Y} + \frac{\partial V^C}{\partial Z} \right) \Big|_{X_2=\mathcal{Y}_\infty}, \quad (2.10)$$

267 where $\boldsymbol{\sigma}^C$ is the stress tensor. From now on, the outer dependent variables are written without
268 the superscript \bullet^C .

\dagger Other choices are clearly possible. For example, Bottaro (2019) tested the friction velocity as advective speed; results shown in the following support the present choice of the slip velocity.

269 At next order, we have

$$270 \quad O(\epsilon) : \begin{cases} \partial_i u_i^{(1)} = -\partial'_i u_i^{(0)}, \\ -\partial_i p^{(1)} + \partial_j^2 u_i^{(1)} = Re_{slip} \left(\partial_1 u_i^{(1)} + \partial'_1 u_i^{(0)} \right) + \partial'_i p^{(0)} - 2\partial_j \partial'_j u_i^{(0)}, \\ \left(-p^{(1)} \delta_{i2} + \partial_2 u_i^{(1)} + \partial_i u_2^{(1)} \right) \Big|_{x_2=y_\infty} = - \left(\partial'_2 u_i^{(0)} + \partial'_i u_2^{(0)} \right) \Big|_{x_2=y_\infty}. \end{cases} \quad (2.11)$$

271 The linearity of (2.9) and (2.11) permits us to assume generic solutions of the problems.
272 For the leading-order problem, we express the dependent variables as

$$273 \quad \begin{cases} u_i^{(0)} = u_{ij}^\dagger S_{j2}, \\ p^{(0)} = p_j^\dagger S_{j2}, \end{cases} \quad (2.12)$$

274 with the closure variables, u_{ij}^\dagger and p_j^\dagger , dependent on only the microscopic coordinates, x_i .
275 Decoupled *ad hoc* auxiliary systems arise from plugging the generic solutions into (2.9);
276 they are

$$277 \quad \begin{cases} \partial_i u_{ij}^\dagger = 0, \\ -\partial_i p_j^\dagger + \partial_l^2 u_{ij}^\dagger = Re_{slip} \partial_1 u_{ij}^\dagger, \\ \left(-p_j^\dagger \delta_{i2} + \partial_2 u_{ij}^\dagger + \partial_i u_{2j}^\dagger \right) \Big|_{x_2=y_\infty} = \delta_{ij}, \end{cases} \quad (2.13)$$

278 where the microscopic problems correspond to $j = 1, 2, 3$. For the problem forced by S_{22}
279 (i.e. with $j = 2$), the analytical solution $u_{i2}^\dagger = 0$, $p_2^\dagger = -1$ is easily retrieved. At $O(\epsilon)$ the
280 following generic forms hold:

$$281 \quad \begin{cases} u_i^{(1)} = u_{ijk}^\ddagger \partial'_k S_{j2}, \\ p^{(1)} = p_{jk}^\ddagger \partial'_k S_{j2}, \end{cases} \quad (2.14)$$

282 leading to

$$283 \quad \begin{cases} \partial_i u_{ijk}^\ddagger = -u_{kj}^\dagger, \\ Re_{slip} \left(\partial_1 u_{ijk}^\ddagger + u_{ij}^\dagger \delta_{k1} \right) = -\partial_i p_{jk}^\ddagger - p_j^\dagger \delta_{ki} + \partial_l^2 u_{ijk}^\ddagger + 2\partial_k u_{ij}^\dagger, \\ \left(-p_{jk}^\ddagger \delta_{i2} + \partial_2 u_{ijk}^\ddagger + \partial_i u_{2jk}^\ddagger \right) \Big|_{x_2=y_\infty} = - \left(u_{ij}^\dagger \delta_{k2} + u_{2j}^\dagger \delta_{ik} \right) \Big|_{x_2=y_\infty}; \end{cases} \quad (2.15)$$

284 these are nine decoupled systems, i.e. corresponding to $j, k = 1, 2, 3$. The closure problems
285 (2.13) and (2.15) are to be solved in a representative unit cell of the microscopic region,
286 subject to periodicity of all the dependent variables along x and z and to the boundary
287 conditions $u_{ij}^\dagger = 0$ and $u_{ijk}^\ddagger = 0$ on the solid grains, arising from the no-slip condition.
288 Further, the microscopic unit cell is delimited from the bottom (theoretically at $y \rightarrow -\infty$) by
289 the bulk of the porous domain, where dependent variables are cyclic of period 1 also along
290 y ; from a numerical perspective, results do not change provided the domain is at least two
291 rows deep.

292 2.3. Formal expressions of the effective boundary conditions

293 Numerical solutions are sought for systems (2.13) and (2.15), with focus on the values of
294 the fields at $x_2 = y_\infty$ since $u_{ij}^\dagger \Big|_{y_\infty}$ and $u_{ijk}^\ddagger \Big|_{y_\infty}$ are eventually the coefficients needed to close
295 the macroscopic effective boundary conditions for the velocity; these conditions result from
296 matching the velocity vector at the fictitious interface between the channel-flow and the

297 interfacial regions, as per (2.4a). The upscaled conditions, second-order accurate in terms of
 298 ϵ , are:

$$299 \quad U_i|_{y_\infty} = \epsilon \left(u_i^{(0)} \Big|_{y_\infty} + \epsilon u_i^{(1)} \Big|_{y_\infty} \right) + \mathcal{O}(\epsilon^3) = \epsilon u_{ij}^\dagger \Big|_{y_\infty} S_{j2} + \epsilon^2 u_{ijk}^\ddagger \Big|_{y_\infty} \frac{\partial S_{j2}}{\partial X_k} + \mathcal{O}(\epsilon^3). \quad (2.16)$$

300 The numerical procedure to solve the closure problems is similar to that followed by Naqvi
 301 & Bottaro (2021) and Ahmed *et al.* (2022b) for porous media of either isotropic (such as
 302 spherical grains) or transversely isotropic microstructures in the \hat{x} – \hat{z} plane (such as spanwise-
 303 or streamwise-elongated elements). We focus on the same parameters which do not vanish
 304 at the matching interface found in these references:

$$305 \quad \begin{aligned} u_{11}^\dagger \Big|_{y_\infty} &= y_\infty + \lambda_x, & u_{33}^\dagger \Big|_{y_\infty} &= y_\infty + \lambda_z, \\ -u_{211}^\ddagger \Big|_{y_\infty} &= u_{121}^\ddagger \Big|_{y_\infty} = 0.5 y_\infty^2 + \lambda_x y_\infty + \mathcal{K}_{xy}^{itf}, \\ -u_{233}^\ddagger \Big|_{y_\infty} &= u_{323}^\ddagger \Big|_{y_\infty} = 0.5 y_\infty^2 + \lambda_z y_\infty + \mathcal{K}_{zy}^{itf}, \\ u_{222}^\ddagger \Big|_{y_\infty} &= \mathcal{K}_{yy}, \end{aligned} \quad (2.17)$$

306 with λ_x and λ_z the dimensionless Navier’s slip coefficients in the streamwise and the
 307 spanwise directions, respectively, \mathcal{K}_{xy}^{itf} and \mathcal{K}_{zy}^{itf} the *interface permeability* coefficients, and
 308 \mathcal{K}_{yy} an *intrinsic permeability* component. The novel contribution here is the incorporation
 309 of the effect of near-interface inertia on the microscale flow behavior, which renders the
 310 aforementioned parameters sensitive to the value of Re_{slip} .

311 Once relations (2.17) are plugged into (2.16) macroscopic matching conditions at the
 312 interface $Y_\infty = \epsilon y_\infty$ between the intermediate and the outer region are obtained. These
 313 conditions can then be transferred to $Y = 0$ by a second-order Taylor expansion, to eventually
 314 yield the following effective boundary conditions:

$$315 \quad U|_{Y=0} = \epsilon \lambda_x S_{12}|_{Y=0} + \epsilon^2 \mathcal{K}_{xy}^{itf} \frac{\partial S_{22}}{\partial X} \Big|_{Y=0} + \mathcal{O}(\epsilon^3), \quad (2.18a)$$

$$317 \quad V|_{Y=0} = -\epsilon^2 \mathcal{K}_{xy}^{itf} \frac{\partial S_{12}}{\partial X} \Big|_{Y=0} - \epsilon^2 \mathcal{K}_{zy}^{itf} \frac{\partial S_{32}}{\partial Z} \Big|_{Y=0} + \epsilon^2 \mathcal{K}_{yy} \frac{\partial S_{22}}{\partial Y} \Big|_{Y=0} + \mathcal{O}(\epsilon^3), \quad (2.18b)$$

$$319 \quad W|_{Y=0} = \epsilon \lambda_z S_{32}|_{Y=0} + \epsilon^2 \mathcal{K}_{zy}^{itf} \frac{\partial S_{22}}{\partial Z} \Big|_{Y=0} + \mathcal{O}(\epsilon^3). \quad (2.18c)$$

320 At this point, something should be said on the scales ($\tilde{\ell}$, \mathcal{L} , \mathcal{U}) used to normalize the preceding
 321 equations, and on whether the principle of separation of scales is satisfied. If the magnitude of
 322 the macroscopic pressure gradient driving the flow in the channel is $\mathcal{M} = |\Delta \hat{p} / \tilde{L}_x|$, one may
 323 derive a stress $\tau_M = \mathcal{M} H = (\tau_B + \tau_T)/2$, with τ_B and τ_T the total shear stresses at $Y = 0$
 324 (bottom) and $Y = 2$ (top), respectively. The corresponding shear velocity $u_{\tau(M)} = \sqrt{\tau_M / \rho}$
 325 is chosen here as the macroscopic velocity scale, i.e. $\mathcal{U} = u_{\tau(M)}$. This is an appropriate
 326 characterization of the velocity of near-wall eddies, since it is known that the root mean
 327 square of the fluctuating speed scales with the friction velocity. As far as the macroscopic
 328 length scale is concerned, it has been proposed first by Luchini (1996) that the important
 329 boundary condition for turbulence is that experienced by quasi-streamwise vortices. The
 330 relevant length scale should thus be the vortex diameter which is around 20 viscous units, i.e.
 331 $\mathcal{L} \sim \alpha \frac{\nu}{u_{\tau(M)}}$, with α a constant close to 20. As far as the microlength scale is concerned,

332 we observe that in the asymptotic analysis by Saffman (1971) for the case of the flow over an

isotropic porous substrate of permeability K , the choice $\tilde{\ell} = \sqrt{K}$ was made. Recently, [Hao & García-Mayoral \(2024\)](#) have argued that the effect of deep porous substrates (those considered in the present paper can also be characterized as “deep”) on the near-wall flow is essentially governed by the intrinsic permeability of the medium, which, in all cases considered here, is a small fraction of ℓ^2 (cf. also [Mei & Vernescu \(2010\)](#); [Zampogna *et al.* \(2019a\)](#); [Lācis *et al.* \(2020\)](#); [Naqvi & Bottaro \(2021\)](#); [Sudhakar *et al.* \(2021\)](#)), with ℓ the periodicity of the grains. For regularly roughened walls, when a substrate permeability cannot be defined, the proper length scale should be a measure of the slip length of the texture, also a small fraction of the periodicity, ℓ . A reader might, at this point, want to anticipate inspection of [table 2](#) where results for all the macroscopic coefficients are given in viscous (“plus”) units, and compare with the corresponding values of ℓ^+ : it is consistently found, for example for the case of cylindrical inclusions, either longitudinal or transverse, that ℓ^+ is about 20 times larger than $\sqrt{\mathcal{K}_{yy}^+}$. Thus, it seems appropriate to say that $\tilde{\ell} \sim \ell/\alpha$, with the same value of the constant α as in the definition of the macrolength \mathcal{L} . We are now able to estimate the small parameter ϵ of the expansion; it is found that $\epsilon \sim \ell^+/\alpha^2$ ranges from around 0.025 up to 0.1 for cylindrical inclusions having ℓ^+ values between 10 and 40. For the “modified” grains described later, ϵ would be even smaller, considering that such inclusions tend to block the flow and the permeability is much lower than in the previous case.

On the basis of the arguments presented, microscopic and macroscopic length scales are sufficiently well separated, for all the cases treated in this paper. The microscopic length scale in our analysis is the displacement of the origin of the near-wall vortex, caused by the presence of either a rough or a porous substrate; the macroscopic scale is the diameter of the vortex itself. One referee of this work objected vigorously to our choice of microscopic length scale, arguing that the only proper microscale is the pattern periodicity. If, as they objected, this was indeed the case, then $\tilde{\ell} \sim \ell$ and the parameter of the expansion would become $\epsilon \sim \ell^+/\alpha$, which exceeds 1 for $\ell^+ > 20$. Beyond $\ell^+ \approx 20$, they argued, separation of scale, and the expansion proposed, would be untenable. In the end, we believe that only *a posteriori* verifications against feature-resolving results can inform on the domain of validity of the upscaling procedure adopted; this crucial point will be addressed in [Sections 3.1 and 4](#).

In dimensional form, the effective boundary conditions are the same that have been found before ([Naqvi & Bottaro 2021](#)) and read

$$\hat{u}|_0 \approx \hat{\lambda}_x \left(\frac{\partial \hat{u}}{\partial \hat{y}} + \frac{\partial \hat{v}}{\partial \hat{x}} \right) \Big|_0 + \frac{\hat{\mathcal{K}}_{xy}^{itf}}{\mu} \frac{\partial}{\partial \hat{x}} \left(-\hat{p} + 2\mu \frac{\partial \hat{v}}{\partial \hat{y}} \right) \Big|_0, \quad (2.19a)$$

$$\hat{v}|_0 \approx \frac{\hat{\mathcal{K}}_{yy}}{\mu} \frac{\partial}{\partial \hat{y}} \left(-\hat{p} + 2\mu \frac{\partial \hat{v}}{\partial \hat{y}} \right) \Big|_0 - \hat{\mathcal{K}}_{xy}^{itf} \frac{\partial}{\partial \hat{x}} \left(\frac{\partial \hat{u}}{\partial \hat{y}} + \frac{\partial \hat{v}}{\partial \hat{x}} \right) \Big|_0 - \hat{\mathcal{K}}_{zy}^{itf} \frac{\partial}{\partial \hat{z}} \left(\frac{\partial \hat{w}}{\partial \hat{y}} + \frac{\partial \hat{v}}{\partial \hat{z}} \right) \Big|_0, \quad (2.19b)$$

$$\hat{w}|_0 \approx \hat{\lambda}_z \left(\frac{\partial \hat{w}}{\partial \hat{y}} + \frac{\partial \hat{v}}{\partial \hat{z}} \right) \Big|_0 + \frac{\hat{\mathcal{K}}_{zy}^{itf}}{\mu} \frac{\partial}{\partial \hat{z}} \left(-\hat{p} + 2\mu \frac{\partial \hat{v}}{\partial \hat{y}} \right) \Big|_0. \quad (2.19c)$$

Further considerations, simplifications, and implementation-related details concerning the condition [\(2.19b\)](#) are given in [Appendix A](#). After having established the effective conditions which hold at $\hat{y} = 0$, we can render them adimensional in the most convenient way. Thus, we now choose to scale the governing equations [\(2.1\)](#) for the free fluid region, as well as the corresponding interface conditions [\(2.19a\)–\(2.19c\)](#), by the use of geometric scales (cf. [figure 1](#)); this corresponds to setting $\mathcal{L} = H$ in equations [\(2.2a–2.2c\)](#). By the same token, the microscopic problems in the unit cells is rescaled with the periodicity of the pattern and this

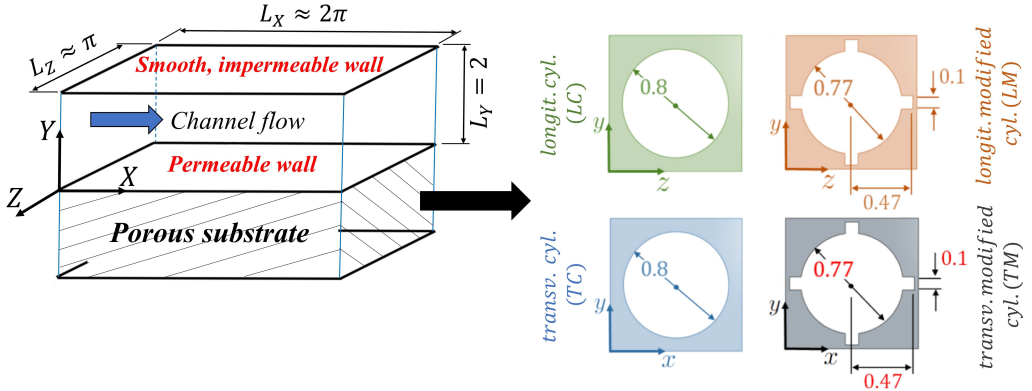


Figure 2: The problems under study. The computational domain is displayed in the left panel, with the dimensions indicated in the macroscopic coordinates (normalized by half the channel height). On the right, the bulk unit cell of the different porous media considered are drawn in microscopic dimensionless coordinates. All media have porosity $\theta = 0.5$.

377 amounts to setting $\tilde{\ell} = \ell$ in equations (2.2a–2.2c) so that, eventually, ϵ is defined by the ratio
 378 ℓ over H , like in the laminar case (Naqvi & Bottaro 2021; Ahmed & Bottaro 2024). Having
 379 rescaled the problem for computational convenience, the dimensional model coefficients now
 380 read

$$381 \quad \hat{\lambda}_{x,z} = \lambda_{x,z} l, \quad \hat{\mathcal{K}}_{xy,zy}^{itf} = \mathcal{K}_{xy,zy}^{itf} l^2, \quad \hat{\mathcal{K}}_{yy} = \mathcal{K}_{yy} l^2. \quad (2.20)$$

382 We want to emphasize that these coefficients are not empirical, but arise from the solution of
 383 auxiliary systems of equations solved in the \hat{x} - or \hat{z} -periodic elementary cell of fig. 1. The two
 384 terms, $\hat{\mathcal{K}}_{xy}^{itf}$ and $\hat{\mathcal{K}}_{zy}^{itf}$, are *interface permeabilities* since, in analogy to Darcy's law in the bulk
 385 of the porous domain, they multiply the streamwise and spanwise gradients of the pressure
 386 in the expressions of $\hat{u}|_0$ and $\hat{w}|_0$. They differ from the corresponding *intrinsic permeability*
 387 components which come from the solution of Stokes problems in a triply periodic unit cell
 388 taken in the bulk of the porous region and, as such, have little in common with the flow
 389 around the porous/free-fluid interface (Bottaro 2019).

390 2.4. Evaluation of the macroscopic coefficients for selected geometries

391 Typical geometries of the inclusions used to construct the porous media under study are
 392 illustrated in figure 2; they are aligned in either the streamwise direction (substrates *LC* and
 393 *LM*) or the spanwise direction (substrates *TC* and *TM*), all satisfying a porosity $\theta = 0.5$,
 394 where θ is defined by considering a cubic unit cell within the porous region and evaluating
 395 the ratio of the volume occupied by the fluid to the total volume of the cell.

396 A simple method, similar to that followed by Ahmed *et al.* (2022b), is used to numerically
 397 evaluate the macroscopic coefficients in the effective boundary conditions. First, the systems
 398 governing the microscale fields u_{11}^\dagger and u_{33}^\dagger are solved on a microscopic domain with a
 399 sufficiently large value of y_∞ (like, for instance, the domain sketched in the left frame of
 400 figure 3). In this work, the solution of the closure problems is conducted using finite-volume
 401 discretization, as by the implementation of Simcenter STAR-CCM+ software; in general,
 402 the microscopic domain is discretized into polygonal/polyhedral cells with sufficient mesh
 403 refinement in close vicinity of the porous/free-fluid interface such that grid-independent
 404 results for the closure fields are eventually obtained. Second, the Navier's slip coefficients
 405 (λ_x, λ_z) are estimated by averaging u_{11}^\dagger and u_{33}^\dagger , respectively, over the plane $y = 0$. The
 406 numerical values of the interface permeability coefficients can be computed via the following

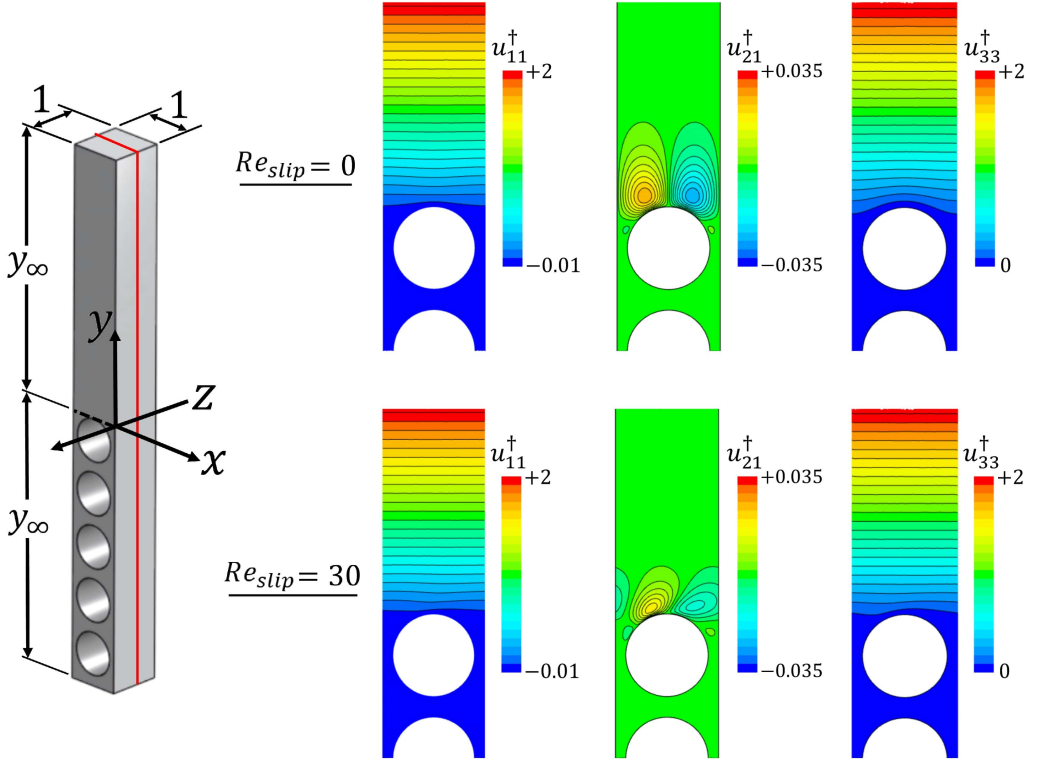


Figure 3: Contours of the microscopic variables u_{11}^\dagger , u_{21}^\dagger , and u_{33}^\dagger at (top) $Re_{slip} = 0$ and (bottom) $Re_{slip} = 30$, shown over an $x - y$ plane for the case of transverse cylinders of porosity $\theta = 0.5$. Close-ups of the contours near the fluid-porous interface are presented, while the typical domain considered in the simulations is shown in the left frame. Slip and permeability coefficients are independent of the value of y_∞ , provided it is larger than 2.

407 volume integrals:

$$\begin{aligned}
 \mathcal{K}_{xy}^{itf} &= \int_{\mathcal{V}_0} u_{11}^\dagger dV, \\
 \mathcal{K}_{zy}^{itf} &= \int_{\mathcal{V}_0} u_{33}^\dagger dV,
 \end{aligned}
 \tag{2.21}$$

409 where \mathcal{V}_0 denotes the whole fluid's volume in the elementary cell below the interface
 410 chosen at $y = 0$. This renders the dimensionless Navier-slip and the interface permeability
 411 coefficients dependent, in general, on the geometry of the inclusions and the slip-velocity
 412 Reynolds number, Re_{slip} , which appears in the microscopic auxiliary systems[†]. On the other
 413 hand, the medium permeability \mathcal{K}_{yy} is intrinsic to the geometry of the porous region, where
 414 the velocity level is much smaller than u_{slip} and the inertial effects are thus negligible; \mathcal{K}_{yy}
 415 can be estimated by solving a Stokes system on a triply-periodic cell of the porous domain,
 416 imposing unit forcing along y , and evaluating the superficial average of the corresponding
 417 microscopic field over that cell (Mei & Vernescu 2010).

418 Transverse (\hat{z} -elongated) and longitudinal (\hat{x} -elongated) inclusions allow for further
 419 simplification of the microscopic, auxiliary problems, by setting either $\partial/\partial x_3$ or $\partial/\partial x_1$ to
 420 zero, respectively, yielding two-dimensional systems of equations. For the case of spanwise-

[†] Note that, after rescaling, Re_{slip} is now defined with ℓ as length scale.

