



UNIVERSITÀ DEGLI
STUDI DI GENOVA



Numerical simulation of a droplet icing on a cold surface

Buccini Saverio

Peccianti Francesco

Supervisors:

Prof. Alessandro Bottaro

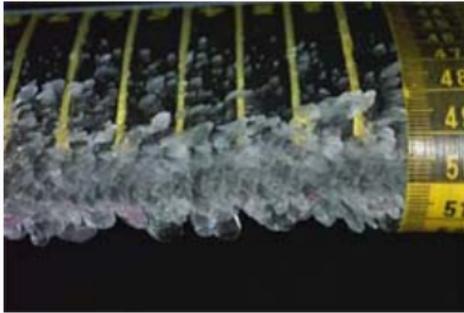
Prof. Dominique Legendre

March 30, 2017

Università degli Studi di Genova

1. Introduction
2. Physical model and experiments
3. Numerical method
4. 1D problem and validation
5. Simulations of the droplet
6. Conclusions

Introduction



Effects

- Lift variation → stall
- Increased drag
- Instrumentation problems → AF447
- Increased weight

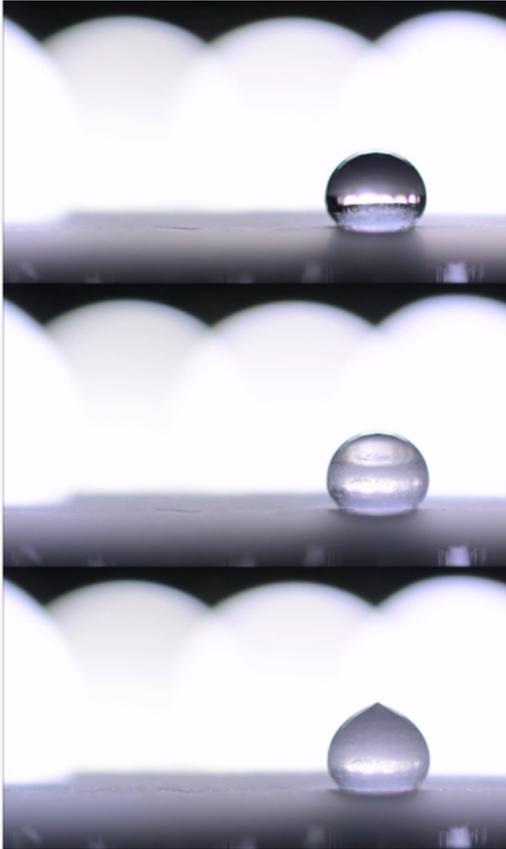
Countermeasures

- De-icing & anti-icing fluids
- De-icing boots
- Electrical resistances
- Hot air bleeding from engines



Physical model and experiments

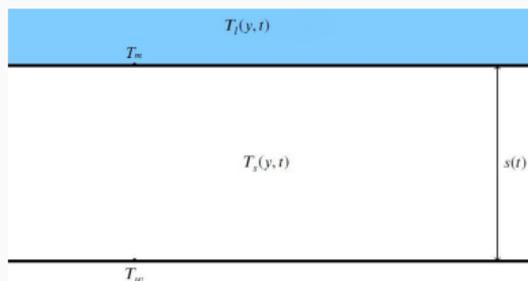
Freezing droplet



Aim of the work

- Freezing front evolution
- Final shape of the droplet and its causes
 1. Density variation
 2. Marangoni effect

Stefan problem (1)



- solid phase: $0 \leq x < s(t)$

$$\frac{\partial T_s}{\partial t} = \alpha_s \frac{\partial^2 T_s}{\partial x_s^2}$$

- liquid phase: $s(t) < x < \infty$

$$\frac{\partial T_l}{\partial t} = \alpha_l \frac{\partial^2 T_l}{\partial x_l^2}$$

Boundary conditions

- Constant temperatures $T(0, t) = T_w$ and $T(x \rightarrow \infty, t) = T_i$
- Interface condition at $x = s(t)$:

$$\begin{cases} -\lambda_l \frac{\partial T_l}{\partial x} \Big|_{s^+} + \lambda_s \frac{\partial T_s}{\partial x} \Big|_{s^-} = \rho_s L \frac{ds}{dt} \\ T_s \Big|_{s^-} = T_l \Big|_{s^+} = T_m \end{cases}$$