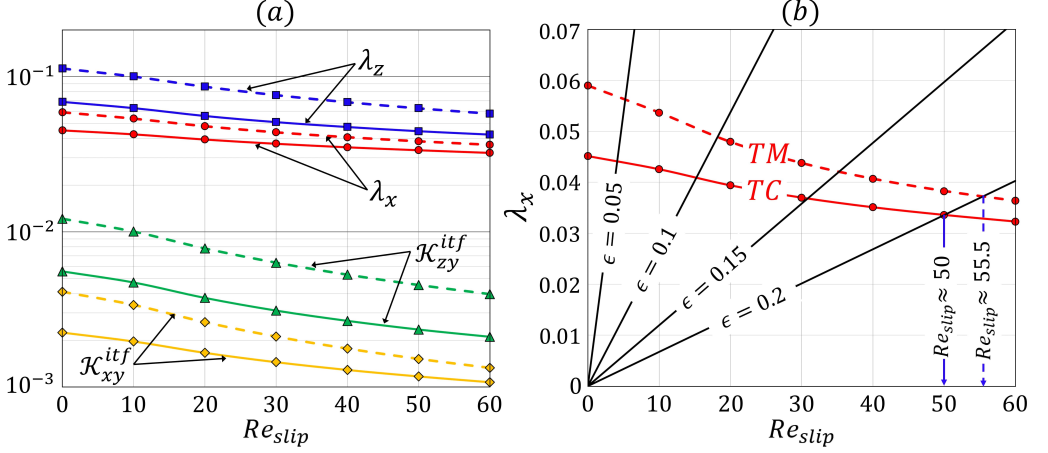


Figure 4: Behaviors of the homogenization model parameters. Frame (a) displays results of the closure problems for the Navier-slip and interface permeability coefficients as functions of Re_{slip} for the porous substrates *TC* (solid lines) and *TM* (dashed lines). In panel (b), the linear relation (2.26) between λ_x and Re_{slip} is plotted (black lines) for four values of ϵ , fixing $Re_{\tau(M)} = 193$, in order to evaluate Re_{slip} at the intersection points.

421 elongated inclusions, we get the following two systems of interest at leading order:

$$422 \quad \begin{cases} \partial_1 u_{11}^\dagger + \partial_2 u_{21}^\dagger = 0, \\ -\partial_1 p_1^\dagger + \partial_1^2 u_{11}^\dagger + \partial_2^2 u_{11}^\dagger = Re_{slip} \partial_1 u_{11}^\dagger, \\ -\partial_2 p_1^\dagger + \partial_1^2 u_{21}^\dagger + \partial_2^2 u_{21}^\dagger = Re_{slip} \partial_1 u_{21}^\dagger, \\ \left. (\partial_2 u_{11}^\dagger + \partial_1 u_{21}^\dagger) \right|_{x_2=y_\infty} = 1, \\ \left. (-p_1^\dagger + 2\partial_2 u_{21}^\dagger) \right|_{x_2=y_\infty} = 0, \end{cases} \quad (2.22)$$

423 and

$$424 \quad \begin{cases} \partial_1^2 u_{33}^\dagger + \partial_2^2 u_{33}^\dagger = Re_{slip} \partial_1 u_{33}^\dagger, \\ \left. (\partial_2 u_{33}^\dagger) \right|_{x_2=y_\infty} = 1. \end{cases} \quad (2.23)$$

425 The numerical solutions of the previous systems under Stokes conditions and at $Re_{slip} = 30$
 426 are shown in figure 3 for the case of transverse cylindrical inclusions, while the dependence
 427 of the macroscopic coefficients on Re_{slip} is displayed in figure 4(a) for the substrates *TC*
 428 and *TM*. A preliminary estimation of the value of the slip velocity can be obtained from the
 429 first-order term in the effective boundary condition of U , equation (2.18a), which may be
 430 recast in terms of the wall distance in viscous units ($Y^+ = Y Re_{\tau(M)}$) and the mean velocity,
 431 already normalized by $u_{\tau(M)}$ and hence from now on indicated as \bar{U}^+ , as follows:

$$432 \quad \bar{U}^+ \Big|_{Y=0} \approx \lambda_x^+ \frac{\partial \bar{U}^+}{\partial Y^+} \Big|_{Y=0}, \quad (2.24)$$

433 where $\lambda_x^+ = \frac{\rho u_{\tau(M)} \hat{\lambda}_x}{\mu} = \epsilon Re_{\tau(M)} \lambda_x$. Provided the roughness maintains a sufficiently small

Table 1: Values of the macroscopic coefficients for the sixteen porous substrates considered in the present study. For all patterns, the porosity is $\theta = 0.5$ and $Re_{\tau(\mathcal{M})} = 193$, while $\epsilon = \ell/H$ is varied from 0.05 (subscript 5) to 0.2 (subscript 20).

Substrate	Re_{slip} (intersection)	Dimensionless macroscopic coefficients				
		λ_x	λ_z	\mathcal{K}_{xy}^{iff}	\mathcal{K}_{zy}^{iff}	\mathcal{K}_{yy}
TC_5	4.1	0.0440	0.0663	0.0021	0.0052	0.0018
TC_{10}	15.2	0.0409	0.0591	0.0018	0.0042	0.0018
TC_{15}	30.9	0.0368	0.0506	0.0014	0.0031	0.0018
TC_{20}	50.0	0.0336	0.0445	0.0012	0.0023	0.0018
LC_{5-20}	Any	0.0688	0.0451	0.0056	0.0022	0.0018
TM_5	5.3	0.0562	0.1062	0.0037	0.0110	0.00012
TM_{10}	18.2	0.0489	0.0888	0.0028	0.0082	0.00012
TM_{15}	35.3	0.0421	0.0721	0.0019	0.0058	0.00012
TM_{20}	55.5	0.0372	0.0599	0.0014	0.0042	0.00012
LM_{5-20}	Any	0.1130	0.0590	0.0121	0.0041	0.00012

434 amplitude so that the velocity gradient $\left. \frac{\partial \bar{U}^+}{\partial Y^+} \right|_{Y=0}$ at the virtual wall remains close to 1, (2.24)
 435 simplifies to a Dirichlet boundary condition, i.e.

$$436 \quad \left. \bar{U}^+ \right|_{Y=0} = \frac{\hat{u}_{slip}}{u_{\tau(\mathcal{M})}} \approx \epsilon Re_{\tau(\mathcal{M})} \lambda_x, \quad (2.25)$$

437 which means that the slip-velocity Reynolds number can be written as

$$438 \quad Re_{slip} = \frac{\rho \hat{u}_{slip} \ell}{\mu} = \frac{\rho u_{\tau(\mathcal{M})} \ell}{\mu} \epsilon Re_{\tau(\mathcal{M})} \lambda_x = \epsilon^2 Re_{\tau(\mathcal{M})}^2 \lambda_x. \quad (2.26)$$

439 With $\lambda_x = \frac{Re_{slip}}{\epsilon^2 Re_{\tau(\mathcal{M})}^2}$, a linear relation between λ_x and Re_{slip} can be drawn for different
 440 values of ϵ , at the fixed value of the friction Reynolds number, $Re_{\tau(\mathcal{M})} = 193$; cf. figure 4(b).
 441 The value of Re_{slip} at the intersection point is evaluated as shown in figure 4(b), yielding as
 442 an immediate consequence all the macroscopic coefficients at this value; table 1 reports all
 443 coefficients for ϵ ranging from 0.05 to 0.2. The reader is referred here to the work by Fairhall
 444 *et al.* (2019) where useful findings regarding the possible deviations of the slip lengths from
 445 the viscous predictions are presented for surface textures different from those considered
 446 here.

447 Streamwise-elongated inclusions (substrates LC and LM) represent a special case since
 448 inertial effects at the microscale level disappear as a consequence of setting $\partial/\partial x_1$ to 0 in the
 449 auxiliary systems (Luchini *et al.* 1991); as such, the macroscopic coefficients are independent

450 of Re_{slip} . The coefficients for these substrates are directly available by revisiting the results for
 451 TC and TM , at $Re_{slip} = 0$, and simply switching the streamwise and spanwise coordinates.

452 3. The macroscale problems

453 For the direct numerical simulations (DNSs) of the macroscale problem, considering the
 454 turbulent channel flow over different porous substrates, the numerical procedure is the same
 455 as that followed by [Ahmed et al. \(2022b\)](#). The dimensions of the computational domain, which
 456 represents here the free-fluid region above the modeled substrate, are $L_X \times L_Y \times L_Z = 2\pi \times 2 \times \pi$
 457 (cf. figure 1) as adopted by other researchers before ([Khorasani et al. 2022](#); [Hao & García-
 458 Mayoral 2024](#)). The mesh is uniform in the streamwise (X) and spanwise (Z) directions, while
 459 it is stretched gradually in the wall-normal direction (Y) departing from the upper and lower
 460 walls (thinnest layer) towards the centerline of the channel (thickest layer); the grid spacings
 461 in viscous units are $h_X^+ = 9.47$, $h_Z^+ = 6.32$, $h_Y^+|_{min} = 0.27$, $h_Y^+|_{max} = 9.25$. The DNSs
 462 are run using the Simcenter STAR-CCM+ finite-volume-based software. For the convective
 463 fluxes, a hybrid third-order discretization scheme is employed, formulated as a linear blend
 464 between a *MUSCL* (Monotone Upstream-centered Schemes for Conservation Laws) third-
 465 order upwind and a third-order central-differencing scheme, with the upwind blending factor
 466 set to 0.1 (i.e., 10% *MUSCL* and 90% central differencing); the reader is referred to the
 467 paper by [van Leer & Nishikawa \(2021\)](#) for further information on *MUSCL*, and to the work
 468 by [West & Caraeni \(2015\)](#) in which the hybrid *MUSCL/CD* approach is implemented. The
 469 computation of gradients is based on the least squares method, with the Venkatakrisnan
 470 gradient limiter activated ([Venkatakrisnan 1993](#)). A pressure correction approach is used
 471 for the pressure-velocity coupling; a second-order fully implicit scheme is employed for the
 472 temporal discretization with time step set to $0.0015 H/u_\tau$ and a minimum of 20 internal
 473 iterations performed for each time step. The averaging time, after the initial transient phase,
 474 is generally between 18 and $35 H/u_\tau$. With the above-mentioned settings and schemes,
 475 [Ahmed et al. \(2022b\)](#) found excellent agreement between the numerical results obtained for
 476 turbulence in a smooth channel (at $Re_\tau = 193$) and corresponding results from previous
 477 studies ([Kim et al. 1987](#); [Vreman & Kuerten 2014](#))[†]. However, given that the DNSs are run
 478 here for turbulence over different modeled substrates using a fixed time step ($0.0015 H/u_\tau$),
 479 there is a possibility that the maximum convective Courant–Friedrichs–Lewy (CFL) number
 480 exceeds 1. This issue has been checked, and it has been found that the maximum convective
 481 CFL number increases to around 2 for the largest value of ϵ considered, i.e., $\epsilon = 0.2$, in the
 482 vicinity of the interface ($0 \lesssim Y^+ \lesssim 15$). Because of this, the homogenization-based DNS
 483 for the pattern TC_{20} was rerun with a smaller time step, satisfying $CFL \lesssim 1$; the comparison
 484 revealed marginal deviations in the results for the main quantities characterizing the turbulent
 485 flow. Finally, it is appropriate to provide further details on how the transpiration boundary
 486 condition (2.19b) is enforced in the numerical code; they are given in Appendix A.

487

3.1. Validation of the model

488 The applicability of the upscaling approach followed is assessed here by considering the
 489 turbulent flow ($Re_{\tau(M)} = 193$) in a channel delimited from the bottom ($Y \leq 0$) by
 490 the substrate TC_{20} (transverse cylinders, $\epsilon = 0.2$), and validating sample results of the
 491 homogenized simulation, based on the effective boundary conditions (2.18a–2.18c) with the
 492 macroscopic coefficients given in Table 1, against a classical fine-grained simulation. The

[†] Unfortunately, a direct comparison with other homogenization-based DNSs is not possible, since no other paper we are aware of uses the same boundary conditions described here to model turbulence over a rough, permeable wall.

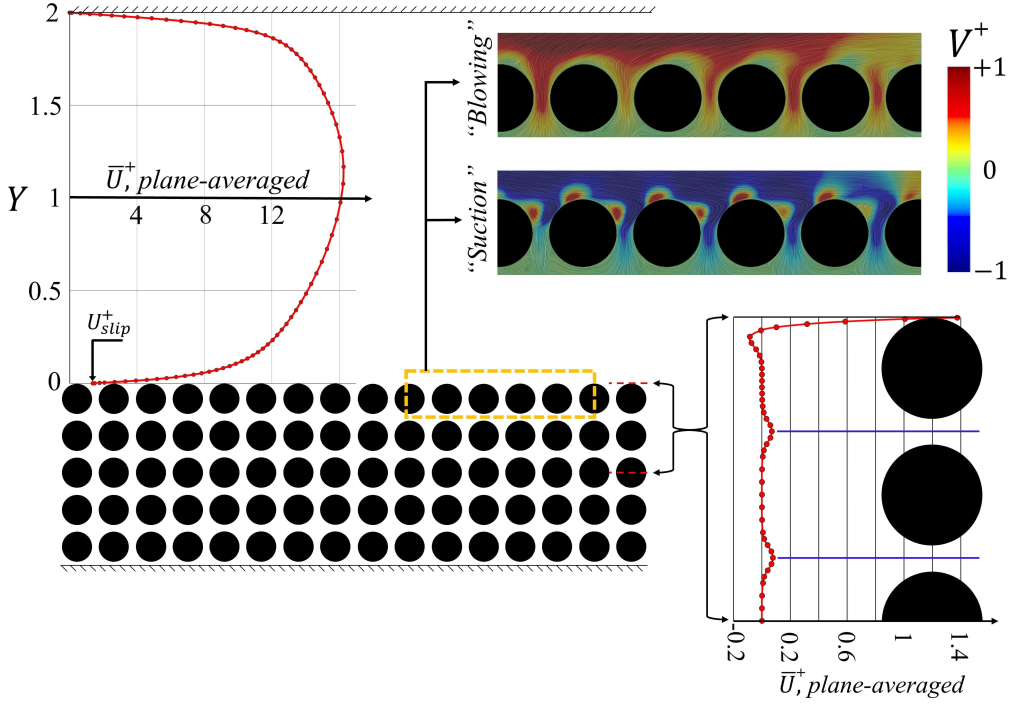


Figure 5: Full feature-resolving simulation of the coupled flow problem including the flow through and the turbulent flow over the porous substrate TC_{20} at $Re_{\tau(M)} = 193$; profiles of the X - Z -averaged mean velocity across the free-fluid region and closely below the fluid-porous interface are plotted. Instantaneous distributions (examples) of the interface-normal velocity component, V^+ , captured during “suction” and “blowing” events are also displayed.

493 mesh requirements, and thus the numerical cost, of the latter are much higher since it needs to
 494 resolve the seepage flow in the bulk of the porous domain and to account for the interactions
 495 occurring across the interfacial region, where significant ejection and sweep events take
 496 place (cf. figure 5). Quantitatively, the number of finite-volume cells in the fully resolving
 497 DNS ($N_{cells} \approx 7.3 \times 10^6$) is four times that in the homogenized DNS ($N_{cells} \approx 1.8 \times 10^6$).
 498 Another point to be taken into account with respect to the full DNS is the technical complexity
 499 associated with the mesh generation, especially in the interfacial region. An unstructured grid
 500 was used in the porous substrate and in the lower half of the channel; the cells are polygonal
 501 in section (on the $X - Y$ plane) and are extruded in the spanwise direction with a uniform
 502 spacing of ≈ 6 viscous units. For the top row of cylinders (the closest to the porous/free-fluid
 503 interface), the mesh is refined such that the first cell center is at a distance of around 0.3
 504 viscous units from the cylindrical grain, measured in the direction normal to the boundary.

505 The results in the free-fluid region are presented and compared (homogenization-based
 506 vs. fine-grained) in figures 6 and 7, in terms of the following dimensionless paramet-
 507 ers: the mean velocity, \bar{U}^+ ; the root-mean-square values (r.m.s.) of the fluctuations in
 508 the velocity components, $(U_{rms}, V_{rms}, W_{rms}) = (\overline{U'U'}^{1/2}, \overline{V'V'}^{1/2}, \overline{W'W'}^{1/2})$ where the
 509 turbulent fluctuations are defined as $U'_i = U_i^+ - \bar{U}_i^+$; the intensity of the fluctuations,
 510 $(I_U, I_V, I_W) = (\frac{U_{rms}}{\bar{U}^+}, \frac{V_{rms}}{\bar{U}^+}, \frac{W_{rms}}{\bar{U}^+})$; the Reynolds shear stress, $\tau_{XY}^R = -\overline{U'V'}$; the viscous
 511 shear stress, $\tau_{XY}^V = \frac{1}{Re_{\tau(M)}} \frac{\partial \bar{U}^+}{\partial Y}$; and the production rate of the turbulent kinetic energy,

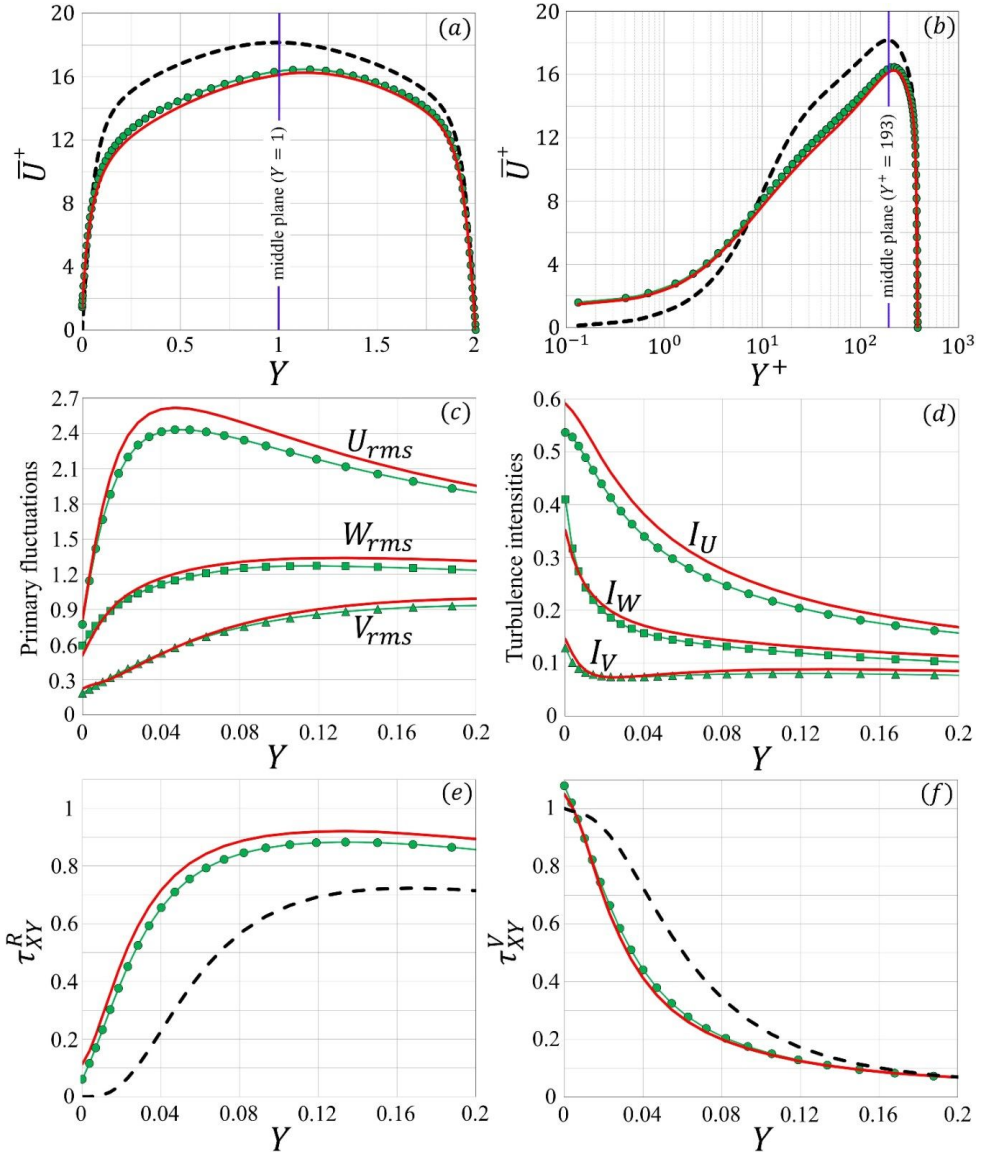


Figure 6: Turbulent channel flow ($Re_{\tau(\mathcal{M})} = 193$) over the porous substrate TC_{20} : predictions of the homogenized model, indicated by green lines with filled symbols, for (a, b) the mean velocity profile across the channel and for the near-interface distributions of (c) the root-mean-squares of the turbulent fluctuations in the three velocity components, (d) the turbulence intensities, and (e, f) the Reynolds/viscous shear stresses are validated against results of the full simulation (red lines). The dashed black profiles refer to the corresponding smooth, impermeable channel case.

512 $P_T = \frac{-1}{Re_{\tau(\mathcal{M})}} \overline{U'_i U'_j} \frac{\partial \overline{U}_i^+}{\partial X_j}$. While figure 6 focuses on the validation of the present model
 513 with the effective boundary conditions of the three velocity components imposed at $Y = 0$,
 514 figure 7 shows, in addition, the corresponding macroscopic results when the interface-normal
 515 velocity component is suppressed (i.e., $V|_{Y=0} = 0$) and only the in-plane slip velocities are

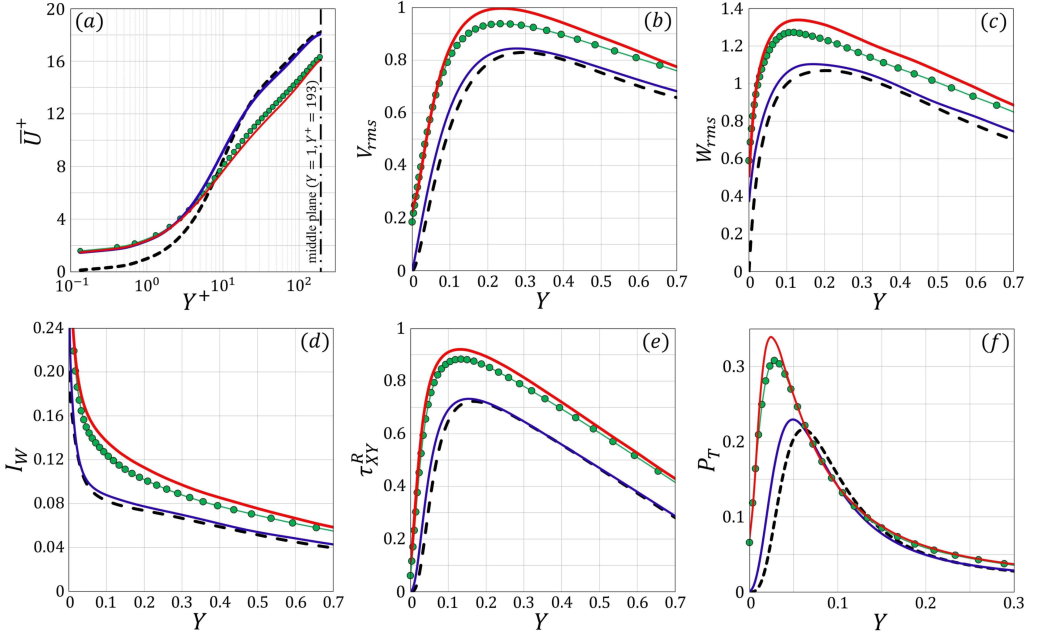


Figure 7: Distribution of the mean velocity (a) and behaviors of quantities of interest related to turbulence statistics (b–f) over the porous substrate TC_{20} : predictions of the homogenized simulation when the effective boundary conditions of the three velocity components are imposed (green lines with filled circles) or when transpiration is neglected (blue lines) are validated against results of the fine-grained simulation (red lines), while the dashed profiles are related to the smooth, impermeable channel case.

516 applied; this is important since it highlights the need of accounting for transpiration at the
 517 virtual boundary (Gómez-de-Segura *et al.* 2018a; Bottaro 2019; Lācis *et al.* 2020).

518 From inspection of figure 6, it is clear that the model captures well the trends of the mean
 519 velocity and the turbulence statistics displayed. The velocity profile can be analyzed in terms
 520 of the slip velocity, $U_{slip}^+ = \overline{U}^+|_{Y=0}$; the shift in the intercept of the logarithmic velocity profile,
 521 ΔU^+ (taking the smooth channel case as a reference for the measurement and averaging the
 522 shift over the region $30 \lesssim Y^+ \lesssim 120$ (Ahmed *et al.* 2022b)); the percentage change in
 523 the bulk (channel-averaged) velocity through the free-fluid region, $\Delta U_{ch}^+ \%$ (taking the bulk
 524 velocity in a fully smooth channel, $U_{ch}^+ \approx 15.69$, as a reference); and the corresponding
 525 percentage change in skin-friction coefficient, $\Delta C_f \%$ (taking the smooth-channel value,
 526 $C_f = 2/(U_{ch}^+)^2 \approx 0.00813$, as a reference). The analysis performed here shows that, for
 527 the turbulent flow over the perturbed boundaries considered, the log-law is still valid (over
 528 $30 \lesssim Y^+ \lesssim 120$), yet it is shifted (relative to that for a smooth wall) by ΔU^+ such that the
 529 logarithmic profile reads

$$530 \quad \overline{U}^+ = \frac{1}{\kappa} \ln(Y^+) + B + \Delta U^+, \quad (3.1)$$

531 where κ is the von Kármán constant and B is the intercept of the logarithmic profile for the
 532 flow over a corresponding smooth wall. Based on (3.1), if $\Delta U^+ < 0$ (respectively $\Delta U^+ > 0$),
 533 the logarithmic profile is shifted downwards (upwards), and in general the skin-friction drag
 534 increases (decreases); this is consistent with the definition of the roughness function, ΔU^+
 535 adopted by Gómez-de-Segura & García-Mayoral (2019), Ibrahim *et al.* (2021), and Khorasani
 536 *et al.* (2022, 2024), which differs in sign from that originally introduced by Hama (1954) and

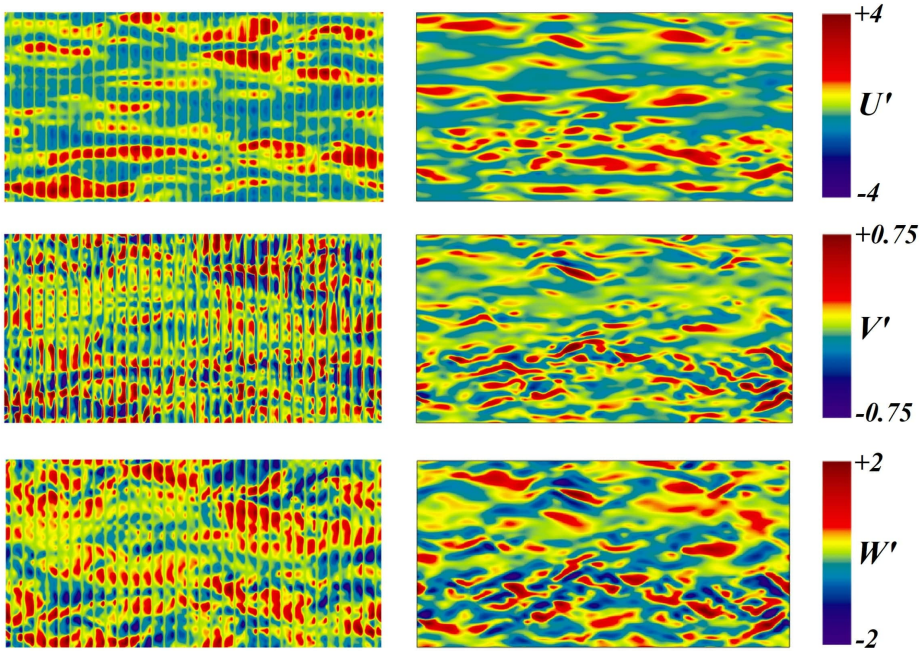


Figure 8: From the top, instantaneous distributions of U' , V' and W' at the porous/free-fluid interface ($Y = 0$) for case TC_{20} . The fully resolved results (left column) are compared with the homogenized ones (right column).

537 Clauser (1954). According to (3.1), $\Delta U^+ < 0$ is generally accompanied by $\Delta U_{ch}^+ \% < 0$ and
 538 $\Delta C_f \% > 0$. The full feature-resolving simulation for the case chosen for validation (TC_{20})
 539 yields $(U_{slip}^+, \Delta U^+, \Delta U_{ch}^+ \%, \Delta C_f \%) \approx (1.37, -2.76, -12.2\%, +29.6\%)$, while the values
 540 obtained from the model are respectively $(1.44, -2.33, -10.3\%, +24.4\%)$; a decrease in flow
 541 rate and, therefore, an increase in skin-friction coefficient is realized in both simulations.
 542 Moreover, the model predictions for the r.m.s. fluctuations of the velocity components at
 543 the fictitious interface ($Y = 0$) match well the results of the full simulation and deviate
 544 significantly from zero. In general, the accuracy of the macroscopic model is reasonable
 545 taking into account that the value of $\epsilon = 0.2$ ($\ell^+ \approx 40$) related to the porous substrate chosen
 546 for validation (TC_{20}) is rather large, meaning that microscopic and macroscopic length scales
 547 do not differ widely. On the other hand, it is obvious from figure 7 that the comparison with
 548 the fine-grained simulation is not satisfactory when the transpiration-free model is applied,
 549 where the mechanism of drag increase is idle, ΔU^+ is close to 0, and the trend of the turbulence
 550 statistics next to the fictitious boundary is similar to that of a smooth, impermeable channel
 551 (cf. Ibrahim *et al.* (2021)). A third, important, scenario is presented later in Section 4, where
 552 the transpiration velocity boundary condition is imposed while \mathcal{K}_{yy} is set to zero, for the
 553 porous substrate to be modeled as a rough, impermeable wall. The discussion there centers
 554 around the evaluation of \mathcal{K}_{yy} for a porous bed which is bounded from the bottom, and on
 555 how the accuracy of the model is affected by neglecting the medium permeability of a deep,
 556 yet finite, substrate such as the one considered here for validation (figure 5).

557 Finally, figure 8 displays a comparison between the results of the full texture-resolving
 558 simulation and the homogenized one, concerning the fluctuating patterns of the three velocity
 559 components at the porous/free-fluid interface. This figure is added following one referee's
 560 advice, with the purpose of providing the readers with the information needed to assess on

Table 2: Values of the macroscopic coefficients characterizing the different configurations considered for the porous substrate, estimated in wall units with $Re_{\tau(\mathcal{M})} = 193$ and ϵ varied from 0.05 (subscript 5) to 0.2 (subscript 20). Major results are presented, with the normalization based on $u_{\tau(\mathcal{M})}$. Monitoring the progress of the mean bulk velocity U_{ch}^+ during 10 additional units of time, ΔU_{ch}^+ % is found to differ by $\pm 0.2\%$ at the most (and $\pm 0.07\%$ on average) from the final values reported in the table.

Substrate	ℓ^+	Model coefficients					Sample results			
		λ_x^+	λ_z^+	$\mathcal{K}_{xy}^{iff,+}$	$\mathcal{K}_{zy}^{iff,+}$	\mathcal{K}_{yy}^+	U_{slip}^+	ΔU^+	ΔU_{ch}^+ %	ΔC_f %
Smooth	0	0	0	0	0	0	0	0	0	0
TC_5	9.7	0.43	0.64	0.20	0.49	0.17	0.43	-0.33	-1.1%	+2.1%
TC_{10}	19.3	0.79	1.14	0.67	1.57	0.68	0.83	-0.77	-3.2%	+6.7%
TC_{15}	29.0	1.07	1.46	1.20	2.57	1.53	1.14	-1.55	-6.4%	+14.2%
TC_{20}	38.6	1.30	1.72	1.74	3.49	2.72	1.44	-2.33	-10.3%	+24.4%
LC_5	9.7	0.66	0.44	0.52	0.21	0.17	0.66	+0.15	+1.1%	-2.1%
LC_{10}	19.3	1.33	0.87	2.07	0.84	0.68	1.33	+0.08	+0.9%	-1.9%
LC_{15}	29.0	1.99	1.31	4.66	1.88	1.53	2.05	-0.54	-1.4%	+2.8%
LC_{20}	38.6	2.66	1.74	8.29	3.34	2.72	2.87	-1.63	-6.7%	+15.0%
TM_5	9.7	0.54	1.03	0.35	1.03	0.01	0.56	-0.61	-2.3%	+4.7%
TM_{10}	19.3	0.94	1.71	1.03	3.06	0.05	1.02	-1.38	-5.5%	+12.0%
TM_{15}	29.0	1.22	2.09	1.62	4.84	0.10	1.36	-2.09	-9.0%	+20.9%
TM_{20}	38.6	1.44	2.31	2.10	6.29	0.18	1.61	-2.56	-11.3%	+27.0%
LM_5	9.7	1.09	0.57	1.13	0.38	0.01	1.07	+0.33	+1.9%	-3.7%
LM_{10}	19.3	2.18	1.14	4.52	1.53	0.05	2.15	+0.45	+2.6%	-5.0%
LM_{15}	29.0	3.27	1.71	10.17	3.44	0.10	3.36	-0.33	-0.4%	+0.7%
LM_{20}	38.6	4.36	2.28	18.08	6.12	0.18	4.48	-0.94	-2.9%	+6.1%

561 their own how well the upscaled boundary conditions mimic the effect of the porous substrate
562 on the turbulence.

563

3.2. Case studies: results and discussion

564 Numerical simulations were run for the channel flow over the different porous substrates (TC ,
565 LC , TM , LM), with four values of ϵ tested for each ($\epsilon = 0.05, 0.1, 0.15, 0.2$). The macroscopic
566 model already validated was employed to study the sixteen problems under consideration,
567 with the Oseen-based upscaled coefficients contributing to the effective boundary conditions
568 available in table 1. The main results are presented and discussed below.

569 3.2.1. *Mean velocity and skin-friction drag*

570 In table 2, the pitch distance and the macroscopic coefficients for each porous pattern are
571 expressed in wall units based on the velocity scale $u_{\tau(\mathcal{M})}$; they are defined by

$$572 \quad \ell^+ = \frac{\rho u_{\tau(\mathcal{M})} \ell}{\mu} = \epsilon Re_{\tau(\mathcal{M})}, \quad (3.2a)$$

$$573 \quad \lambda_x^+ = \frac{\rho u_{\tau(\mathcal{M})} \hat{\lambda}_x}{\mu} = \epsilon Re_{\tau(\mathcal{M})} \lambda_x, \quad \lambda_z^+ = \epsilon Re_{\tau(\mathcal{M})} \lambda_z, \quad (3.2b)$$

$$576 \quad \mathcal{K}_{xy}^{itf,+} = \epsilon^2 Re_{\tau(\mathcal{M})}^2 \mathcal{K}_{xy}^{itf}, \quad \mathcal{K}_{zy}^{itf,+} = \epsilon^2 Re_{\tau(\mathcal{M})}^2 \mathcal{K}_{zy}^{itf}, \quad \mathcal{K}_{yy}^+ = \epsilon^2 Re_{\tau(\mathcal{M})}^2 \mathcal{K}_{yy}. \quad (3.2c)$$

577 Values of the major quantities related to the behavior of mean velocity through the free-fluid
578 region are also listed in the table (refer to the definitions in Section 3.1). The most significant
579 finding is that reduction of the skin-friction drag coefficient (negative values of $\Delta C_f\%$,
580 associated with positive ΔU^+ and ΔU_{ch}^+ %) is attainable only by the porous substrates formed
581 by longitudinal inclusions (*LC* and *LM*), those characterized by streamwise-preferential
582 slip lengths and interface permeabilities ($\lambda_x^+ > \lambda_z^+$, $\mathcal{K}_{xy}^{itf,+} > \mathcal{K}_{zy}^{itf,+}$). Such a favorable
583 influence (up to 5% reduction in C_f) takes place exclusively at relatively small values of ℓ^+ ,
584 a behavior similar to that found by Gómez-de-Segura & García-Mayoral (2019) for this kind
585 of permeable boundaries and analogous to that exhibited by riblets (Bechert & Bartenwerfer
586 1989; Garcia-Mayoral & Jiménez 2011; Endrikat *et al.* 2021a,b; Wong *et al.* 2024). On
587 the other hand, permeable beds consisting of transverse grains yield only drag increase,
588 and this becomes more pronounced with ℓ^+ . For comparison purposes, the results obtained
589 by normalizing results with the shear velocity of the bottom surface, $u_{\tau(\mathcal{B})}$, are given in
590 Appendix B.

591 The behavior of the sample quantities reported on the right-hand side of table 2 for the four
592 substrate configurations are graphically presented as function of the streamwise Navier-slip
593 lengths in figure 9. It is important to highlight the following features with reference to the
594 trends of the figure:

- 595 (i) As discussed in Section 2.4, the first-order term in the effective boundary condition
596 of the streamwise velocity yields a slip velocity at the permeable interface $U_{slip}^+ \approx$
597 $\lambda_x^+ \frac{\partial \bar{U}^+}{\partial Y^+} \Big|_{Y=0} \approx \lambda_x^+$. Figure 9(a) shows that this linear dependence fits well with the results
598 of the simulations, for the roughness amplitudes considered. Besides the omission of
599 the higher-order term, the small percentage errors (up to $\approx 11\%$ in absolute value) may
600 be attributed to the deviation of $\frac{\partial \bar{U}^+}{\partial Y^+} \Big|_{Y=0}$ from 1 because the parameters are expressed
601 in wall units based on $u_{\tau(\mathcal{M})}$, and not the permeable-interface shear velocity $u_{\tau(\mathcal{B})}$.
602 However, one can write $\frac{\partial \bar{U}^+}{\partial Y^+} \Big|_{Y=0} = \frac{\partial \bar{U}^{+(\mathcal{B})}}{\partial Y^{+(\mathcal{B})}} \Big|_{Y=0} \left[\frac{u_{\tau(\mathcal{B})}}{u_{\tau(\mathcal{M})}} \right]^2$, where $\frac{\partial \bar{U}^{+(\mathcal{B})}}{\partial Y^{+(\mathcal{B})}} \Big|_{Y=0} \approx 1$
603 (provided that the Reynolds stress at $Y = 0$ is much smaller than the viscous stress),
604 which results in the modified relation $U_{slip}^+ \approx \left[\frac{u_{\tau(\mathcal{B})}}{u_{\tau(\mathcal{M})}} \right]^2 \lambda_x^+$. This expression enhances
605 the predictions of the slip velocity (maximum error below 4%), yet it cannot be employed
606 *a priori*, since the values of the shear-velocity ratio (cf. table 3) are available only after
607 numerical simulations have been conducted.

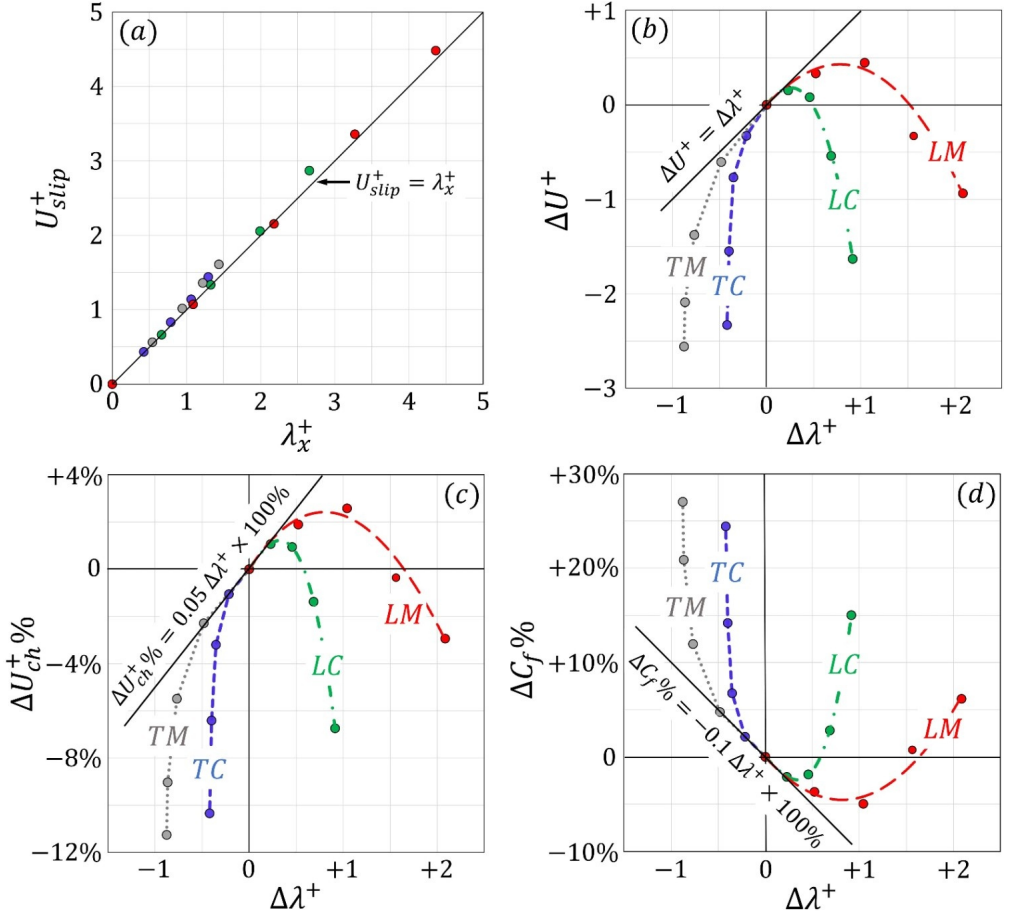


Figure 9: Dependence of (a) the slip velocity U_{slip}^+ on λ_x^+ and of (b) the shift of the logarithmic profile intercept ΔU^+ , (c) the percentage change in the bulk mean velocity $\Delta U_{ch}^+ \%$, and (d) the percentage change in the skin-friction coefficient $\Delta C_f \%$ on $\Delta \lambda^+ = \lambda_x^+ - \lambda_z^+$, for turbulent channel flows ($Re_{\tau(M)} = 193$) over the four types of permeable beds under study; cf. table 2. Simple linear relations fitting the behavior of U_{slip}^+ with λ_x^+ and the performance of the other quantities at small values of $\Delta \lambda^+$ are presented.

608 (ii) It has been found convenient to express the roughness function as the difference
 609 between the shifts of the virtual origins of mean and turbulent flows, i.e. $\Delta U^+ \approx \ell_U^+ -$
 610 ℓ_{Turb}^+ . (Ibrahim *et al.* 2021). For small protrusion heights, Luchini *et al.* (1991)
 611 have shown that ΔU^+ takes the form $\Delta U^+ = \lambda_x^+ - \lambda_z^+ = \Delta \lambda^+$; in the present settings, this
 612 assumption holds only up to $|\Delta \lambda^+| \lesssim 0.25$; cf. figure 9(b). Also Gómez-de-Segura *et al.*
 613 (2018b) plotted the roughness function against the difference between the displacements
 614 of the virtual origins, and they did it for a variety of complex surfaces (anisotropic porous
 615 substrates, superhydrophobic surfaces, riblets, and canopies), highlighting a behavior
 616 (figure 5 in their paper) qualitatively similar to that displayed in figure 9(b).

617 (iii) As far as the trends of $\Delta C_f \% = \frac{C_f - C_{f,smooth}}{C_{f,smooth}} \times 100\%$ are concerned, the

618 classical linearized relation $\Delta C_f\% = \frac{-\Delta U^+}{(2C_{f,smooth})^{-0.5} + (2\kappa)^{-1}} \times 100\%$ is expected
 619 to align well with the results for small changes in C_f (Luchini 1996; Bechert *et al.*
 620 1997). With $\Delta U^+ = \Delta\lambda^+$, $C_{f,smooth} = 0.00813$, and the von Kármán constant $\kappa = 0.4$,
 621 the linear dependence $\Delta C_f\% \approx -0.1 \Delta\lambda^+ \times 100\%$ is valid provided that $|\Delta\lambda^+|$ remains
 622 sufficiently small, as confirmed in figure 9(d). Under the same condition, it can be shown
 623 that $\Delta U_{ch}^+\% \approx -0.5 \Delta C_f\% \approx +0.05 \Delta\lambda^+ \times 100\%$, which fits well the results in figure
 624 9(c).

625 (iv) It is notable that, at any fixed value of $\Delta\lambda^+$, the porous substrates *LM* and *TM*
 626 outperform the configurations *LC* and *TC* in terms of either maximizing the drag
 627 reduction or minimizing the drag increase. One possible justification is that the permeable
 628 beds constructed with modified cylinders (*LM* and *TM*) exhibit much smaller values of
 629 the medium permeability \mathcal{K}_{yy}^+ compared to those designed based on flat cylinders (*LC*
 630 and *TC*), as can be realized from table 2. This favorable feature enhances ΔU^+ by
 631 attenuating the transpiration velocity at the fictitious interface ($Y = 0$), an effect which
 632 can be perceived as a mitigation of the blowing and suction events. The influence of
 633 transpiration on ΔU^+ will be discussed in further detail in Section 3.3.

634 In figure 10, the different results are plotted against the pitch distance, ℓ^+ . With regard to
 635 the slip velocity, assuming the simple linear relation $U_{slip}^+ \approx \lambda_x^+ = \ell^+ \lambda_x$ and recalling the
 636 trends of λ_x from table 1, one can expect that U_{slip}^+ changes linearly with ℓ^+ for the porous
 637 beds *LC* and *LM* since λ_x is independent of ℓ^+ for these streamwise-elongated patterns, in
 638 contrast to the spanwise-elongated patterns *TC* and *TM* for which the coefficient λ_x decreases
 639 with the increase of ℓ^+ on account of near-interface advection. These expectations agree with
 640 the behaviors displayed in figure 10(a). For small ℓ^+ values, the quantities ΔU^+ , $\Delta U_{ch}^+\%$,
 641 and $\Delta C_f\%$ are directly proportional to $\Delta\lambda^+ = \ell^+ \Delta\lambda$ (Luchini 1996), where $\Delta\lambda$ is equal
 642 to $\lambda_x - \lambda_z$. Table 1 implies that $\Delta\lambda|_{LM} > \Delta\lambda|_{LC} > \Delta\lambda|_{TC} > \Delta\lambda|_{TM}$ with the first two
 643 positive and the last two negative. For a small value of ℓ^+ , one should therefore expect
 644 $\Delta U^+|_{LM} > \Delta U^+|_{LC} > \Delta U^+|_{TC} > \Delta U^+|_{TM}$ (and likewise for $\Delta U_{ch}^+\%$ and $-\Delta C_f\%$) with
 645 the substrate *LM* yielding the maximum drag reduction and *TM* resulting in the maximum
 646 drag increase; cf. figure 10(b–d). Departing from the viscous regime, it is found that the
 647 drag reduction attainable by *LM* and *LC* peaks at some value of ℓ^+ between 10 and 20. The
 648 performance of these porous substrates then degrades, yet drag reduction is still achievable
 649 until a threshold within $20 \lesssim \ell^+ \lesssim 30$ is reached, beyond which drag increase takes place.
 650 Gómez-de-Segura *et al.* (2018a) studied highly connected porous media with streamwise-
 651 preferential permeability and attributed the aforementioned behavior to the formation of drag-
 652 increasing spanwise-coherent rollers associated with a Kelvin-Helmholtz-like instability
 653 whose initiation is governed by the intrinsic permeability component \mathcal{K}_{yy}^+ of the medium.
 654 Finally, we should not forget that all results plotted in figures 9 and 10 are obtained via
 655 homogenization-based DNSs. The accuracy of the trends displayed is thus dependent on the
 656 accuracy of the upscaling approach for each of the cases considered (in this respect, one may
 657 want to go back to the validation conducted considering the pattern *TC*₂₀ in Section 3.1).

658 3.2.2. The mechanism of drag increase/reduction

659 The influence of porous substrates on the near-interface turbulence is considered next. For
 660 sufficiently small values of ℓ^+ , the wall texture alters the structure of turbulence merely by
 661 shifting down its virtual origin by a distance $\ell_{Turb}^+ \approx \lambda_z^+$, whereas the effect is much more
 662 complicated beyond the viscous regime, especially with the increase in transpiration velocity.
 663 It is therefore useful to present and discuss some turbulence statistics of interest for the channel

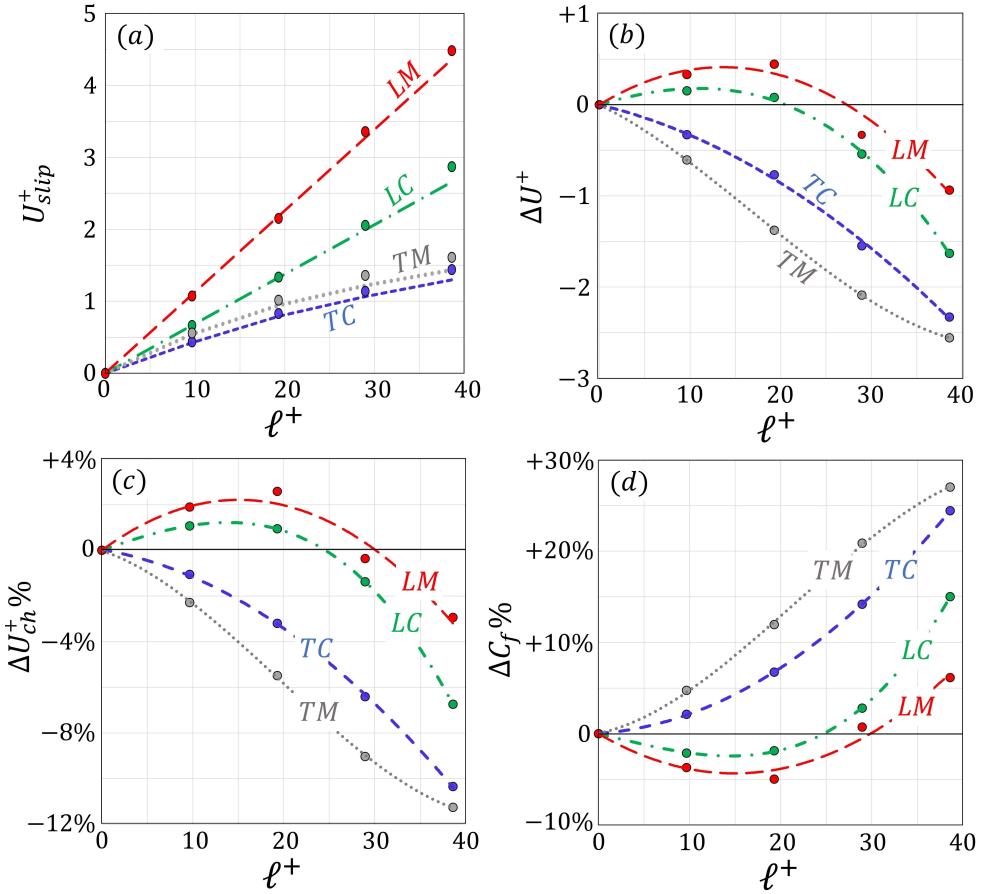


Figure 10: Dependence of major quantities characterizing the turbulent channel flow over the porous substrates under study on the pitch distance of the inclusions measured in wall units, $\ell^+ = \epsilon Re_{\tau(M)}$. Results of the homogenization-based DNSs are plotted with filled circles. The lines in panel (a) represent the simple relation $U_{slip}^+ = \ell^+ \lambda_x$, while those in the other panels are simple fitting curves.

664 flow over selected porous beds of relatively large grain spacings/sizes (LM_{10} : longitudinal
665 modified inclusions, $\ell^+ \approx 20$, the maximum drag reduction reported; LM_{20} : longitudinal
666 modified inclusions, $\ell^+ \approx 40$, drag increase; TM_{10} : transverse modified inclusions, $\ell^+ \approx 20$,
667 drag increase; TM_{20} : transverse modified inclusions, $\ell^+ \approx 40$, the maximum drag increase
668 reported). The velocity profiles are plotted in figure 11(a). The turbulence-characterizing
669 quantities plotted in figure 11(b) are chosen since, as shown by Ahmed *et al.* (2022b), their
670 behaviors near the porous/free-fluid interface can be linked to the favorable/adverse effects
671 of the permeable boundaries on friction drag. With focus on the peak values of V_{rms} , W_{rms} ,
672 τ_{XY}^R , and P_T , and the distributions of I_W , it can be realized that the drag-reducing substrate
673 (LM_{10}) yields results comparable to those in the reference case of turbulence over a smooth,
674 impermeable wall; this applies also to the other drag-reducing patterns not considered in the
675 figure, i.e. LM_5 , LC_5 , LC_{10} . Conversely, the drag-increasing ones result in intensified levels
676 of these quantities. For instance, with TM_{20} , the peak values V_{rms} , τ_{XY}^R , and P_T are larger
677 than the values in a smooth channel by about 16%, 24%, and 50%, respectively. The values
678 of the quantities at the fictitious interface, $Y = 0$, are of particular interest in the present work

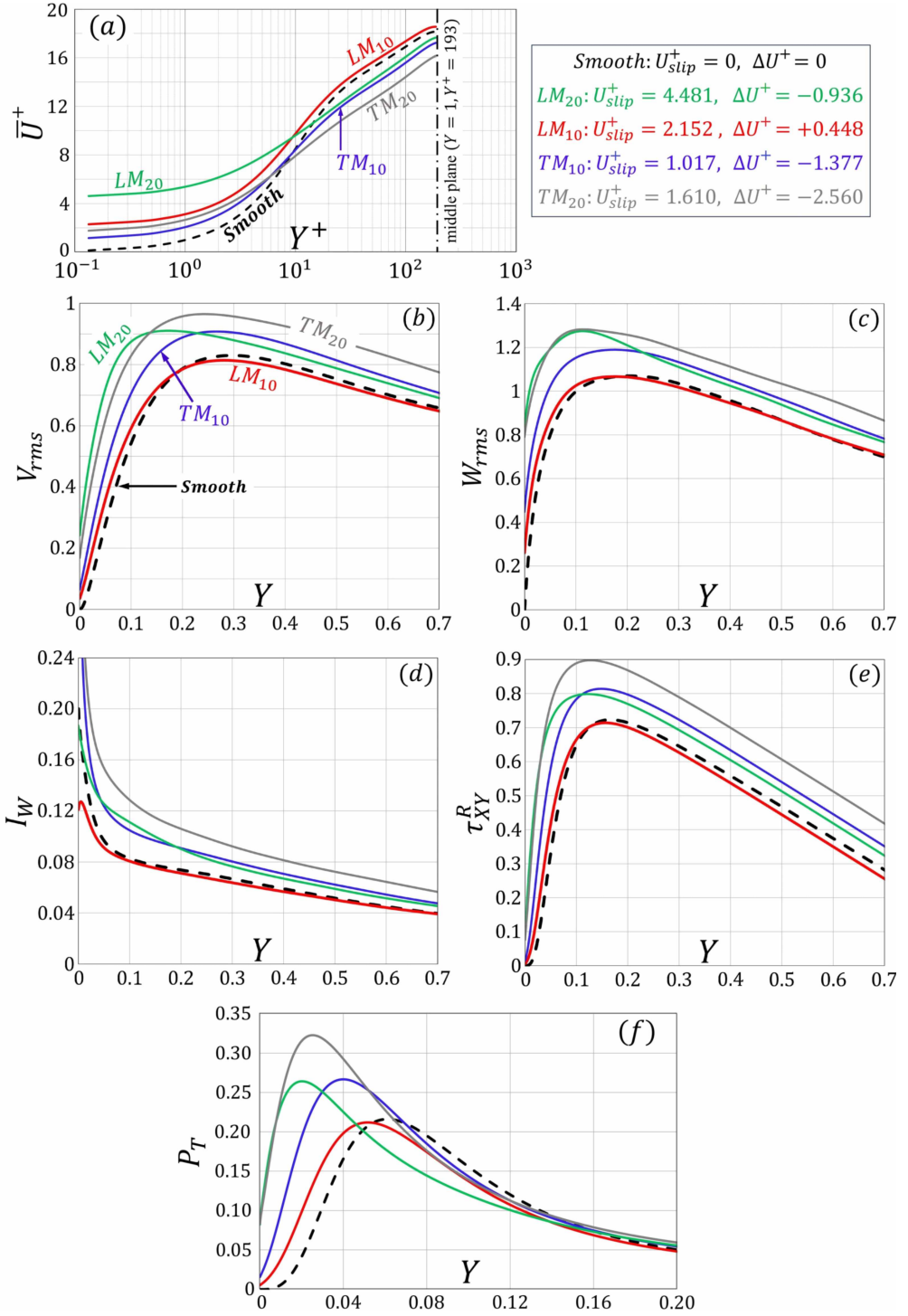


Figure 11: Predictions of the homogenization-based model for (a) the mean velocity profiles and (b-f) sample statistics for the channel flow ($Re_{\tau(\mathcal{M})} = 193$) over four different porous substrates.

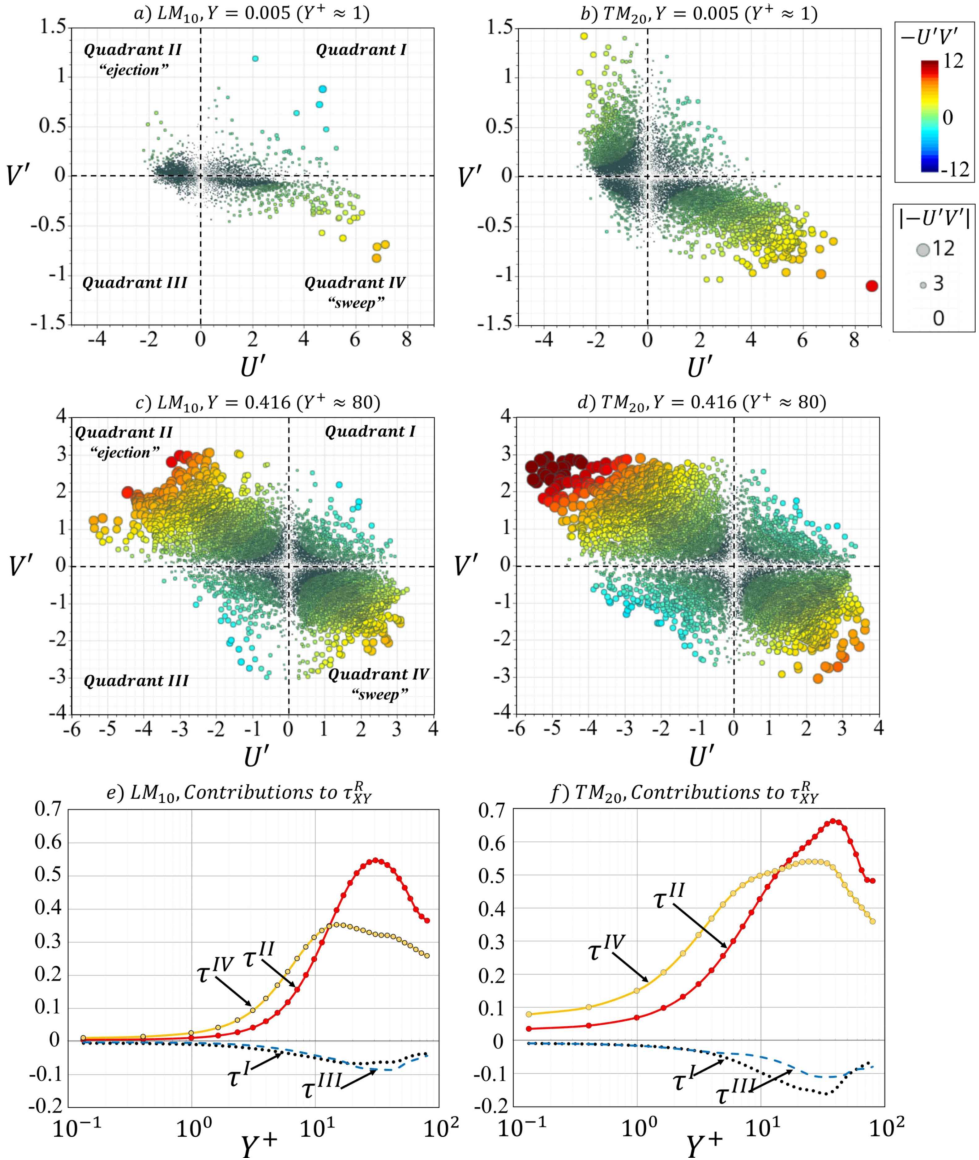


Figure 12: Quadrant analysis of the Reynolds shear stress, τ_{xy}^R , for turbulent channel flows ($Re_{\tau(\mathcal{M})} = 193$) over two different porous substrates (LM_{10} and TM_{20}). Instantaneous values of (U', V') throughout the planes at $Y = 0.005$ and $Y = 0.416$ (evaluated at all grid points) are shown in panels (a) to (d), while contributions to τ_{xy}^R from each quadrant are plotted in the bottom frames against $Y^+ = YRe_{\tau(\mathcal{M})}$ up to the centerline of the channel.

679 and their correlations with ΔU^+ are explored in Section 3.3; it is evident from the figure that
 680 significant values of V_{rms} are obtained at the plane $Y = 0$, in particular when ℓ^+ is sufficiently
 681 large, an important effect (Jiménez *et al.* 2001; Orlandi *et al.* 2003, 2006; Orlandi & Leonardi
 682 2006, 2008) which would obviously be absent if transpiration were unaccounted for in the
 683 formulation of the model.

684 The quadrant analysis in figure 12 reveals details of the generation of the Reynolds stress,
 685 τ_{xy}^R , from the turbulent events taking place in the flow near the substrates LM_{10} and TM_{20} . In

686 figure 12, the instantaneous distributions of (U', V') are displayed over the plane at $Y^+ \approx 1$,
 687 directly adjacent to the substrate-channel interface, and the plane at $Y^+ \approx 80$, well above the
 688 substrate. The phenomena can be classified into negative-production events (first and third
 689 quadrants, with $-U'V' < 0$) and positive-production ones (second and fourth quadrants,
 690 with $-U'V' > 0$); refer to, for instance, Wallace *et al.* (1972). Eventually, the Reynolds stress
 691 generated from the sum of the positive contributions from the *ejection* (second quadrant,
 692 bursting of low-speed fluid) and the *sweep* (fourth quadrant, inrush of high-speed fluid)
 693 events at any Y^+ level is generally larger than that arising from the sum of the contributions
 694 of the other two quadrants. The production of turbulence is dominated by the sweep event
 695 in the close vicinity of the boundary (cf. figure 12(a, b)), while ejection is dominant away
 696 from the wall (cf. figure 12(c, d)). For a better understanding, the contributions from the four
 697 quadrants to the Reynolds shear stress at a given time instant, evaluated over different $X - Z$
 698 planes up to $Y^+ \approx 80$, are plotted in figure 12(e, f); they are obtained by integrating the values
 699 of $-U'V'$ related to each of the quadrants, separately, over the area occupied by the specific
 700 event and using the overall area of the $X - Z$ plane ($= 2\pi \times \pi$) as a weight. It is notable that
 701 ejection becomes dominant beyond a threshold within $Y^+ = 12-15$. All the findings above
 702 agree qualitatively with the results by Kim *et al.* (1987) in a channel delimited by smooth,
 703 impermeable walls. From a quantitative perspective, the production of turbulence via both
 704 ejection and sweep is clearly intensified for case TM_{20} (the porous substrate of maximum
 705 drag increase) compared to the levels with LM_{10} (the substrate of largest drag reduction), at
 706 all the values of Y^+ considered.

707 In addition to the material presented in this section, it is beneficial to provide, via
 708 visualizations, some qualitative insights into the effects of the surface texture on the coherent
 709 structures (e.g., the pattern of streaks) and the turbulent events occurring in the inner region
 710 of the boundary layer; this is available in the *Supplemental Movie* published online alongside
 711 this article. It might also be of interest, for future research focussed on the flow physics, to
 712 explore how different substrate topologies affect the spectral density of the Reynolds stress
 713 and the premultiplied spectra of the velocity components next to the interface. This would
 714 probably need also a more extensive comparison between texture-resolving and modelled
 715 simulations, considering a large variety of porous microstructures. For these reasons, in the
 716 present contribution we prefer to address attention to the relation between the roughness
 717 function and the upscaled coefficients of the model.

718 3.3. In pursuit of a correlation for ΔU^+ over porous/textured walls

719 We proceed from the earlier discussion on figure 11, concerning how the near-wall distri-
 720 butions of some turbulence-characterizing parameters can control the mechanism of drag
 721 reduction/increase over the permeable boundaries, to explore the correlation between the
 722 roughness function ΔU^+ and the fictitious-interface values of quantities of particular interest:
 723 $\tilde{V}_{rms} = V_{rms}|_{Y=0}$, $\tilde{W}_{rms} = W_{rms}|_{Y=0}$, and $\tilde{\tau}_{XY}^R = \tau_{XY}^R|_{Y=0}$. Figure 13(a-c) reveals that
 724 the dependence of ΔU^+ on \tilde{V}_{rms} cannot be described by a universal function valid for all
 725 permeable boundaries; the same can be said for \tilde{W}_{rms} and $\tilde{\tau}_{XY}^R$. Conversely, each configuration
 726 yields a unique relationship, and even the general trends differ when porous substrates of
 727 streamwise-preferential permeability (LC and LM , non-monotonic behavior) are compared
 728 with those consisting of spanwise-elongated grains (TC and TM , strictly monotonic decrease).
 729 To explain this, let us assume conditions corresponding to a small value of \tilde{V}_{rms} fixed for
 730 the four patterns (e.g., $\tilde{V}_{rms} = 0.01$) and analyze the resulting ΔU^+ . While a fixed value of
 731 \tilde{V}_{rms} may imply that, for all the boundaries, the virtual origin of turbulence has the same
 732 shift from the $Y = 0$ plane (i.e., constant ℓ_{Turb}^+), the position of the virtual origin of the
 733 mean flow, $\ell_U^+ \approx \lambda_x^+$, can significantly differ according to the value of the streamwise Navier-

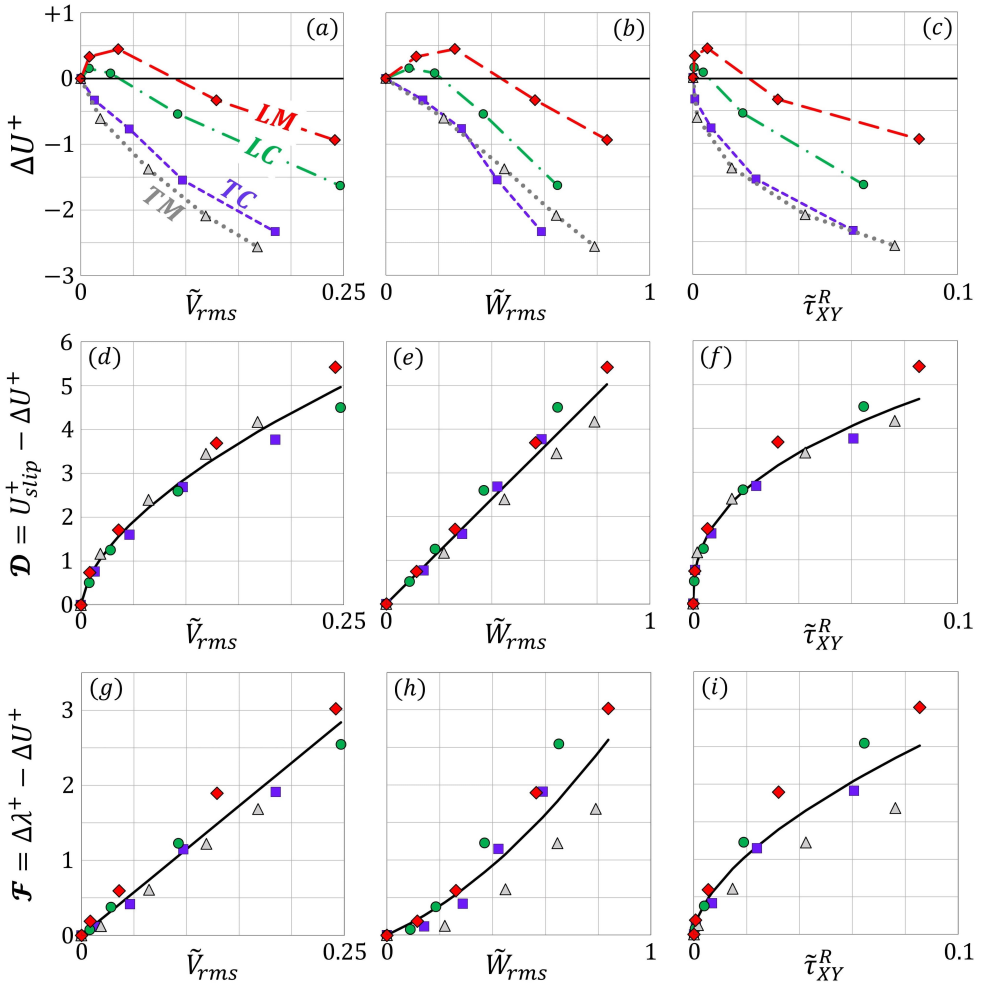


Figure 13: Dependence of ΔU^+ (top panels) and the related quantities \mathcal{D} (middle panels) and \mathcal{F} (bottom panels) on turbulence-characterizing parameters of interest measured at the fictitious interface (at $Y = 0$). The filled symbols indicate results of the homogenized simulations for turbulent flow over the four substrate configurations under study (cf. figure 2), with ℓ^+ varied for each pattern as described in Table 2, while the fitting relations (3.3–3.8) are plotted with solid lines in the middle and the bottom frames.

734 slip length, λ_x^+ , for each wall, and, consequently, different values of the roughness function
 735 $\Delta U^+ = \ell_U^+ - \ell_{Turb}^+$, are obtained. In the search of a function displaying a universal behavior,
 736 we follow two separate paths.

737 The first path relies on analyzing the mean velocity profile, $\bar{U}^+(Y^+)$, over each of the
 738 permeable substrates to monitor the upward shifts of the velocity at matched Y^+ values, taking
 739 the profile over a smooth, impermeable wall as a reference (for instance, cf. figure 11(a)).
 740 Such a velocity shift is, by definition, equal to U_{slip}^+ at $Y = 0$ and to ΔU^+ in the logarithmic
 741 region. Whether ΔU^+ is positive or negative, it is $U_{slip}^+ > \Delta U^+$ for all textured boundaries
 742 (for $\ell^+ = 0$, the smooth, impermeable wall is retrieved, and the limit $U_{slip}^+ = \Delta U^+ = 0$
 743 is reached). The function $\mathcal{D} = U_{slip}^+ - \Delta U^+ \geq 0$ can therefore be defined to indicate the

744 depression in the velocity shift when moving from the wall to the logarithmic region; it is
 745 plotted against the turbulence parameters in figure 13(d-f).

746 In the second path, we proceed from the fact that the approximation $\Delta U^+ = \Delta \lambda^+$ holds only
 747 for small surface roughness, while a further reduction in the value of the roughness function
 748 occurs with the increase of ℓ^+ , i.e. $\Delta U^+ = \Delta \lambda^+ - \mathcal{F}$, with the newly defined function $\mathcal{F} \geq 0$.
 749 The behavior of \mathcal{F} is shown in figure 13(g-i).

750 Both functions \mathcal{D} and \mathcal{F} increase monotonically with each of \tilde{V}_{rms} , \tilde{W}_{rms} , and $\tilde{\tau}_{XY}^R$, and
 751 it can be realized from figure 13(d-i) that, even from a quantitative point of view, general
 752 trends emerge. Eventually, the following fitting relationships can be proposed (together with
 753 their accuracy levels):

$$754 \quad \mathcal{D} = 11.5 \times [\tilde{V}_{rms}]^{0.6}, \quad NRMS_{error} \approx 11\%, \quad (3.3)$$

$$755 \quad \mathcal{D} = 6 \times \tilde{W}_{rms}, \quad NRMS_{error} \approx 13\%, \quad (3.4)$$

$$756 \quad \mathcal{D} = 12.5 \times [\tilde{\tau}_{XY}^R]^{0.4}, \quad NRMS_{error} \approx 11\%, \quad (3.5)$$

$$758 \quad \mathcal{F} = 11.5 \times \tilde{V}_{rms}, \quad NRMS_{error} \approx 18\%, \quad (3.6)$$

$$760 \quad \mathcal{F} = 1.8 \times [\tilde{W}_{rms}]^2 + 1.6 \times \tilde{W}_{rms}, \quad NRMS_{error} \approx 37\%, \quad (3.7)$$

$$762 \quad \mathcal{F} = 11 \times [\tilde{\tau}_{XY}^R]^{0.6}, \quad NRMS_{error} \approx 29\%, \quad (3.8)$$

763 where the normalized root-mean-square error, $NRMS_{error}$, is evaluated by dividing the
 764 conventional RMS_{error} by the mean value of either \mathcal{D} or \mathcal{F} . The ranges of validity of the
 765 relations proposed are

$$766 \quad 0 \leq \tilde{V}_{rms} \leq 0.25, \quad 0 \leq \tilde{W}_{rms} \leq 0.85, \quad 0 \leq \tilde{\tau}_{XY}^R \leq 0.085. \quad (3.9)$$

767 In the remainder of this section, we aim to demonstrate (i) that transpiration strongly controls
 768 the depression in the velocity shift over a wide range of textured boundaries and (ii) that
 769 correlating \tilde{V}_{rms} to the macroscopic coefficients of the homogenization model permits the
 770 use of (3.3) and (3.6) for an *a priori* estimate of the roughness-function-related parameters
 771 \mathcal{D} and \mathcal{F} .

772 [Orlandi et al. \(2003\)](#) demonstrated that the principal characteristics of the flow over a
 773 rough surface are closely related to the presence of wall-normal velocity distribution at the
 774 interface between the protrusions and the overlying turbulent boundary layer. A more formal
 775 description of this dependence has been proposed by [Orlandi et al. \(2006\)](#) and [Orlandi &
 776 Leonardi \(2006\)](#) who found good correlation between the quantity $\mathcal{D} = U_{slip}^+ - \Delta U^+$ and the
 777 r.m.s. fluctuations of the wall-normal velocity at the plane passing through the crests of the
 778 roughness elements. Later, [Orlandi & Leonardi \(2008\)](#) explored the relationship between \mathcal{D}
 779 and \tilde{V}_{rms} for walls with different textures, by collecting and plotting many results from the
 780 literature ([Cheng & Castro 2002](#); [Leonardi et al. 2003](#); [Orlandi & Leonardi 2006](#); [Burattini
 781 et al. 2008](#); [Flores & Jiménez 2006](#)) together with new ones related to the flow over surfaces
 782 roughened with longitudinal/transverse bars or various three-dimensional patterns. They
 783 concluded their study proposing the correlation $\mathcal{D} = \frac{B}{\kappa} \tilde{V}_{rms}$, with B and κ as by (3.1). Most
 784 of the data considered by [Orlandi & Leonardi \(2008\)](#) in addition to the recent results by [Hao
 785 & García-Mayoral \(2024\)](#) are presented in figure 14(a); the strong correlation between \mathcal{D}
 786 and \tilde{V}_{rms} is evident, and the linear relationship by [Orlandi & Leonardi \(2008\)](#), plotted with
 787 $B = 5.5$ and $\kappa = 0.4$ is found to perform well, where $NRMS_{error}$ is below 12%. Interestingly,
 788 good correlation between \mathcal{D} and \tilde{V}_{rms} can also be realized in figure 14(b) for the turbulent
 789 flow over permeable boundaries, based on the values reported by [Hao & García-Mayoral](#)

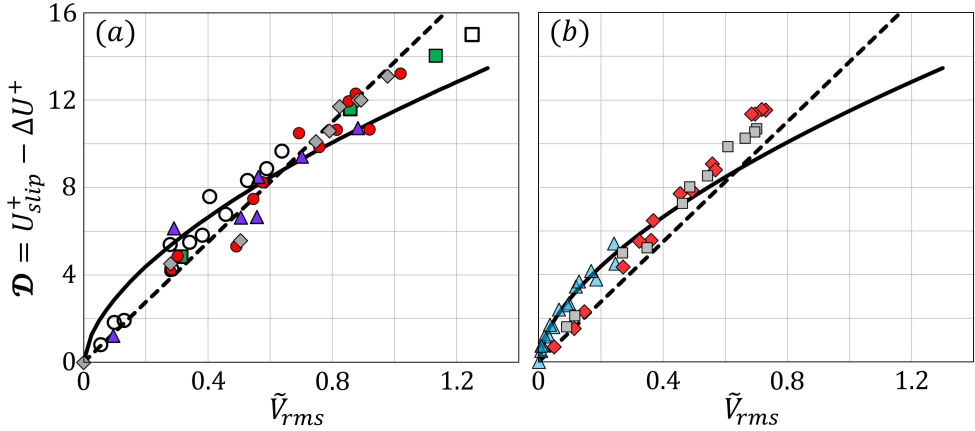


Figure 14: Values of the parameter \mathcal{D} plotted against the r.m.s. of the turbulent fluctuations in the wall-normal velocity at the plane $Y = 0$. In panel (a), results from the literature for channels roughened with streamwise-elongated, spanwise-elongated, or three-dimensional elements are shown: blank square, Cheng & Castro (2002); red circles, Leonardi *et al.* (2003); purple triangles, Orlandi & Leonardi (2006); green squares, Burattini *et al.* (2008); gray diamonds, Orlandi & Leonardi (2008); blank circles, Hao & García-Mayoral (2024). In panel (b), the results of Hao & García-Mayoral (2024) for symmetric channels bounded by either deep (red diamonds) or shallow (gray squares) porous substrates are plotted, together with the values of the present homogenization-based simulations (light-blue triangles). Solid lines refer to correlation (3.3), while the linear relationship by Orlandi & Leonardi (2008) is plotted with dashed lines.

(2024) plotted next to the results of the present macroscopic DNSs; the $NRMS_{error}$ for Orlandi-Leonardi relationship is about 23%. With regard to the present correlation (3.3), the deviations are comparable to those reported above, with $NRMS_{error} \approx 14\%$ for the rough walls and $\approx 18\%$ for the porous boundaries, even for values of \tilde{V}_{rms} much larger than the validity limit (3.9) of our simulations. Figure 14 thus confirms that \tilde{V}_{rms} is a key parameter which controls the roughness function in the turbulent flow over rough/porous boundaries and that (3.3) performs well even for quite large values of \tilde{V}_{rms} . The major difficulty in putting (3.3), or Orlandi-Leonardi correlation, to practical use is that \tilde{V}_{rms} is not available until a full simulation of the turbulent flow above a textured wall is conducted.

The crux of the matter is thus the search of a simplified expression for \tilde{V}_{rms} , as function of the macroscopic coefficients which permit to describe the near wall flow. After some efforts, we have found that the parameter Ψ defined as

$$\Psi = \left(\frac{\mathcal{K}_{xy}^{itf,+}}{\lambda_x^+} + \frac{\mathcal{K}_{zy}^{itf,+}}{\lambda_z^+} + \sqrt{\mathcal{K}_{yy}^+} \right) \left(\frac{\lambda_z^+}{\lambda_x^+} \right)^{0.25} \quad (3.10)$$

is well correlated to \tilde{V}_{rms} , as shown in figure 15. It is worth highlighting that (3.10) is based on the coefficients present in the boundary condition for the transpiration velocity (2.19b): the

parameters $\frac{\mathcal{K}_{xy}^{itf,+}}{\lambda_x^+}$ and $\frac{\mathcal{K}_{zy}^{itf,+}}{\lambda_z^+}$ appear when the streamwise/spanwise Navier-slip conditions

$\left(\frac{\partial \hat{u}}{\partial \hat{y}} + \frac{\partial \hat{v}}{\partial \hat{x}} \right) \Big|_0 = \frac{\hat{u}|_0}{\lambda_x}$ and $\left(\frac{\partial \hat{w}}{\partial \hat{y}} + \frac{\partial \hat{v}}{\partial \hat{z}} \right) \Big|_0 = \frac{\hat{w}|_0}{\lambda_z}$ are substituted into the second and the third

terms on the right hand side of (2.19b) and the equation is recast in wall units, while $\sqrt{\mathcal{K}_{yy}^+}$

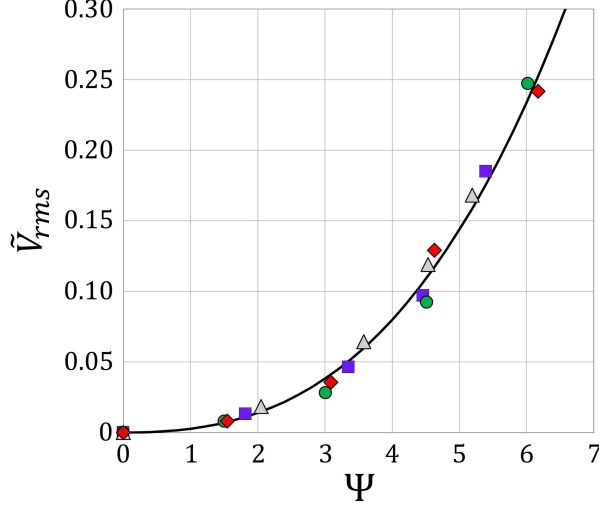


Figure 15: The r.m.s. of turbulent fluctuations in the transpiration velocity at $Y = 0$, plotted against the compound macroscopic parameter Ψ for the different porous patterns considered (same symbols as in figure 13). The solid line represents a third-order polynomial fitting.

810 quantifies the role of the intrinsic permeability for porous boundaries. The presence of $\frac{\lambda_z^+}{\lambda_x^+}$
 811 in (3.10) permits to differentiate walls with spanwise-preferential slip ($\lambda_z^+ > \lambda_x^+$) from those
 812 exhibiting preferential streamwise slip ($\lambda_x^+ > \lambda_z^+$), and implies that, for the same values of
 813 $\frac{\mathcal{K}_{xy}^{itf,+}}{\lambda_x^+}$, $\frac{\mathcal{K}_{zy}^{itf,+}}{\lambda_z^+}$, and $\sqrt{\mathcal{K}_{yy}^+}$, relatively stronger transpiration is associated with the former
 814 wall patterns (e.g. substrates with transverse inclusions). Based on the data plotted in figure
 815 15, we can propose the fitting equation

$$816 \quad \tilde{V}_{rms} = 0.00075 \Psi^3 + 0.002 \Psi^2, \quad (3.11)$$

817 for which the $NRMS_{error}$ is less than 10%. Substituting (3.11) into (3.3) and (3.6), we finally
 818 obtain the following expressions for the roughness-function-related quantities:

$$819 \quad \mathcal{D} = U_{slip}^+ - \Delta U^+ = 11.5 \times \left(0.00075 \Psi^3 + 0.002 \Psi^2 \right)^{0.6}, \quad (3.12)$$

820

$$821 \quad \mathcal{F} = \Delta \lambda^+ - \Delta U^+ = 11.5 \times \left(0.00075 \Psi^3 + 0.002 \Psi^2 \right), \quad (3.13)$$

822 valid up to $\Psi \approx 6$. These expressions are plotted in figure 16 together with the results
 823 obtained from the homogenization-based DNSs conducted for the porous patterns TC , LC ,
 824 TM , and LM . Estimates of \mathcal{D} and \mathcal{F} for the turbulent flow over a perturbed wall of given
 825 microstructure and given value of $\ell^+ = \epsilon Re_{\tau(M)}$ are thus available provided (i) ℓ^+ is lower
 826 than about 40, and (ii) outer layer similarity is maintained.

827 As a side remark, we observe that the relations obtained in this section have been generated
 828 by fitting data that pertain to the turbulent flow in a channel with asymmetric boundaries,
 829 and all the quantities (mean streamwise velocity, turbulence statistics, and macroscopic
 830 coefficients) have been normalized with the macroscopic-pressure-gradient-based shear
 831 velocity, $u_{\tau(M)}$. Since different choices appear in the literature, we provide in Appendix

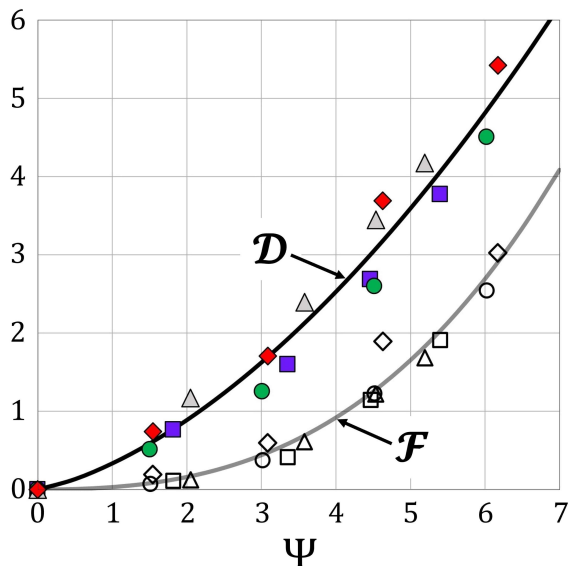


Figure 16: The roughness-function-related quantities \mathcal{D} and \mathcal{F} , plotted against the parameter Ψ for the different porous patterns considered (same symbols as in figure 13, filled for \mathcal{D} and empty for \mathcal{F}). Correlations (3.12) and (3.13) are plotted with solid lines.

832 **B** key quantities scaled with the total stress at the bottom wall. It is also shown that equations
 833 (3.12) and (3.13) remain reasonably accurate, independently of the choice of u_τ .

834

3.4. Can we make a-priori predictions?

835 It is useful to assess the accuracy of (3.12) and (3.13) for the turbulent flow over perturbed
 836 boundaries different from the porous ones based on which these correlations have been
 837 generated. In particular, we choose to check the generality of the relations above by validating
 838 them against existing numerical/experimental results for the motion over rough, impermeable
 839 walls ($\mathcal{K}_{yy} = 0$) with either two- or three-dimensional wall corrugations. The results in figure
 840 17 are related to the turbulent flow ($Re_{\tau(\mathcal{M})} = 182.70$) in a symmetric channel delimited by
 841 walls roughened with in-line patterns of cubical protrusions having side length e and pitch $\ell =$
 842 $2e$. The Oseen-based upscaled coefficients, sensitive to the level of near-interface advection
 843 and hence to the value of ℓ^+ , are evaluated for $\ell^+ = (0, 12, 23.9, 35.9, 47.8)$ and are plotted
 844 in figure 17(a). The corresponding values of Ψ are $(0, 2.84, 4.39, 5.78, 7.29)$, and are used to
 845 predict the behavior of the quantity \mathcal{D} in figure 17(b). These predictions are compared against
 846 the numerical results of the feature-resolving simulations by Hao & García-Mayoral (2024),
 847 and good agreement is observed. To highlight the need of incorporating near-wall advection
 848 into the homogenization model, the calculations have been repeated by setting Re_{slip} equal
 849 to 0 in (2.22) and (2.23), and significant errors in the predictions of \mathcal{D} are found when ℓ^+
 850 exceeds 10. In fact, the Stokes-based results coincide with the Oseen-based ones for $\ell^+ \lesssim 10$, a
 851 threshold similar to that reported by Ahmed & Bottaro (2024) for laminar channel flows. Since
 852 $\Delta U^+ = U_{slip}^+ - \mathcal{D}$, the calculation of the roughness function based on the values obtained for
 853 \mathcal{D} requires knowledge of the slip velocity, U_{slip}^+ . It may be tempting to use the approximation

854
$$U_{slip}^+ = \lambda_x^+ \left. \frac{\partial \bar{U}^+}{\partial Y^+} \right|_{Y=0} \approx \lambda_x^+,$$
 but care must be exerted, since significant errors appear in the
 855 predicted U_{slip}^+ as ℓ^+ becomes large, as a result of the large Reynolds stress generated at the
 856 channel virtual boundary in $Y = 0$ (Hao & García-Mayoral 2024). It is the approximation

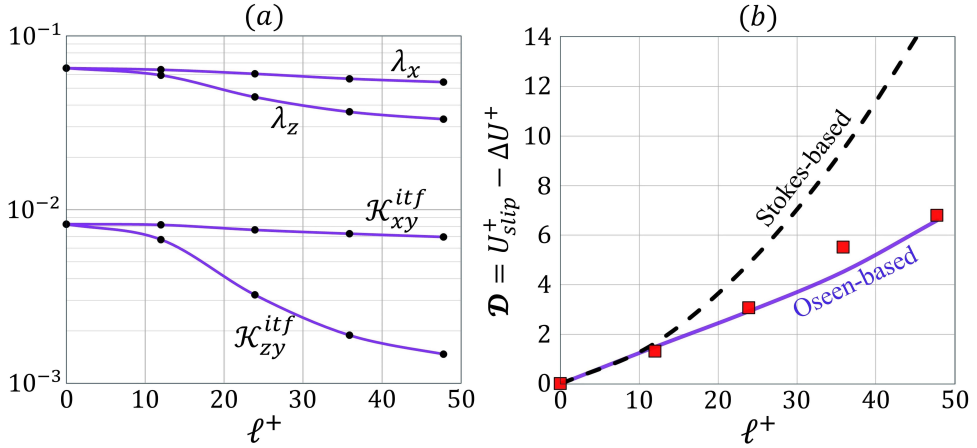


Figure 17: Turbulent flow ($Re_\tau \approx 180$) in a symmetric channel whose top/bottom boundaries are roughened with cubes (in-line arrangement) of size-to-pitch ratio $e/\ell = 0.5$, with the spacing in wall units, $\ell^+ = \epsilon Re_\tau(\mathcal{M})$, varied up to 50. Values of the macroscopic coefficients are plotted against ℓ^+ in panel (a). In panel (b), the behavior of the parameter \mathcal{D} based on (3.12) is shown (blue curve), and is validated against the results by Hao & García-Mayoral (2024) obtained from full simulations (squares). The black dashed curve refers to the predictions of (3.12) when Ψ is evaluated with the Stokes-based upscaled coefficients, neglecting near-wall inertia; they are $\lambda_x = \lambda_z \approx 0.0653$ and $\mathcal{K}_{xy}^{itf} \approx \mathcal{K}_{zy}^{itf} = 0.0083$.

857 $\left. \frac{\partial \overline{U}^+}{\partial Y^+} \right|_{Y=0} = 1$ which eventually breaks down. In fact, based on the values of U_{slip}^+ and λ_x^+
 858 reported by Hao & García-Mayoral (2024), we observe that the absolute deviations between
 859 the two quantities, for $\ell^+ = (12, 23.9, 35.9, 47.8)$, are respectively (1%, 4%, 28%, 53%). If
 860 we substitute $U_{slip}^+ = \lambda_x^+$ into (3.12), with the Oseen-based coefficients, we obtain $\Delta U^+ \approx$
 861 $(-0.73, -1.48, -2.49, -4.01)$, progressively deviating from the values computed by Hao &
 862 García-Mayoral (2024): $\Delta U^+ \approx (-0.50, -1.69, -3.77, -4.91)$.

863 The next case examined is that of riblets. Rather than explicitly using the expression
 864 recalled earlier, $\Delta U^+ = \ell_U^+ - \ell_{Turb.}^+$, which is not predictive unless turbulent simulations are
 865 conducted for any shape of the riblets (or a model allowing for a priori predictions of $\ell_{Turb.}^+$
 866 is formulated, e.g., the “viscous vortex model” by Wong *et al.* (2024)), we employ (3.13).
 867 Clearly, when Ψ is vanishingly small the relationship (3.13) yields the classical viscous
 868 approximation $\Delta U^+ = \Delta \lambda^+$ (Luchini 1996; García-Mayoral & Jiménez 2011). Conversely,
 869 the behavior of the roughness function can deviate significantly from this linear equation as ℓ^+
 870 increases and transpiration becomes more pronounced. Different ribletted surfaces are shown
 871 in figure 18. For each geometry, the macroscopic coefficients are calculated (Appendix C)
 872 and expressed in wall units by applying (3.2b) and (3.2c) for different spacings $\ell^+ = \epsilon Re_\tau(\mathcal{M})$
 873 within the range considered ($0 \leq \ell^+ \leq 36$); the values of Ψ are accordingly between 0 and
 874 7.4. The predictions in the form ΔU^+ versus ℓ^+ , plotted with blue solid lines, are validated
 875 against the DNS results by Wong *et al.* (2024) and the experimental findings by Bechert
 876 *et al.* (1997); a reasonably good agreement can be ascertained from the figure, including the
 877 deviation from the linear dependence departing from the viscous regime, the performance
 878 degradation when the pitch distance exceeds a threshold between 15 and 20, and eventually
 879 the drag increase for large riblets’ periodicity. For larger values of ℓ^+ , not considered in
 880 the figure, predictions of the correlation are questionable since the resulting values of Ψ
 881 are significantly beyond the applicability range of the present correlation. For instance, Gatti
 882 *et al.* (2020) studied the turbulent flow over trapezoidal riblets (similar to those in figure 18(d))

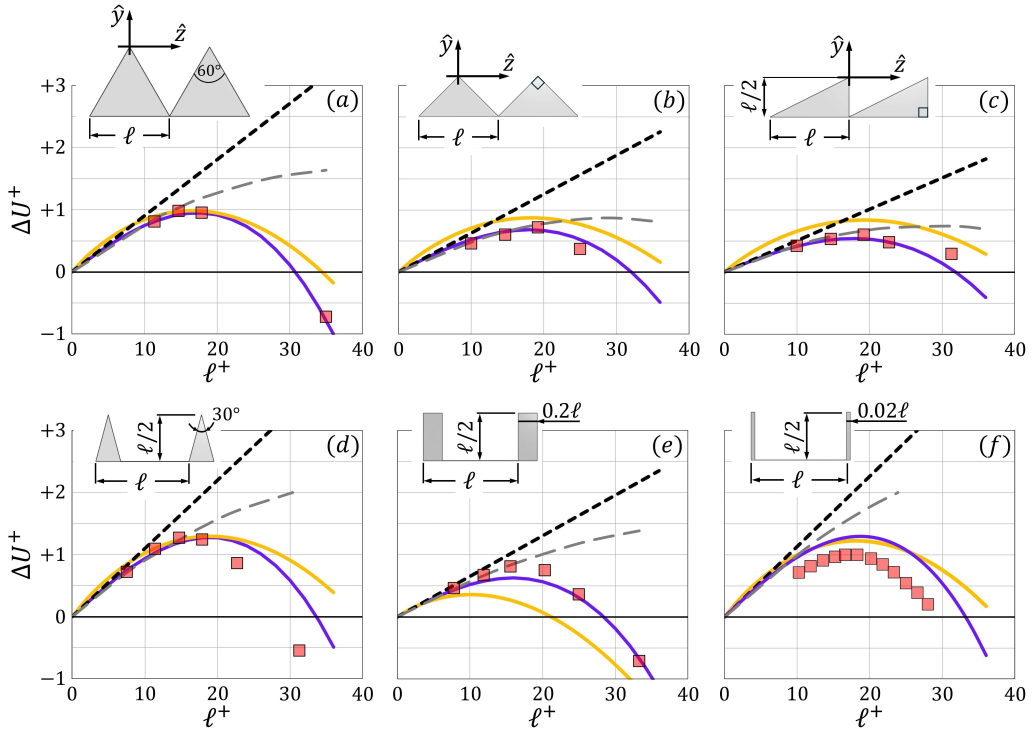


Figure 18: Behavior of ΔU^+ with the increase in ℓ^+ , for the turbulent flow over surfaces with different shapes of riblets. The proposed correlations (\mathcal{D} -based (3.12): black solid lines; \mathcal{F} -based (3.13): blue solid lines) are validated against relevant DNS/experimental results from the literature (red symbols). The literature results plotted are by (a–e) Wong *et al.* (2024) and (f) Bechert *et al.* (1997); the latter were reported originally in terms of $\frac{\Delta C_f}{C_{f,smooth}}$ and the corresponding values of ΔU^+ are obtained here employing the relation $\Delta U^+ = -\frac{\Delta C_f}{C_{f,smooth}} [(2C_{f,smooth})^{-0.5} + 1.25]$. In all panels, the thick black dashed lines represent the simple linear dependence $\Delta U^+ = \lambda_x^+ - \lambda_z^+ = (\lambda_x - \lambda_z) \ell^+$, while the gray dashed lines (wide dashes) show the predictions for ΔU^+ given by Wong *et al.* (2024) based on the so-called “viscous vortex model”.

883 but with angle of 53.5° and height equal to 0.476ℓ) and found that ΔU^+ tends to become
 884 almost constant for ℓ^+ larger than about 60, a behavior which cannot be captured by (3.13).
 885 Another point to be mentioned is that, for the ribletted surfaces examined in figure 18, the
 886 \mathcal{D} -based predictive relationship (3.12), with U_{slip}^+ set to λ_x^+ , yields results for ΔU^+ (plotted
 887 with orange solid lines) which are generally of lower accuracy than those obtained from
 888 (3.13). In addition, the *viscous-vortex-model*-based predictions of the roughness function,
 889 provided by Wong *et al.* (2024), are added to the figure; they generally exhibit reasonable
 890 accuracy up to the optimal ℓ^+ value for each ribletted surface (i.e., that corresponding to the
 891 maximum attainable drag reduction).

892 It is worth concluding this section with some notes of caution as to the applicability of our
 893 predictive correlations.

894 (i) The expressions (3.12) and (3.13) are formulated based on the results of sixteen
 895 homogenization-based DNSs, considering only four configurations of the porous sub-
 896 strate; all cases relate to transversely isotropic patterns and are characterized by a unique
 897 value of porosity, $\theta = 0.5$. More work is certainly needed before the generality of these

898 predictive relationships can be fully confirmed. This is also emphasized in view of the
 899 possible deviations between the upscaling-based numerical results (employed to obtain
 900 all the trends/relationships in this paper) and the real values of the quantities of interest,
 901 attainable for example via high-fidelity feature-resolving DNSs.

902 (ii) There are configurations for which the two proposed correlations may not be tenable.
 903 An example is the case of a superhydrophobic wall, with a flat and undeformable
 904 liquid/gas interface. In this case $\tilde{V}_{rms} = 0$ and equation (3.12) reduces to $\Delta U^+ = U_{slip}^+$

905 (incidentally, also the expression $\mathcal{D} = \frac{B}{\kappa} \tilde{V}_{rms}$ of [Orlandi & Leonardi \(2008\)](#) yields the
 906 same result). Since $U_{slip}^+ \approx \lambda_x^+$ the roughness function would then have a value larger
 907 than that of the conventional viscous approximation, $\Delta U^+ = \lambda_x^+ - \lambda_z^+$ (which is retrieved
 908 by the \mathcal{F} -based relationship (3.13)). For the case of superhydrophobic ribs it has been
 909 shown by [Luchini \(2015\)](#) that results for ΔU^+ obtained with either no-slip/no-shear
 910 boundary conditions or with a homogenized condition collapse well with the linear,
 911 viscous approximation until $\ell^+ \approx 30$.

912 (iii) The good agreement between the predictions of (3.13) and the reference results for
 913 ΔU^+ in figure 18 does not imply that the correlation captures, for example, the initiation
 914 of a Kelvin-Helmholtz instability past some threshold value of ℓ^+ . We believe that our
 915 correlations represent an improvement over linear, viscous results (dashed lines in figure
 916 18) to predict the roughness function, but we would not want to push this as far as stating
 917 that they capture the physics at large values of ℓ^+ . From a mathematical perspective,
 918 equation (3.13) appears to reasonably quantify drag reduction up to and beyond its
 919 maximum attainable value, for each ribletted surface considered.

920 4. Assumptions and range of validity of the model

921 It is necessary to highlight and properly assess the validity of the assumptions and simpli-
 922 fications adopted in the present work, considering the physical problem and the upscaling
 923 approach. Here, we focus on the following issues:

924 (i) The effect of near-wall advection appears in the homogenization model through an
 925 Oseen-like linearization of the momentum equation governing the microscale problem.
 926 This approximation, described in Section 2.2, requires the choice of a streamwise
 927 convective speed representative of the flow near the porous/free-fluid interface (for
 928 instance, refer to the near-interface behavior of \overline{U}^+ displayed in figure 5). The slip
 929 velocity \hat{u}_{slip} , averaged over the fictitious interface, is used in the present work as a
 930 characteristic uniform scale to linearize the problem, and with this simple assumption
 931 a good agreement between the model predictions and the results of the fine-grained
 932 DNS is obtained (Section 3.1). However, there are other options which are “reasonable”,
 933 albeit more complicated, that could be adopted, for example assigning a distribution of
 934 the streamwise velocity component, as function of the wall-normal coordinate, going
 935 from the Darcy’s velocity \hat{u}_{darcy} in the deep porous region to the slip velocity \hat{u}_{slip}
 936 at $\hat{y} = 0$ and, finally, to a linearly increasing behavior for $\hat{y} > 0$; clearly, this choice
 937 requires an approximation of the way the velocity decays below the porous/free-fluid
 938 interface. For future research, near-interface inertia may be taken into account with a
 939 fully nonlinear model, rather than with the current Oseen linearization. This can be
 940 achieved by the use of adjoint homogenization ([Bottaro 2019](#)). Furthermore, it would
 941 be interesting to explore how the values of the upscaled coefficients estimated from the

942 different approaches compare with those predicted by machine learning algorithms for
 943 a large variety of wall microstructures.

944 (ii) The normalization adopted, embodied by equations (2.2a)–(2.2c), implies that the
 945 characteristic time scale of the fluid within the porous medium is much larger than the
 946 temporal scale of phenomena in the free-fluid domain. This is corroborated by results
 947 of several, previous texture-resolving simulations conducted under conditions similar to
 948 the present ones. Further, to ensure the absence of time-dependent effects in the present
 949 microscopic closure problems, we have numerically solved them with a time-dependent
 950 solver for values of Re_{slip} up to 60, eventually always reaching steady solutions. Should
 951 near-wall transient effects become significant, for example beyond some critical value of
 952 Re_{slip} function of the geometry of the porous substrate, time should be incorporated into
 953 the upscaling framework and the effective interface conditions would involve convolution
 954 kernels, similar to the case of poroelastic interfaces (Zampogna *et al.* 2019b). Then,
 955 because of phenomena such as unsteady vortex shedding near the porous/free-fluid
 956 boundary, sufficiently large microscopic elementary cells (possibly consisting of several
 957 geometric unit cells) must be used to solve the closure problems (Agnaou *et al.* 2016).

958 (iii) The first term in the transpiration velocity boundary condition (2.19b) is associated
 959 with the vertical gradient of the normal stress S_{22} and includes the *intrinsic* medium
 960 permeability \mathcal{K}_{yy} as a macroscopic coefficient. The parameter \mathcal{K}_{yy} vanishes by definition
 961 for rough, impermeable walls, while it can be easily evaluated for a deep porous bed
 962 from the solution of a Stokes system on a triply-periodic unit cell, imposing unit forcing
 963 along y . From a theoretical perspective, this approach assumes that the porous region
 964 is formally infinite in depth, for periodicity to perfectly apply along y . In practical
 965 situations, permeable substrates are, conversely, of finite depth and typically bounded
 966 at the bottom in $\hat{y} = -h$ (as in the pattern considered in figure 5). Since a correct
 967 transpiration velocity condition is sensitive mainly to the flow characteristics in a layer
 968 around the interface at $\hat{y} = 0$, we believe that the procedure followed to evaluate \mathcal{K}_{yy}
 969 holds also for porous substrates bounded from below, at least as long as their depth
 970 is sufficiently large. If one were, on the other hand, to solve a Stokes system (with
 971 unit forcing imposed along y) on a unit cell periodic in x and z and extending all the
 972 way to the bottom impermeable boundary, then the result $\mathcal{K}_{yy} = 0$ would be found;
 973 as a consequence, the transpiration boundary condition (at least, up to second-order
 974 accuracy in ϵ) would be free of a velocity-pressure coupling term[†]. In this regard, it is
 975 pertinent to refer to the study by Hao & García-Mayoral (2024) on porous beds formed
 976 by staggered cubes, where they concluded that substrates deeper than about 50 viscous
 977 units can be classified as “*sufficiently deep*”. Under this condition, the turbulent flow
 978 perceives the substrate as deep enough to exhibit its permeable character fully such
 979 that the flow characteristics become almost insensitive to any further increase in the
 980 depth. Since the grains’ pitch distance ℓ^+ is varied in the present work between 10
 981 and 40, five rows of solid inclusions are enough for the above-mentioned threshold of
 982 the substrate depth to be safely satisfied, for all the porous beds considered. The good
 983 agreement between the model results and the grain-resolving simulation (Section 3.1) for
 984 the pattern TC_{20} (with bed depth ≈ 200 viscous units) confirm that this is the case. For
 985 the same configuration, we elaborate on the significance of incorporating the medium-
 986 permeability-related term in the transpiration velocity boundary condition (2.19b) by
 987 showing in figure 19 the predictions of the homogenization-based DNS when \mathcal{K}_{yy} is set

[†] A similar issue was treated by Sharma & García-Mayoral (2020) in the evaluation of the wall-normal flow impedance for a canopy with a bottom, impermeable boundary.

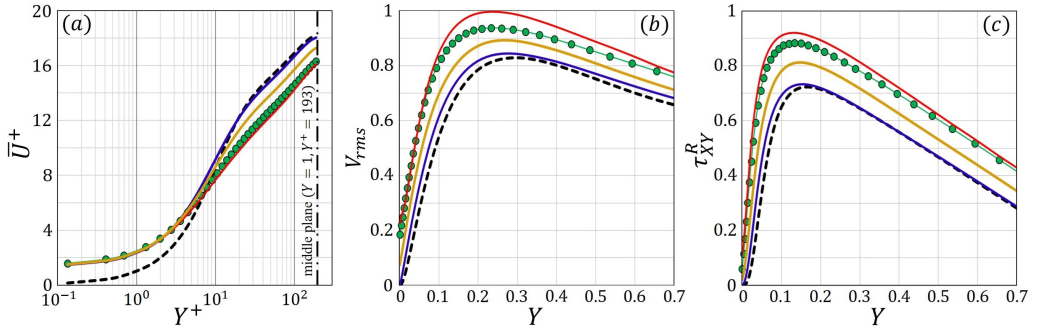


Figure 19: Turbulent channel flow ($Re_{\tau(\mathcal{M})} = 193$) over the porous substrate TC_{20} . Results of the fine-grained simulation (red lines) are used to validate the predictions of three different homogenized simulations, i.e. with the effective boundary conditions of the three velocity components imposed (green lines with filled circles), with the transpiration velocity suppressed (blue lines), or with the *intrinsic* medium permeability $\hat{\mathcal{K}}_{yy}$ set to zero in (2.19b) for the substrate to be modeled as a rough, impermeable wall (yellow lines). The dashed black profiles refer to the smooth, impermeable channel case.

988 to zero. It is clear that modeling such a deep porous substrate as a rough, impermeable
 989 boundary adversely affects the accuracy of the predictions, yet the results remain better
 990 than when transpiration at the fictitious interface is fully suppressed \ddagger . The role of the
 991 medium permeability is less important in the case of the patterns TM and LM for which
 992 $\mathcal{K}_{yy} \ll \mathcal{K}_{xy,zy}^{it,f}$, as shown in table 1.

993 (iv) Finally, for the case of shallow substrates (not treated here), one would probably
 994 need to define and solve different auxiliary, microscopic problems.

995 With respect to the applicability range of the effective boundary conditions (2.19a–2.19c),
 996 it is a complex undertaking to seek a single formal criterion that determines the limit of
 997 validity of the upscaling approach since the accuracy of the model can be sensitive to a large
 998 number of geometric and flow parameters, for instance, the size, shape, and orientation of
 999 the grains, the porosity of the substrate, the degree of regularity of the surface microstructure
 1000 and the Reynolds number. Taking all these factors into considerations requires extensive
 1001 studies in which the model predictions are to be validated against fully-resolving DNSs
 1002 and/or accurate experimental results. From a conceptual perspective, the first-order “*Navier-*
 1003 *slip*” effective conditions of the streamwise and the spanwise velocity components are valid
 1004 only for vanishingly small surface elements, while taking the boundary conditions to higher
 1005 order, including the definition of the transpiration velocity component (2.19b), allows us to
 1006 consider larger surface manipulations. The incorporation of near-wall advection is believed
 1007 to enhance significantly the robustness of the present model.

1008 The discussion in Section 3.3 highlights the role of the r.m.s. fluctuations of the transpira-
 1009 tion velocity at the virtual plane, \tilde{V}_{rms} , key parameter that controls turbulence over irregular
 1010 and porous walls; *ergo* we find it pertinent to judge, preliminarily, the applicability of the
 1011 effective boundary conditions based on the level of \tilde{V}_{rms} estimated a priori from (3.11)
 1012 as function of the macroscopic parameter Ψ of the rough/porous wall. The porous pattern
 1013 chosen for validation of the homogenization-based model in Section 3.1 is characterized by
 1014 $\Psi \approx 5.4$ and \tilde{V}_{rms} close to 0.2; reasonable accuracy of the model is observed upon validation,

\ddagger The reader is also referred to the imposition of the transpiration velocity boundary condition, including the medium permeability effect, in the studies by Lācis *et al.* (2020) and Naqvi & Bottaro (2021), where different flow problems and porous patterns are considered.

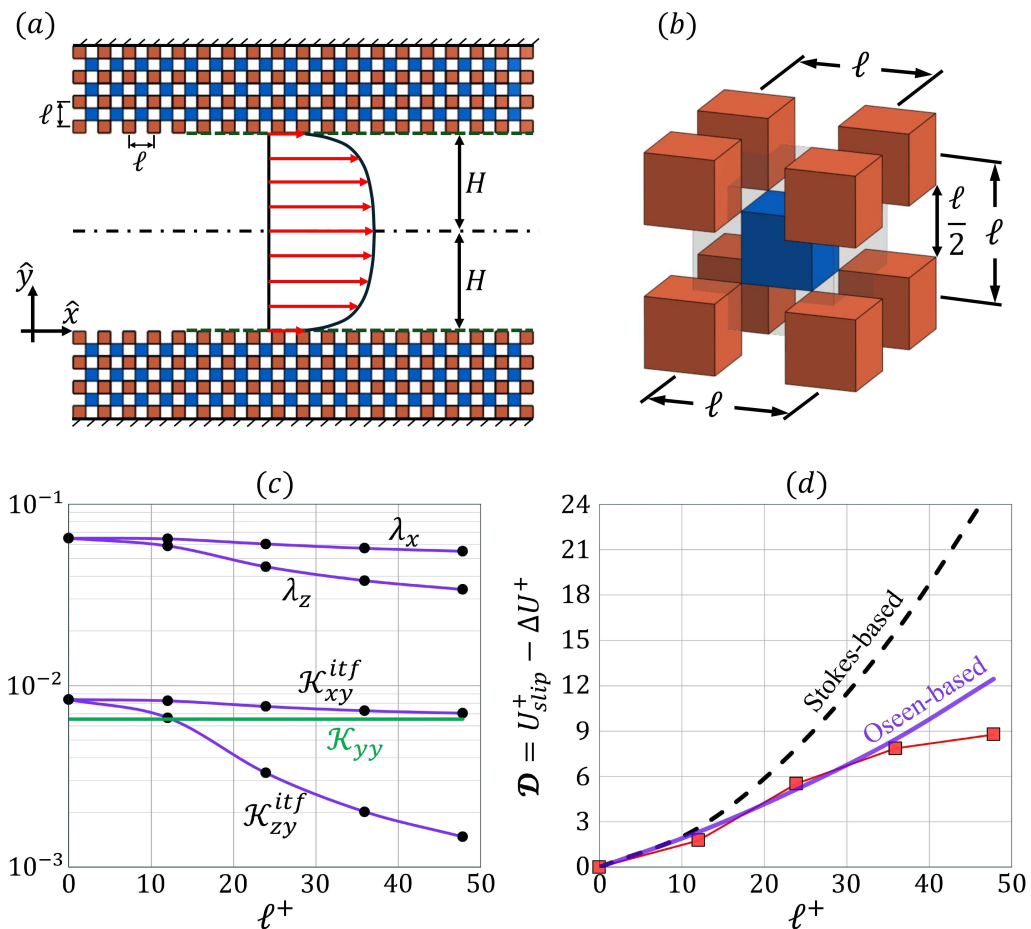


Figure 20: Turbulent flow in a symmetric channel bounded by permeable substrates consisting of staggered cubes: (a) sketch of the full domain considered by Hao & García-Mayoral (2024); (b) topology of the staggered pattern, where the unit cell dimensions are $\ell \times \ell \times \ell$; (c) the macroscopic coefficients, evaluated for different values of ℓ^+ following the procedure explained in Section 2. Since the pattern is three-dimensional, we cannot set any of the spatial derivatives to zero to simplify closure problems (2.13) and (2.15). In frame (d) the behavior of the parameter \mathcal{D} based on (3.12) with either the Oseen-based or the Stokes-based upscaled coefficients, validated against the reference results plotted with filled square symbols.

1015 which is encouraging taking into consideration the significantly low numerical cost of the
 1016 homogenized DNS compared to the full texture-resolving one.

1017 Up to this point, only results for turbulence over anisotropic permeable substrates have
 1018 been discussed, with the inclusions placed in an inline arrangement and infinitely elongated
 1019 in either the streamwise (patterns *LC* and *LM*) or the spanwise (*TC* and *TM*) direction. It
 1020 is appropriate, at this stage, to test the model also for the case of the turbulent flow over
 1021 geometrically isotropic porous arrays consisting of three-dimensional staggered inclusions.
 1022 This is more representative of patterns of packed grains. The configuration studied is
 1023 illustrated in figure 20(a), one of those investigated via fine-grained numerical analysis
 1024 by Hao & García-Mayoral (2024). The $\ell \times \ell \times \ell$ unit cell of the porous domain, shown in
 1025 figure 20(b), consists of a full solid cube in the middle, with edge length $\ell/2$, and one-eighth

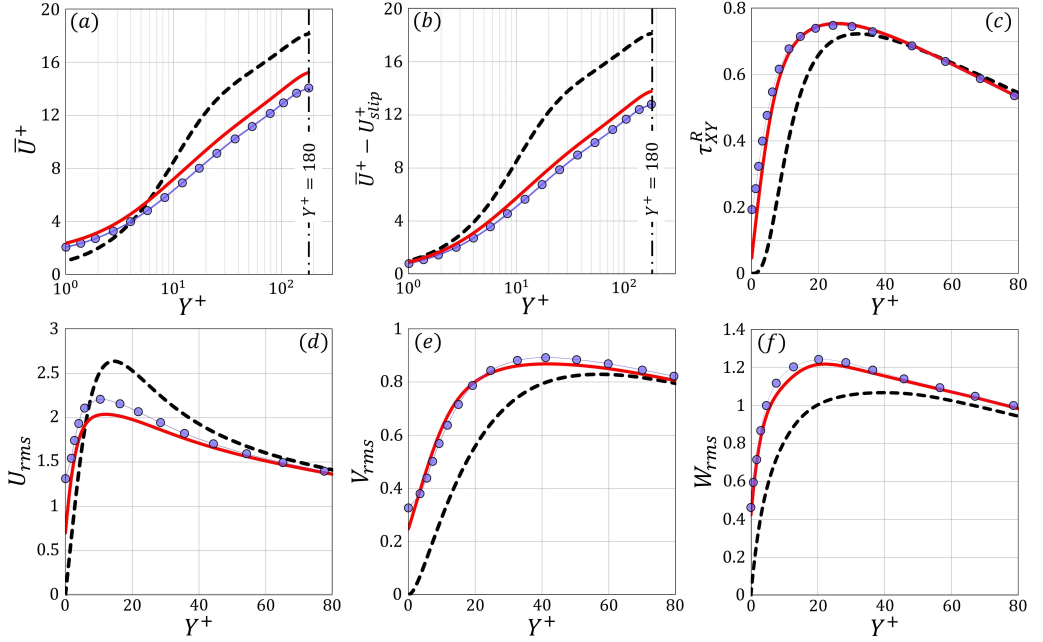


Figure 21: Distribution of the mean velocity and behaviors of sample turbulence statistics for the flow over staggered cubes characterized by $\theta = 0.75$ and $\ell^+ = 24$ (cf. figure 20): predictions of the homogenization-based DNS (red lines) are validated against results of the fine-grained DNS (filled circles) by Hao & García-Mayoral (2024), while the dashed profiles pertain to the smooth, impermeable channel case.

1026 of a cube at each of the corners, satisfying a porosity of 0.75. The Oseen-based upscaled
 1027 coefficients are evaluated for varying values of ℓ^+ (figure 20(c)), where the corresponding
 1028 values of Ψ are estimated to be around (3.8, 6.3, 8.5, 10.7) when ℓ^+ is equal to (12, 24, 36,
 1029 48). While the values of the interface coefficients are close to those obtained earlier for the
 1030 rough, impermeable surface (cf. figure 17), the corresponding values of Ψ are now larger
 1031 due to the contribution of the medium permeability $\mathcal{K}_{yy} \approx 0.0065$ (cf. equation 3.10). Our
 1032 predictions based on (3.12) for \mathcal{D} are calculated and plotted in figure 20(d); they match the
 1033 reference results by Hao & García-Mayoral (2024) up to $\ell^+ \approx 36$ ($\Psi \approx 8.5$). Our DNS cannot
 1034 extend up to such a value of Ψ , on account of the stability issues discussed in Appendix
 1035 A; running the model using the current computational scheme on cases for which \tilde{V}_{rms}
 1036 exceeds 0.25 ($\Psi \gtrsim 6.5$) may result in questionable numerical solutions. A direct numerical
 1037 simulation, employing the effective boundary conditions, is thus conducted for the same
 1038 configuration shown in figure 20, with $\ell^+ \approx 24$ ($\Psi \approx 6.3$), near what we consider to be
 1039 the limit of applicability of the model[†]. Sample results are displayed in figure 21 and are
 1040 compared against those by Hao & García-Mayoral (2024). It is interesting that at such a
 1041 value of Ψ the model can still provide trends reasonably consistent with the reference results,
 1042 concerning the distribution of the mean streamwise velocity in the channel (which displays
 1043 a considerable increase in drag) as well as the near-interface behaviors of the Reynolds
 1044 stress and of the turbulent fluctuations in the velocity components. The present findings
 1045 are encouraging for future research in which the accuracy of the model can be assessed

[†] We define the limit of applicability with respect to the ability of the model to reproduce macroscopic feature-resolved results (e.g. roughness function, flow rate, skin friction coefficient, etc.) to within an approximation of $\pm 20\%$. For the pattern TC_{20} this occurs when $\Psi = 5.4$, as discussed in Section 3.1.

1046 (and adjustments/improvements of the formulation recommended) for several types of wall
 1047 microstructures, including irregular porous media and rough surfaces, ribletted walls, liquid-
 1048 infused surfaces under the condition of lubricant depletion, etc.

1049 5. Conclusions

1050 Before summarizing the outcomes of the present work, it is useful to briefly outline
 1051 the objectives we were planning to achieve. Our primary aim was to derive a model of
 1052 wall boundary conditions capable to replace the expensive texture-resolving simulations of
 1053 turbulent flows, to test its validity and assess its limitations. The boundary model derived
 1054 extends that going by the name of Beavers-Joseph-Saffman in several respects: it goes to
 1055 higher order in terms of the expansion parameter ϵ , it includes effects of advection (admittedly,
 1056 in an approximate fashion), and it contains no empirical parameters. The second goal we were
 1057 aiming to achieve was to find a correlation between the model constants (slip and permeability
 1058 coefficients) and macroscopic features of the flow, such as the vertical fluctuating velocity
 1059 and Hama's roughness function. The third objective was to assess whether the model's
 1060 parameters, stemming from the microscopic simulations, could be used to make *a priori*
 1061 predictions of turbulent flows in channels bounded by microstructured/permeable walls. We
 1062 believe that, on all three counts above, several interesting advances have been made.

1063 A more detailed account of results and conclusions now follows. The macroscopic
 1064 parameters characterizing porous/rough walls are the two Navier-slip coefficients (λ_x, λ_z), the
 1065 two interface permeability coefficients ($\mathcal{K}_{xy}^{iff}, \mathcal{K}_{zy}^{iff}$), and the intrinsic medium permeability
 1066 (\mathcal{K}_{yy} , nonzero for sufficiently deep porous substrates); all of them are sensitive to both the
 1067 micro-structural details of the wall and to the level of advection in the vicinity of the interface.
 1068 The asymptotic homogenization framework adopted incorporates the latter effect into the
 1069 analysis of the microscale problem via an *Oseen-like* linearization, and a Reynolds number
 1070 $Re_{slip} = \ell^+ U_{slip}^+$ hence appears in the closure problems used to evaluate the upscaled
 1071 coefficients of the model, which contribute to the definition of high-order *effective* boundary
 1072 conditions of the three velocity components (2.19a–2.19c) at a virtual plane boundary next
 1073 to the physical porous/rough one.

1074 The effective boundary conditions were employed to simplify a set of direct numerical
 1075 simulations of the turbulent flow in a channel delimited from one side (at $Y = 2$) by a
 1076 smooth, impermeable wall and from the other side (at $Y \leq 0$) by a transversely isotropic
 1077 porous substrate having a porosity $\theta = 0.5$. Four patterns of the substrate were studied, two
 1078 streamwise-elongated and two spanwise-elongated, and for each of them four values of the
 1079 inclusions pitch, ℓ^+ , were tested in the range $0 < \ell^+ < 40$. The model was validated, for
 1080 one challenging case (transverse cylinders with $\ell^+ \approx 40$) against a classical fine-grained
 1081 DNS, and acceptable agreement was found. The mean velocity profiles and the turbulence
 1082 statistics at, and next to, the permeable walls were analyzed to interpret the behavior of the
 1083 roughness function and the ensuing increase/reduction in skin-friction drag, $\Delta C_f^{\%}$. Drag
 1084 reduction (here up to 5%) is achieved exclusively with substrates of streamwise-preferential
 1085 permeability (where $\lambda_x^+ > \lambda_z^+$ and $\mathcal{K}_{xy}^{iff,+} > \mathcal{K}_{zy}^{iff,+}$), and is proportional, for small values
 1086 of ℓ^+ , to $\Delta\lambda^+ = \lambda_x^+ - \lambda_z^+$. For the turbulent flow over substrates of spanwise-preferential
 1087 permeability (or even those elongated in the streamwise direction and characterized by
 1088 excessive ℓ^+ values), an increase in the skin-friction drag is detected (here up to 27%) and
 1089 is accompanied by large levels of r.m.s. fluctuations in wall-normal and spanwise velocity
 1090 components, in the Reynolds stress, τ_{xy}^R , and in the rate of production of turbulent kinetic
 1091 energy, P_T , near the substrate/channel interface.

1092 In view of the results extracted from the sixteen DNSs performed for the turbulent flow

1093 over modeled substrates, special attention was directed to the dependence of the roughness
 1094 function, ΔU^+ , on \tilde{V}_{rms} , \tilde{W}_{rms} , and $\tilde{\tau}_{xy}^R$ (tildes are used to denote values at the porous/free-
 1095 fluid interface, $Y = 0$). While the relation between ΔU^+ and each of these turbulence-
 1096 characterizing quantities differs according to the geometry/configuration of the porous bed,
 1097 the data are found to collapse quite well when specific roughness-function-related quantities
 1098 are examined; they are $\mathcal{D} = U_{slip}^+ - \Delta U^+$ and $\mathcal{F} = \Delta \lambda^+ - \Delta U^+$, and they increase monotonically
 1099 with \tilde{V}_{rms} , \tilde{W}_{rms} , and $\tilde{\tau}_{xy}^R$. Moreover, evidence of the significant role played by \tilde{V}_{rms} as a
 1100 control parameter in the turbulent flow over not only permeable but also rough, impermeable
 1101 boundaries was demonstrated, particularly thanks to the work by Leonardi, Orlandi and
 1102 collaborators (Leonardi *et al.* 2003; Orlandi & Leonardi 2006, 2008). The quantities \mathcal{D} and
 1103 \mathcal{F} were expressed as functions of \tilde{V}_{rms} via the fitting correlations (3.3) and (3.6), respectively.
 1104 To put these relationships to practical use in the *a priori* evaluation of the roughness function
 1105 (i.e., without the need for running the direct numerical simulations) the dependence of \tilde{V}_{rms}
 1106 on the upscaled coefficients of the homogenization model was explored; based on the present
 1107 results, a compound macroscopic quantity Ψ , defined by (3.10), is proposed as a single
 1108 parameter correlated to \tilde{V}_{rms} . Eventually, the most significant result of the present study is
 1109 the nexus found among the roughness function, the slip velocity, and the upscaled coefficients,
 1110 i.e.

$$1111 \quad \Delta U^+ = U_{slip}^+ - 11.5 \times \left(0.00075 \Psi^3 + 0.002 \Psi^2 \right)^{0.6}, \quad (4.1)$$

$$1113 \quad \Delta U^+ = \Delta \lambda^+ - 11.5 \times \left(0.00075 \Psi^3 + 0.002 \Psi^2 \right). \quad (4.2)$$

1114 Although these equations are originally based on fitting the present results for the turbulent
 1115 flow over porous substrates, they yield satisfactory agreement with simulation and experi-
 1116 mental results for selected rough, impermeable boundaries (Hao & García-Mayoral 2024;
 1117 Wong *et al.* 2024; Bechert *et al.* 1997), within the range of validity of the model (cf. Section
 1118 4). One very interesting point is that the non-monotonic behavior of ΔU^+ with the increase in
 1119 ℓ^+ for the case of riblets (linear/non-linear trends of drag reduction followed by performance
 1120 degradation and eventually drag increase) can be captured by (4.2) up to ℓ^+ values of about
 1121 40.

1122 The present analysis provides sufficient motivation to carry out further investigations
 1123 for the purpose of either assessing the versatility of (4.1) and (4.2) for the turbulent
 1124 flow over various textured boundaries or proposing more robust correlations. Once this
 1125 is accomplished, the findings can be employed, for instance, to accelerate large-scale
 1126 optimization studies of the wall micro-structure (topology/size/arrangement of the grains),
 1127 avoiding direct or large eddy simulations at least in the preliminary stages of the work.

1129 **Funding.** Activity funded by the European Union Next Generation EU, via PRIN PNRR 2022 grant, project
 1130 code P2022CZ5KZ (“SLIPS”).

1131 **Declaration of interests.** The authors report no conflict of interest.

1132 **Author ORCID.** Essam Nabil Ahmed, <https://orcid.org/0000-0002-4103-9273>; Alessandro Bottaro,
 1133 <https://orcid.org/0000-0003-0853-2522>

1134 Appendix A. Considerations on the transpiration velocity boundary condition

1135 The following assumptions/simplifications related to the imposition of the boundary con-
 1136 dition (2.19b) in the direct numerical simulations are adopted, mainly to guarantee the

1137 stability of the solution. Handling the pressure gradient $\frac{\partial \hat{p}}{\partial \hat{y}}$ at the fictitious plane $\hat{y} = 0$
 1138 is of much importance. If the physical wall were smooth and impermeable, one would
 1139 write $\frac{\partial \hat{p}}{\partial \hat{y}} \Big|_0 = \mu \frac{\partial^2 \hat{v}}{\partial \hat{y}^2} \Big|_0$, which also applies to walls/substrates with small surface protrusions,
 1140 e.g., vanishingly small values of ℓ^+ . The present work includes the study of the turbulent
 1141 flow over porous substrates having relatively large values of ℓ^+ (up to ≈ 40), and thus the
 1142 aforementioned expression becomes questionable. We have found it effective and sufficiently
 1143 accurate to incorporate the inertial effects associated with the transpiration velocity into the
 1144 expression above, to obtain $\frac{\partial \hat{p}}{\partial \hat{y}} \Big|_0 = \left(\mu \frac{\partial^2 \hat{v}}{\partial \hat{y}^2} - \rho \hat{v} \frac{\partial \hat{v}}{\partial \hat{y}} \right) \Big|_0$. The boundary condition (2.19b) now
 1145 reads

$$1146 \quad \hat{v}|_0 \approx \frac{\hat{\mathcal{K}}_{yy}}{\mu} \left(\rho \hat{v} \frac{\partial \hat{v}}{\partial \hat{y}} + \mu \frac{\partial^2 \hat{v}}{\partial \hat{y}^2} \right) \Big|_0 - \hat{\mathcal{K}}_{xy}^{itf} \frac{\partial}{\partial \hat{x}} \left(\frac{\partial \hat{u}}{\partial \hat{y}} + \frac{\partial \hat{v}}{\partial \hat{x}} \right) \Big|_0 - \hat{\mathcal{K}}_{zy}^{itf} \frac{\partial}{\partial \hat{z}} \left(\frac{\partial \hat{w}}{\partial \hat{y}} + \frac{\partial \hat{v}}{\partial \hat{z}} \right) \Big|_0. \quad (\text{A1})$$

1147 With the continuity equation in mind, we have

$$1148 \quad \frac{\partial^2 \hat{v}}{\partial \hat{y}^2} \Big|_0 = \frac{\partial}{\partial \hat{y}} \left(\frac{\partial \hat{v}}{\partial \hat{y}} \right) \Big|_0 = \frac{\partial}{\partial \hat{y}} \left(-\frac{\partial \hat{u}}{\partial \hat{x}} - \frac{\partial \hat{w}}{\partial \hat{z}} \right) \Big|_0, \quad (\text{A2})$$

1149 and (A1) becomes

$$1150 \quad \hat{v}|_0 \approx \hat{\mathcal{K}}_{yy} \left(\frac{\rho}{\mu} \hat{v} \frac{\partial \hat{v}}{\partial \hat{y}} - \frac{\partial}{\partial \hat{x}} \frac{\partial \hat{u}}{\partial \hat{y}} - \frac{\partial}{\partial \hat{z}} \frac{\partial \hat{w}}{\partial \hat{y}} \right) \Big|_0 - \hat{\mathcal{K}}_{xy}^{itf} \frac{\partial}{\partial \hat{x}} \left(\frac{\partial \hat{u}}{\partial \hat{y}} + \frac{\partial \hat{v}}{\partial \hat{x}} \right) \Big|_0 - \hat{\mathcal{K}}_{zy}^{itf} \frac{\partial}{\partial \hat{z}} \left(\frac{\partial \hat{w}}{\partial \hat{y}} + \frac{\partial \hat{v}}{\partial \hat{z}} \right) \Big|_0. \quad (\text{A3})$$

1151 Employing the Navier's slip conditions

$$1152 \quad \hat{u}|_0 = \hat{\lambda}_x \left(\frac{\partial \hat{u}}{\partial \hat{y}} + \frac{\partial \hat{v}}{\partial \hat{x}} \right) \Big|_0 \approx \hat{\lambda}_x \frac{\partial \hat{u}}{\partial \hat{y}} \Big|_0, \quad \hat{w}|_0 = \hat{\lambda}_z \left(\frac{\partial \hat{w}}{\partial \hat{y}} + \frac{\partial \hat{v}}{\partial \hat{z}} \right) \Big|_0 \approx \hat{\lambda}_z \frac{\partial \hat{w}}{\partial \hat{y}} \Big|_0, \quad (\text{A4})$$

1153 to further simplify (A3), we eventually obtain the following expression:

$$1154 \quad \hat{v}|_0 \approx \frac{\rho \hat{\mathcal{K}}_{yy}}{\mu} \left(\hat{v} \frac{\partial \hat{v}}{\partial \hat{y}} \right) \Big|_0 - \frac{\hat{\mathcal{K}}_{xy}^{itf} + \hat{\mathcal{K}}_{yy}}{\hat{\lambda}_x} \frac{\partial \hat{u}}{\partial \hat{x}} \Big|_0 - \frac{\hat{\mathcal{K}}_{zy}^{itf} + \hat{\mathcal{K}}_{yy}}{\hat{\lambda}_z} \frac{\partial \hat{w}}{\partial \hat{z}} \Big|_0. \quad (\text{A5})$$

1155 Note that the simplification made to the first-order Navier's slip conditions in (A4) by
 1156 neglecting the terms where \hat{v} appears derived with respect to either \hat{x} or \hat{z} relies on the fact
 1157 that the vertical velocity at the wall is of order ϵ^2 (cf. 2.18b). This assumption is employed
 1158 in particular to render $\frac{\partial}{\partial \hat{x}} \frac{\partial \hat{u}}{\partial \hat{y}} \Big|_0$ and $\frac{\partial}{\partial \hat{z}} \frac{\partial \hat{w}}{\partial \hat{y}} \Big|_0$ in the first term of (A3) equal to $\frac{1}{\hat{\lambda}_x} \frac{\partial \hat{u}}{\partial \hat{x}} \Big|_0$
 1159 and $\frac{1}{\hat{\lambda}_z} \frac{\partial \hat{w}}{\partial \hat{z}} \Big|_0$, respectively, while the complete first-order Navier's slip conditions can be
 1160 used directly for the interface-permeability-related terms. Interestingly, if the viscous terms
 1161 $\mu \frac{\partial^2 \hat{v}}{\partial \hat{x}^2} \Big|_0$ and $\mu \frac{\partial^2 \hat{v}}{\partial \hat{z}^2} \Big|_0$ were included in the definition of $\frac{\partial \hat{p}}{\partial \hat{y}} \Big|_0$, the same expression (A5) would
 1162 be obtained without the need for the approximation in (A4).

1163 It is important to emphasize that any simplifications made here to the transpiration velocity
 1164 boundary condition should be perceived as part of the modeling procedure, where our final
 1165 validity criterion is the comparison between the results of the macroscopic model and the
 1166 fine-grained DNSs (cf. figures 6, 7, and 21). In this manner, we assess the combined influence
 1167 of the different sources of errors entailed in the upscaling method on the accuracy of the

1168 predictions. For example, the transient term $-\rho \frac{\partial \hat{v}}{\partial \hat{t}} \Big|_0$, omitted here in the definition of $\frac{\partial \hat{p}}{\partial \hat{y}} \Big|_0$,
 1169 would contribute to $\hat{v}|_0$ by an amount $\hat{\mathcal{K}}_{yy} \frac{\rho}{\mu} \frac{\partial \hat{v}}{\partial \hat{t}} \Big|_0$ which is of order $\epsilon^5 Re_\tau u_\tau$; this becomes
 1170 as large as $\epsilon^2 u_\tau$, i.e. theoretically comparable to the terms in (A5), when ϵ approaches 0.2
 1171 (for $Re_\tau \approx 190$). Nonetheless, one cannot quantify the inaccuracy of the method solely
 1172 based on the growth of this term, unaccounted for in equation (A5). Ideally, should transient
 1173 effects be significant in the microscopic region, a more sophisticated upscaling model would
 1174 be needed to incorporate them, yielding macroscopic coefficients which are possibly time-
 1175 variant (Zampogna *et al.* 2019b; Lasseux *et al.* 2019) and/or higher-order unsteady terms in
 1176 the expressions of the effective boundary conditions (Ahmed *et al.* 2022a).

1177 The following equation, which can be simply derived from (A5), is the expression of the
 1178 transpiration velocity boundary condition implemented in the numerical code:

$$1179 \quad \hat{v}|_0 \approx \left(-\frac{\hat{\mathcal{K}}_{xy}^{itf} + \hat{\mathcal{K}}_{yy}}{\hat{\lambda}_x} \frac{\partial \hat{u}}{\partial \hat{x}} \Big|_0 - \frac{\hat{\mathcal{K}}_{zy}^{itf} + \hat{\mathcal{K}}_{yy}}{\hat{\lambda}_z} \frac{\partial \hat{w}}{\partial \hat{z}} \Big|_0 \right) / \left(1 - \frac{\rho \hat{\mathcal{K}}_{yy}}{\mu} \frac{\partial \hat{v}}{\partial \hat{y}} \Big|_0 \right). \quad (\text{A6})$$

1180 Special attention is directed to the denominator of the right-hand-side term in (A6) since
 1181 small values at one iteration may result in exceedingly large transpiration velocities, which
 1182 can seriously disrupt the progress of the iterative process and the solution. For numerical
 1183 calculations at a given time, \hat{t} , the value of the denominator is explicitly evaluated from the
 1184 previous time instant, $\hat{t} - \Delta \hat{t}$. Clearly, for vanishingly small values of ℓ^+ , the near-interface

1185 advection is negligible compared to the viscous effects, and hence $\frac{\rho \hat{\mathcal{K}}_{yy}}{\mu} \frac{\partial \hat{v}}{\partial \hat{y}} \Big|_0$ approaches
 1186 0 so that the denominator in (A6) tends to 1. On the other hand, for porous substrates
 1187 made of transverse/longitudinal cylindrical inclusions with the largest ℓ^+ studied here, the
 1188 distributions of the value of the denominator over space (\hat{x} - \hat{z}) at different time instants are
 1189 found to lie within a range extending from 0.25 to 2; values outside this range (recorded at
 1190 less than 1% of the points on the virtual wall) are considered as outliers and are forced equal
 1191 to the closest limit (either 0.25 or 2). Similarly, the value of the transpiration velocity $\hat{v}|_0$ is
 1192 monitored and is bounded within $\pm 2 u_{\tau(M)}$, again with outliers detected at less than 1% of the
 1193 points. It is worth noting that these outliers are observed here for the modeled substrates TC_{20}
 1194 and LC_{20} only. If porous patterns with larger periodicity or porosity were considered, we
 1195 would expect the errors associated with imposing such artificial limits to be more significant.
 1196 Finally, for conservation of mass to be satisfied over the whole computational domain, the
 1197 plane-averaged value of $\hat{v}|_0$ must vanish. Small deviations associated with numerical error
 1198 are found to undermine convergence; to overcome this, the plane-averaged value of $\hat{v}|_0$ is
 1199 evaluated every 10 time steps and uniformly subtracted from the local values.

1200 At each time instant, evaluation of the effective boundary conditions takes place as part of
 1201 the iterative process of the implicit scheme used for temporal discretization; the convergence
 1202 of the numerical solution is demonstrated in figure 22 considering two sample cases, TC_{10}
 1203 (top) and TC_{20} (bottom).

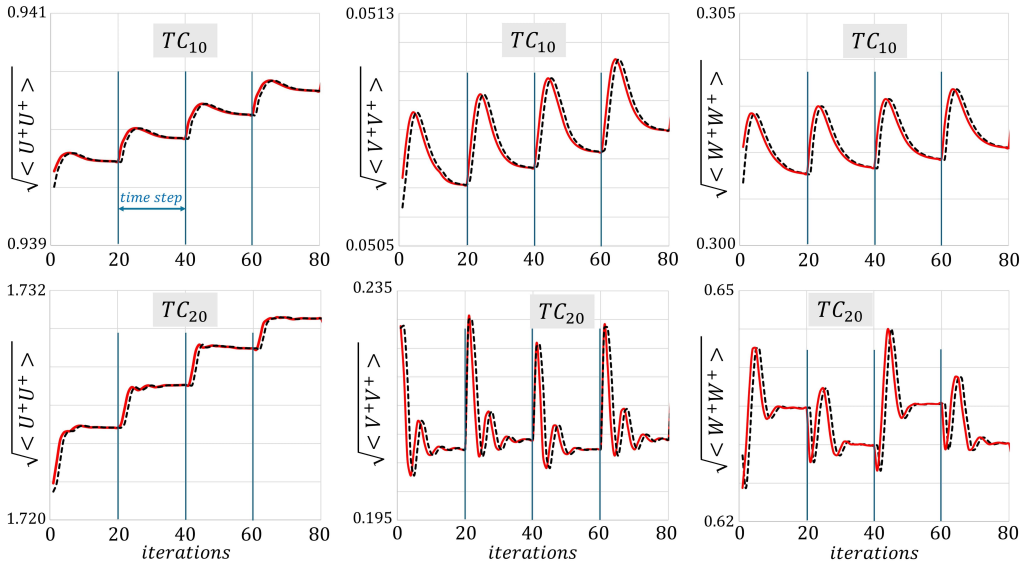


Figure 22: Convergence of $\sqrt{\langle U_i^+ U_i^+ \rangle}$ at $Y = 0$ during the iterative process, over 4 time steps (one time step requires 20 inner iterations of the implicit procedure; $\langle \rangle$ indicates X - Z -spatial averaging). Red lines are plotted with the velocities obtained from the numerical solution at the end of each inner iteration, while black dashed lines are obtained by explicitly evaluating all terms in the effective conditions imposed in the code.

1204 Appendix B. Normalization based on wall shear velocity

1205 The macroscopic-pressure-gradient-based velocity scale $u_{\tau(M)}$ has been used for normal-
 1206 ization throughout the paper. To facilitate comparisons with previous studies we also provide
 1207 the values of the major parameters related to the mean velocity profile when normalized by
 1208 the permeable-interface shear velocity $u_{\tau(B)}$, and of the model coefficients when the $Re_{\tau(B)}$
 1209 is used in (3.2b) and (3.2c); these quantities are available in table 3. It is evident that the
 1210 cases of skin-friction drag increase are characterized by shear-velocity ratios $\frac{u_{\tau(B)}}{u_{\tau(M)}}$, and

1211 therefore stress ratios $\frac{\tau_B}{\tau_M}$, larger than 1, which can be attributed to the fact that the shear
 1212 stress at the permeable boundary for each of these cases, with account of the Reynolds stress,
 1213 is larger than that at the top smooth wall. The opposite applies to the cases of drag reduction.
 1214 Accordingly, the values of ΔU^+ , ΔU_{ch}^+ %, and ΔC_f % in table 3 are all larger, in absolute
 1215 value, than those in table 2.

1216 In figure 23, the values of $\mathcal{D} = U_{slip}^+ - \Delta U^+$ and $\mathcal{F} = \Delta \lambda^+ - \Delta U^+$ are plotted against
 1217 Ψ (3.10), where the mean velocities and the macroscopic coefficients are normalized with
 1218 either the macroscopic-pressure-gradient-based shear velocity $u_{\tau(M)}$ (cf. table 2) or the
 1219 bottom-wall shear velocity, $u_{\tau(B)}$ (cf. table 3). For both choices of u_{τ} , the expressions (3.12)
 1220 and (3.13) exhibit trends in reasonable agreement with the numerical results.

Table 3: Macroscopic coefficients and major results defined/normalized based on the fictitious-interface (bottom) shear velocity $u_{\tau(\mathcal{B})}$. The roughness function ΔU^+ is evaluated by averaging the shift in the mean streamwise velocity (taking the smooth channel case as a reference) over the region $30 \lesssim Y^+ \lesssim 120$, with Y^+ defined now based on $u_{\tau(\mathcal{B})}$.

Substrate	$\frac{u_{\tau(\mathcal{B})}}{u_{\tau(\mathcal{M})}}$	Macroscopic coefficients					Sample results			
		λ_x^+	λ_z^+	$\mathcal{K}_{xy}^{itf,+}$	$\mathcal{K}_{zy}^{itf,+}$	\mathcal{K}_{yy}^+	U_{slip}^+	ΔU^+	$\Delta U_{ch}^+ \%$	$\Delta C_f \%$
Smooth	1	0	0	0	0	0	0	0	0	0
TC_5	1.008	0.43	0.65	0.20	0.49	0.17	0.43	-0.45	-1.8%	+3.8%
TC_{10}	1.023	0.81	1.17	0.71	1.64	0.71	0.81	-1.12	-5.4%	+11.8%
TC_{15}	1.037	1.10	1.52	1.29	2.76	1.65	1.10	-2.10	-9.7%	+22.7%
TC_{20}	1.068	1.38	1.83	1.99	3.98	3.10	1.35	-3.32	-16.0%	+41.8%
LC_5	0.996	0.66	0.43	0.51	0.21	0.17	0.67	+0.31	+1.5%	-2.9%
LC_{10}	0.996	1.32	0.87	2.06	0.83	0.68	1.34	+0.24	+1.3%	-2.6%
LC_{15}	1.011	2.01	1.32	4.77	1.92	1.57	2.03	-0.71	-2.5%	+5.1%
LC_{20}	1.045	2.78	1.82	9.05	3.65	2.97	2.75	-2.29	-10.8%	+25.6%
TM_5	1.014	0.55	1.04	0.36	1.05	0.01	0.55	-0.82	-3.6%	+7.7%
TM_{10}	1.037	0.98	1.78	1.10	3.29	0.05	0.98	-1.94	-8.9%	+20.5%
TM_{15}	1.063	1.30	2.22	1.83	5.47	0.11	1.28	-3.05	-14.5%	+36.6%
TM_{20}	1.078	1.55	2.49	2.45	7.31	0.21	1.49	-3.67	-17.7%	+47.7%
LM_5	0.990	1.08	0.56	1.11	0.38	0.01	1.08	+0.59	+2.9%	-5.6%
LM_{10}	0.988	2.15	1.12	4.41	1.49	0.04	2.18	+0.74	+3.8%	-7.3%
LM_{15}	1.010	3.30	1.72	10.38	3.52	0.10	3.32	-0.49	-1.4%	+2.8%
LM_{20}	1.024	4.47	2.33	18.96	6.42	0.19	4.38	-1.29	-5.2%	+11.3%

1221 Appendix C. Macroscopic coefficients for surfaces with riblets

1222 For the different ribletted surfaces sketched in figure 18, values of the upscaled coefficients
1223 contributing to the effective boundary conditions (2.18a–2.18c) are evaluated (table 4)
1224 for a virtual boundary at $\hat{y} = 0$, i.e. the plane passing through the tips/outer rims of
1225 the longitudinal protrusions. These walls are impermeable ($\mathcal{K}_{yy} = 0$), and they exhibit
1226 streamwise-preferential slip with $\lambda_x > \lambda_z$ and $\mathcal{K}_{xy}^{itf} > \mathcal{K}_{zy}^{itf}$. For each surface, the coefficients
1227 are calculated by solving the auxiliary systems (2.22) and (2.23) over a two-dimensional ($\hat{y}-\hat{z}$)
1228 elementary cell representative of the microscopic domain. The riblets are \hat{x} -elongated, which
1229 allows to set $\partial/\partial x_1$ to zero in the closure problems, thus rendering them advection-insensitive.

1230

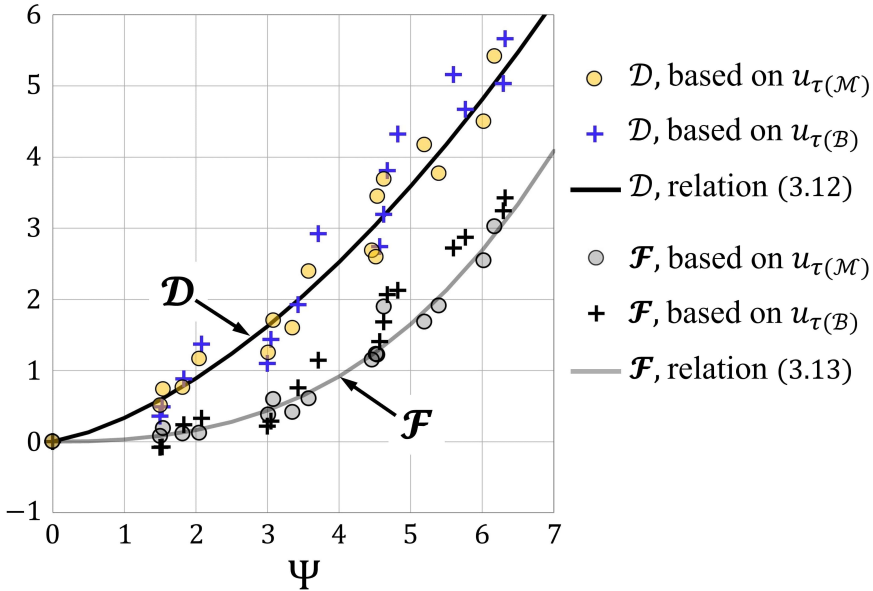


Figure 23: The quantities \mathcal{D} and \mathcal{F} plotted against the parameter Ψ for the sixteen porous patterns modeled in this work. The results for these quantities are obtained with the parameters contributing to their definitions normalized based on either $u_{\tau(\mathcal{M})}$ or $u_{\tau(\mathcal{B})}$. Predictions of (3.12) and (3.13) are plotted with solid lines.

Table 4: Macroscopic coefficients for surfaces altered with riblets.

Riblets' geometry	Dimensionless macroscopic coefficients			
	λ_x	λ_z	\mathcal{K}_{xy}^{itf}	\mathcal{K}_{zy}^{itf}
equilateral triangle	0.1708	0.0807	0.02821	0.00586
right triangle, symmetric	0.1397	0.0770	0.01683	0.00573
right triangle, asymmetric	0.1273	0.0768	0.01411	0.00502
trapezoidal	0.1915	0.0816	0.03484	0.00542
thick blade	0.1144	0.0491	0.02102	0.00213
thin blade	0.1915	0.0783	0.03788	0.00455

REFERENCES

- 1231 ABDERRAHAMAN-ELENA, N., FAIRHALL, C.T. & GARCÍA-MAYORAL, R. 2019 Modulation of near-wall
1232 turbulence in the transitionally rough regime. *J. Fluid Mech.* **865**, 1042–1071.
- 1233 ABDERRAHAMAN-ELENA, N. & GARCÍA-MAYORAL, R. 2017 Analysis of anisotropically permeable surfaces
1234 for turbulent drag reduction. *Phys. Rev. Fluids* **2** (11), 114609.
- 1235 AGNAOU, M., LASSEUX, D. & AHMADI, A. 2016 From steady to unsteady laminar flow in model porous
1236 structures: an investigation of the first Hopf bifurcation. *Comput. Fluids* **136**, 67–82.

- 1237 AHMED, E.N. & BOTTARO, A. 2024 Laminar flow in a channel bounded by porous/rough walls: Revisiting
1238 Beavers-Joseph-Saffman. *Eur. J. Mech. B Fluids* **103**, 269–283.
- 1239 AHMED, E.N., BOTTARO, A. & TANDA, G. 2022a A homogenization approach for buoyancy-induced flows
1240 over micro-textured vertical surfaces. *J. Fluid Mech.* **941**, A53.
- 1241 AHMED, E.N., NAQVI, S.B., BUDA, L. & BOTTARO, A. 2022b A homogenization approach for turbulent channel
1242 flows over porous substrates: Formulation and implementation of effective boundary conditions.
1243 *Fluids* **7** (5), 178.
- 1244 ANTONIA, R.A., ZHU, Y. & SOKOLOV, M. 1995 Effect of concentrated wall suction on a turbulent boundary
1245 layer. *Phys. Fluids* **7** (10), 2465–2474.
- 1246 BABUŠKA, I. 1976 Homogenization and its application. Mathematical and computational problems, in:
1247 Hubbard, B. (Ed.), *Numerical Solution of Partial Differential Equations–III*, pp. 89–116. Academic
1248 Press .
- 1249 BECHERT, D.W. & BARTENWERFER, M. 1989 The viscous flow on surfaces with longitudinal ribs. *J. Fluid*
1250 *Mech.* **206**, 105–129.
- 1251 BECHERT, D.W., BRUSE, M., HAGE, W., VAN DER HOEVEN, J.G.T. & HOPPE, G. 1997 Experiments on drag-
1252 reducing surfaces and their optimization with an adjustable geometry. *J. Fluid Mech.* **338**, 59–87.
- 1253 BERNARD, P.S., THOMAS, J.M. & HANDLER, R.A. 1993 Vortex dynamics and the production of Reynolds
1254 stress. *J. Fluid Mech.* **253**, 385–419.
- 1255 BERNARDINI, M., GARCÍA CARTAGENA, E.J., MOHAMMADI, A., SMITS, A.J. & LEONARDI, S. 2021 Turbulent
1256 drag reduction over liquid-infused textured surfaces: effect of the interface dynamics. *J. Turbul.*
1257 **22** (11), 681–712.
- 1258 BOTTARO, A. 2019 Flow over natural or engineered surfaces: an adjoint homogenization perspective. *J. Fluid*
1259 *Mech.* **877**, P1.
- 1260 BOTTARO, A. & NAQVI, S.B. 2020 Effective boundary conditions at a rough wall: a high-order homogenization
1261 approach. *Meccanica* **55** (9), 1781–1800.
- 1262 BREUGEM, W.P., BOERSMA, B.J. & UITTENBOGAARD, R.E. 2006 The influence of wall permeability on
1263 turbulent channel flow. *J. Fluid Mech.* **562**, 35–72.
- 1264 BUDA, L. 2021 Drag reduction over rough permeable surfaces: A homogenized-based
1265 approach. Master’s Thesis in Physics, University of Genoa, Italy. Available at
1266 http://www.dicat.unige.it/bottaro/Presentation%20group/Thesis_Buda.pdf.
- 1267 BURATTINI, P., LEONARDI, S., ORLANDI, P. & ANTONIA, R.A. 2008 Comparison between experiments and
1268 direct numerical simulations in a channel flow with roughness on one wall. *J. Fluid Mech.* **600**,
1269 403–426.
- 1270 CHANG, J., JUNG, T., CHOI, H. & KIM, J. 2019 Predictions of the effective slip length and drag reduction
1271 with a lubricated micro-groove surface in a turbulent channel flow. *J. Fluid Mech.* **874**, 797–820.
- 1272 CHAVARIN, A., GÓMEZ-DE-SEGURA, G., GARCÍA-MAYORAL, R. & LUHAR, M. 2021 Resolvent-based
1273 predictions for turbulent flow over anisotropic permeable substrates. *J. Fluid Mech.* **913**, A24.
- 1274 CHENG, H. & CASTRO, I.P. 2002 Near wall flow over urban-like roughness. *Boundary-Layer Met.* **104**,
1275 229–259.
- 1276 CHENG, X.Q., WONG, C.W., HUSSAIN, F., SCHRÖDER, W. & ZHOU, Y. 2021 Flat plate drag reduction using
1277 plasma-generated streamwise vortices. *J. Fluid Mech.* **918**.
- 1278 CHOI, K.S. 2002 Near-wall structure of turbulent boundary layer with spanwise-wall oscillation. *Phys. Fluids*
1279 **14** (7), 2530–2542.
- 1280 CHUNG, D., HUTCHINS, N., SCHULTZ, M.P. & FLACK, K.A. 2021 Predicting the drag of rough surfaces. *Annu.*
1281 *Rev. Fluid Mech.* **53**, 439–471.
- 1282 CLAUSER, F.H. 1954 Turbulent boundary layers in adverse pressure gradients. *J. Aeronaut. Sci.* **21** (2),
1283 91–108.
- 1284 VON DEYN, L.H., GATTI, D. & FROHNAPFEL, B. 2022 From drag-reducing riblets to drag-increasing ridges.
1285 *J. Fluid Mech.* **951**, A16.
- 1286 EL-SAMNI, O.A., CHUN, H.H. & YOON, H.S. 2007 Drag reduction of turbulent flow over thin rectangular
1287 riblets. *Intl. J. Eng. Sci.* **45** (2–8), 436–454.
- 1288 ENDRIKAT, S., MODESTI, D., GARCÍA-MAYORAL, R., HUTCHINS, N. & CHUNG, D. 2021a Influence of riblet
1289 shapes on the occurrence of Kelvin–Helmholtz rollers. *J. Fluid Mech.* **913**, A37.
- 1290 ENDRIKAT, S., MODESTI, D., MACDONALD, M., GARCÍA-MAYORAL, R., HUTCHINS, N. & CHUNG, D. 2021b
1291 Direct numerical simulations of turbulent flow over various riblet shapes in minimal-span channels.
1292 *Flow Turbul. Combust.* **107** (1), 1–29.

- 1293 ESTEBAN, L.B., RODRÍGUEZ-LÓPEZ, E., FERREIRA, M.A. & GANAPATHISUBRAMANI, B. 2022 Mean flow of
1294 turbulent boundary layers over porous substrates. *Phys. Rev. Fluid* **7** (9), 094603.
- 1295 FAIRHALL, C.T., ABDERRAHAMAN-ELENA, N. & GARCÍA-MAYORAL, R. 2019 The effect of slip and surface
1296 texture on turbulence over superhydrophobic surfaces. *J. Fluid Mech.* **861**, 88–118.
- 1297 FLACK, K.A. & SCHULTZ, M.P. 2010 Review of hydraulic roughness scales in the fully rough regime. *ASME*
1298 *J. Fluids Eng.* **132** (4), 041203.
- 1299 FLACK, K.A., SCHULTZ, M.P. & BARROS, J.M. 2020 Skin friction measurements of systematically-varied
1300 roughness: Probing the role of roughness amplitude and skewness. *Flow Turbul. Combust.* **104** (2-3),
1301 317–329.
- 1302 FLORES, O. & JIMÉNEZ, J. 2006 Effect of wall-boundary disturbances on turbulent channel flows. *J. Fluid*
1303 *Mech.* **566**, 357–376.
- 1304 FOROOGHI, P., STROH, A., MAGAGNATO, F., JAKIRLIĆ, S. & B., FROHNAPFEL 2017 Toward a universal roughness
1305 correlation. *ASME. J. Fluids Eng.* **139** (12), 121201.
- 1306 FU, M.K., ARENAS, I., LEONARDI, S. & HULTMARK, M. 2017 Liquid-infused surfaces as a passive method
1307 of turbulent drag reduction. *J. Fluid Mech.* **824**, 688–700.
- 1308 GARCIA-MAYORAL, R. & JIMÉNEZ, J. 2011 Drag reduction by riblets. *Philos. Trans. Royal Soc. A* **369** (1940),
1309 1412–1427.
- 1310 GARCIA-MAYORAL, R. & JIMENEZ, J. 2011 Hydrodynamic stability and breakdown of the viscous regime
1311 over riblets. *J. Fluid Mech.* **678**, 317–347.
- 1312 GATTI, D., VON DEYN, L., FOROOGHI, P. & FROHNAPFEL, B. 2020 Do riblets exhibit fully rough behaviour?
1313 *Exp. Fluids* **61** (3), 81.
- 1314 GÓMEZ-DE-SEGURA, G. & GARCÍA-MAYORAL, R. 2019 Turbulent drag reduction by anisotropic permeable
1315 substrates—analysis and direct numerical simulations. *J. Fluid Mech.* **875**, 124–172.
- 1316 GÓMEZ-DE-SEGURA, G., SHARMA, A. & GARCÍA-MAYORAL, R. 2018a Turbulent drag reduction using
1317 anisotropic permeable substrates. *Flow Turbul. Combust.* **100** (4), 995–1014.
- 1318 GÓMEZ-DE-SEGURA, G., SHARMA, A. & GARCÍA-MAYORAL, R. 2018b Virtual origins in turbulent flows over
1319 complex surfaces. In *Center for Turbulence Research Proceedings of the Summer Program 2018* (ed.
1320 Moin, P. & Urzay, J.), vol. 3, pp. 277–286. Stanford University.
- 1321 HAMA, F.R. 1954 Boundary layer characteristics for smooth and rough surfaces. *Trans. Soc. Nav. Archit.*
1322 *Mar. Engrs* **62**, 333–358.
- 1323 HAO, Z. & GARCÍA-MAYORAL, R. 2024 Turbulent flows over porous and rough substrates, arXiv: 2402.15244.
- 1324 IBRAHIM, J.I., GÓMEZ-DE-SEGURA, G., CHUNG, D. & GARCÍA-MAYORAL, R. 2021 The smooth-wall-like
1325 behaviour of turbulence over drag-altering surfaces: a unifying virtual-origin framework. *J. Fluid*
1326 *Mech.* **915**, A56.
- 1327 JEONG, J., HUSSAIN, F., SCHOPPA, W. & KIM, J. 1997 Coherent structures near the wall in a turbulent channel
1328 flow. *J. Fluid Mech.* **332**, 185–214.
- 1329 JIMÉNEZ, J. 1994 On the structure and control of near wall turbulence. *Phys. Fluids* **6** (2), 944–953.
- 1330 JIMÉNEZ, J. 2004 Turbulent flows over rough walls. *Annu. Rev. Fluid Mech.* **36**, 173–196.
- 1331 JIMÉNEZ, J. & PINELLI, A. 1999 The autonomous cycle of near-wall turbulence. *J. Fluid Mech.* **389**, 335–359.
- 1332 JIMÉNEZ, J., UHLMANN, M., PINELLI, A. & KAWAHARA, G. 2001 Turbulent shear flow over active and passive
1333 porous surfaces. *J. Fluid Mech.* **442**, 89–117.
- 1334 JIMÉNEZ BOLAÑOS, S. & VERNESCU, B. 2017 Derivation of the Navier slip and slip length for viscous flows
1335 over a rough boundary. *Phys. of Fluids* **29** (5), 057103.
- 1336 JOUYBARI, M.A., YUAN, J., BRERETON, G.J. & MURILLO, M.S. 2021 Data-driven prediction of the equivalent
1337 sand-grain height in rough-wall turbulent flows. *J. Fluid Mech.* **912**, A8.
- 1338 KANG, S. & CHOI, H. 2000 Active wall motions for skin-friction drag reduction. *Phys. Fluids* **12** (12),
1339 3301–3304.
- 1340 KHORASANI, S.M.H., LUHAR, M. & BAGHERI, S. 2024 Turbulent flows over porous lattices: alteration of
1341 near-wall turbulence and pore-flow amplitude modulation. *J. Fluid Mech.* **984**, A63.
- 1342 KHORASANI, S.M.H., LĂCIS, U., PASCHE, S., ROSTI, M.E. & BAGHERI, S. 2022 Near-wall turbulence alteration
1343 with the transpiration-resistance model. *J. Fluid Mech.* **942**, A45.
- 1344 KIM, J., MOIN, P. & R., MOSER 1987 Turbulence statistics in fully developed channel flow at low reynolds
1345 number. *J. Fluid Mech.* **177**, 133–166.
- 1346 KUWATA, Y. & SUGA, K. 2017 Direct numerical simulation of turbulence over anisotropic porous media. *J.*
1347 *Fluid Mech.* **831**, 41–71.
- 1348 LĂCIS, U., SUDHAKAR, Y., PASCHE, S. & BAGHERI, S. 2020 Transfer of mass and momentum at rough and
1349 porous surfaces. *J. Fluid Mech.* **884**, A21.

- 1350 LĀCIS, U., ZAMPOGNA, G.A. & BAGHERI, S. 2017 A computational continuum model of poroelastic beds.
1351 *Proc. R. Soc. A* **473**, 20160932.
- 1352 LASSEUX, D., VALDÉS-PARADA, F.J. & BELLET, F. 2019 Macroscopic model for unsteady flow in porous
1353 media. *J. Fluid Mech.* **862**, 283–311.
- 1354 LEE, S., YANG, J., FOROOGHI, P., STROH, A. & BAGHERI, S. 2022 Predicting drag on rough surfaces by transfer
1355 learning of empirical correlations. *J. Fluid Mech.* **933**, A18.
- 1356 VAN LEER, B. & NISHIKAWA, H. 2021 Towards the ultimate understanding of MUSCL: Pitfalls in achieving
1357 third-order accuracy. *J. Comput. Phys.* **446**, 110640.
- 1358 LEONARDI, S., ORLANDI, P., SMALLEY, R.J., DJENIDI, L. & ANTONIA, R.A. 2003 Direct numerical simulations
1359 of turbulent channel flow with transverse square bars on one wall. *J. Fluid Mech.* **491**, 229–238.
- 1360 LUCHINI, P. 1996 Reducing the turbulent skin friction. In *Computational Methods in Applied Sciences '96*
1361 (ed. J.A. Désidéri et al.), pp. 466–470.
- 1362 LUCHINI, P. 2015 The relevance of longitudinal and transverse protrusion heights for drag reduction by
1363 a superhydrophobic surface. In *European Drag Reduction and Flow Control Meeting – EDRFCM*
1364 *2015 March 23–26, 2015, Cambridge, UK*, pp. 81–82.
- 1365 LUCHINI, P., MANZO, F. & POZZI, A. 1991 Resistance of a grooved surface to parallel flow and cross-flow. *J.*
1366 *Fluid Mech.* **228**, 87–109.
- 1367 MANES, C., POGGI, D. & RIDOLFI, L. 2011 Turbulent boundary layers over permeable walls: scaling and
1368 near-wall structure. *J. Fluid Mech.* **687**, 141–170.
- 1369 MANSOUR, N.N., KIM, J. & MOIN, P. 1988 Reynolds-stress and dissipation-rate budgets in a turbulent channel
1370 flow. *J. Fluid Mech.* **194**, 15–44.
- 1371 MEI, C.C. & VERNESCU, B. 2010 *Homogenization Methods for Multiscale Mechanics*. World Sci.
- 1372 MONTI, A., NICHOLAS, S., OMDYEGANEH, M., PINELLI, A. & ROSTI, M.E. 2022 On the solidity parameter in
1373 canopy flows. *J. Fluid Mech.* **945**, A17.
- 1374 MORIMOTO, M., AOKI, R., KUWATA, Y. & SUGA, K. 2024 Measurements for characteristics of turbulence
1375 over a streamwise preferential porous substrate. *Flow Turbul. Combust.* **113** (1), 71–92.
- 1376 NAQVI, S.B. & BOTTARO, A. 2021 Interfacial conditions between a free-fluid region and a porous medium.
1377 *Int. J. Multiph. Flow* **141**, 103585.
- 1378 NAVIER, C. 1823 Mémoire sur les lois du mouvement des fluides. *Mém. Acad. R. Sci. Inst. France* **6**, 389–440.
- 1379 NIKURADSE, J. 1933 Laws of flow in rough pipes. *Tech. Memo.* 1292 .
- 1380 ORLANDI, P. & LEONARDI, S. 2006 DNS of turbulent channel flows with two- and three-dimensional
1381 roughness. *J. Turbul.* **7**, N73.
- 1382 ORLANDI, P. & LEONARDI, S. 2008 Direct numerical simulation of three-dimensional turbulent rough
1383 channels: parameterization and flow physics. *J. Fluid Mech.* **606**, 399–415.
- 1384 ORLANDI, P., LEONARDI, S. & ANTONIA, R.A. 2006 Turbulent channel flow with either transverse or
1385 longitudinal roughness elements on one wall. *J. Fluid Mech.* **561**, 279–305.
- 1386 ORLANDI, P., LEONARDI, S., TUZI, R. & ANTONIA, R.A. 2003 Direct numerical simulation of turbulent
1387 channel flow with wall velocity disturbances. *Phys. Fluids* **15** (12), 3587–3601.
- 1388 PARK, H., PARK, H. & KIM, J. 2013 A numerical study of the effects of superhydrophobic surface on
1389 skin-friction drag in turbulent channel flow. *Phys. Fluids* **25** (11), 110815.
- 1390 RASTEGARI, A. & AKHAVAN, R. 2015 On the mechanism of turbulent drag reduction with super-hydrophobic
1391 surfaces. *J. Fluid Mech.* **773**.
- 1392 ROSTI, M.E., BRANDT, L. & PINELLI, A. 2018 Turbulent channel flow over an anisotropic porous wall—drag
1393 increase and reduction. *J. Fluid Mech.* **842**, 381–394.
- 1394 ROSTI, M.E., CORTELEZZI, L. & QUADRIO, M. 2015 Direct numerical simulation of turbulent channel flow
1395 over porous walls. *J. Fluid Mech.* **784**, 396–442.
- 1396 SAFFMAN, P.G. 1971 On the boundary condition at the surface of a porous medium. *Studies in Applied*
1397 *Mathematics* **50**, 93–101.
- 1398 SCHLICHTING, H. 1937 Experimental investigation of the problem of surface roughness. *Tech. Memo.* 823,
1399 *Natl. Adv. Comm. Aeronaut., Washington, DC* .
- 1400 SHARMA, A. & GARCÍA-MAYORAL, R. 2020 Turbulent flows over dense filament canopies. *J. Fluid Mech.*
1401 **888**, A2.
- 1402 SHI, Z., KHORASANI, S.M.H., SHIN, H., YANG, J., LEE, S. & BAGHERI, S. 2024 Drag prediction of rough-wall
1403 turbulent flow using data-driven regression, arXiv: 2405.09256.
- 1404 SUDHAKAR, Y., LĀCIS, U., PASCHE, S. & BAGHERI, S. 2021 Higher-order homogenized boundary conditions
1405 for flows over rough and porous surfaces. *Transp. Porous Med.* **136** (1), 1–42.

- 1406 SUGA, K. 2016 Understanding and modelling turbulence over and inside porous media. *Flow Turbul.*
1407 *Combust.* **96** (3), 717–756.
- 1408 SUGA, K., OKAZAKI, Y., HO, U. & KUWATA, Y. 2018 Anisotropic wall permeability effects on turbulent
1409 channel flows. *J. Fluid Mech.* **855**, 983–1016.
- 1410 SUGA, K., TOMINAGA, S., MORI, M. & KANEDA, M. 2013 Turbulence characteristics in flows over solid and
1411 porous square ribs mounted on porous walls. *Flow Turbul. Combust.* **91** (1), 19–40.
- 1412 TOWNSEND, A.A. 1976 *The Structure of Turbulent Shear Flow*, 2nd edn.. Cambridge University Press.
- 1413 VENKATKRISHNAN, V. 1993 On the accuracy of limiters and convergence to steady state solutions. In *the*
1414 *31st Aerospace Sci. Meet.*, Reno, Nevada, USA. (doi: 10.2514/6.1993-880).
- 1415 VIJAY, S. & LUHAR, M. 2024 Pressure drop measurements over anisotropic porous substrates in channel
1416 flow. *Exp. Fluids* **65**, 135.
- 1417 VREMAN, A.W. & KUERTEN, J.G.M. 2014 Comparison of direct numerical simulation databases of turbulent
1418 channel flow at $Re_\tau = 180$. *Phys. Fluids* **26** (1), 015102.
- 1419 WALLACE, J.M., ECKELMANN, H. & BRODKEY, R.S. 1972 The wall region in turbulent shear flow. *J. Fluid*
1420 *Mech.* **54** (1), 39–48.
- 1421 WALSH, M. & LINDEMANN, A. 1984 Optimization and application of riblets for turbulent drag reduction. In
1422 *the 22nd Aerosp. Sci. Meet.*, Reno, NV, USA. (doi: 10.2514/6.1984-347).
- 1423 WANG, W., CHU, X., LOZANO-DURÁN, A., HELMIG, R. & WEIGAND, B. 2021 Information transfer between
1424 turbulent boundary layers and porous media. *J. Fluid Mech.* **920**, A21.
- 1425 WANG, W., LOZANO-DURÁN, A., HELMIG, R. & CHU, X. 2022 Spatial and spectral characteristics of
1426 information flux between turbulent boundary layers and porous media. *J. Fluid Mech.* **949**, A16.
- 1427 WEST, A. & CARAENI, M. 2015 Jet noise prediction using a permeable FW-H solver. In *the 21st AIAA/CEAS*
1428 *Aeroacoust. Conf.*, Dallas, TX, USA, p. 2371. (doi: 10.2514/6.2015-2371).
- 1429 WISE, D.J. & RICCO, P. 2014 Turbulent drag reduction through oscillating discs. *J. Fluid Mech.* **746**, 536–564.
- 1430 WONG, J., CAMOBRECO, C.J., GARCÍA-MAYORAL, R., HUTCHINS, N. & D., CHUNG 2024 A viscous vortex
1431 model for predicting the drag reduction of riblet surfaces. *J. Fluid Mech.* **978**, A18.
- 1432 YANG, J., STROH, A., LEE, S., BAGHERI, S., FROHNAPFEL, B. & FOROOGHI, P. 2023 Prediction of equivalent
1433 sand-grain size and identification of drag-relevant scales of roughness – a data-driven approach. *J.*
1434 *Fluid Mech.* **975**, A34.
- 1435 YANG, J., STROH, A., LEE, S., BAGHERI, S., FROHNAPFEL, B. & FOROOGHI, P. 2024 Assessment of roughness
1436 characterization methods for data-driven predictions. *Flow Turbul. Combust.* **113** (2), 275–292.
- 1437 YANG, X.I.A. & MENEVEAU, C. 2016 Large eddy simulations and parameterisation of roughness element
1438 orientation and flow direction effects in rough wall boundary layers. *J. Turbul.* **17** (11), 1072–1085.
- 1439 YANG, X.I.A., SADIQUE, J., MITTAL, R. & MENEVEAU, C. 2016 Exponential roughness layer and analytical
1440 model for turbulent boundary layer flow over rectangular-prism roughness elements. *J. Fluid Mech.*
1441 **789**, 127–165.
- 1442 ZAMPOGNA, G.A., MAGNAUDET, J. & BOTTARO, A. 2019a Generalized slip condition over rough surfaces. *J.*
1443 *Fluid Mech.* **858**, 407–436.
- 1444 ZAMPOGNA, G., NAQVI, S.B., MAGNAUDET, J. & BOTTARO, A. 2019b Compliant riblets: Problem formulation
1445 and effective macrostructural properties. *Journal of Fluids and Structures* **91**, 102708.