Stefan problem (2)

Assumptions

- Heat transfer is driven by the sole conduction
- Thermophysical properties constant with temperature in each phase
- Phase change temperature fixed and known
- The entire domain initially at $T(x, 0) = T_i$

Analytical solution

$$s = 2\delta\sqrt{\alpha_s t}$$

$$T_s(x, t) = T_{wall} + \frac{(T_m - T_{wall})}{\operatorname{erf}(\delta)} \operatorname{erf}\left(\frac{x}{2\sqrt{\alpha_s t}}\right)$$

$$T_l(x, t) = T_i - \frac{(T_i - T_m)}{\operatorname{erfc}(\delta\alpha)} \operatorname{erfc}\left(\frac{x}{2\sqrt{\alpha_l t}}\right)$$

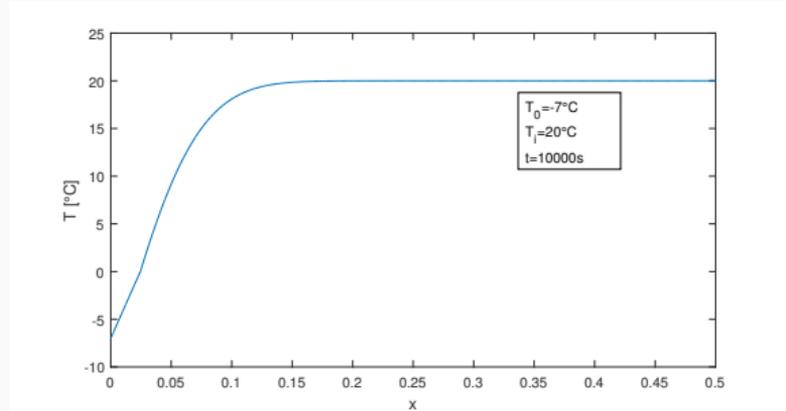
Stefan problem (3)

Adimensional parameters

$$Ste = \frac{\rho_s c_{p,s} (T_m - T_{wall})}{\rho_s L}$$

$$\phi = \frac{\rho_l c_{p,l} (T_i - T_m)}{\rho_s c_{p,s} (T_m - T_{wall})}$$

$$\alpha = \sqrt{\frac{\alpha_s}{\alpha_l}}$$



Equation for δ

$$\frac{e^{\delta^2}}{\text{erf}(\delta)} - \frac{e^{-\delta^2 \alpha^2}}{\text{erfc}(\delta \alpha)} \frac{\phi}{\alpha} = \frac{\delta \sqrt{\pi}}{Ste}$$

Continuity

$$\rho_{liq} V_{liq} + \rho_{sol} V_{sol} = const \quad \rightarrow \quad v_{liq} = \frac{dH}{dt} = \frac{ds}{dt} \cdot \underbrace{\left(1 - \frac{\rho_{sol}}{\rho_{liq}}\right)}_r$$

Governing equation $\frac{\partial T_l}{\partial t} + v_{liq} \frac{\partial T_l}{\partial y} = \alpha_l \frac{\partial^2 T_l}{\partial x_l^2}$

Being the parameter r the indicator of the expansion:

$$T_l = T_0 + (T_m - T_0) \frac{\operatorname{erfc} \left[\alpha \delta \left(\frac{x}{2\delta\sqrt{\alpha_s t}} - r \right) \right]}{\operatorname{erfc} [\alpha \delta (1 - r)]}$$

$$\frac{e^{-\delta^2}}{\operatorname{erf}(\delta)} - \frac{\phi}{\alpha} \frac{e^{-(\alpha\delta)^2}}{\operatorname{erfc}[\alpha\delta(1-r)]} \frac{e^{2r(\alpha\delta)^2}}{e^{(r\alpha\delta)^2}} = \frac{\delta\sqrt{\pi}}{Ste}$$

Numerical method

Jadim is a research code developed by J. Magnaudet and D. Legendre's team in the Interface group at *Institut de Mécaniques des Fluides de Toulouse*. The code permits to describe in an accurate way physical mechanisms present in multiphasic flows.

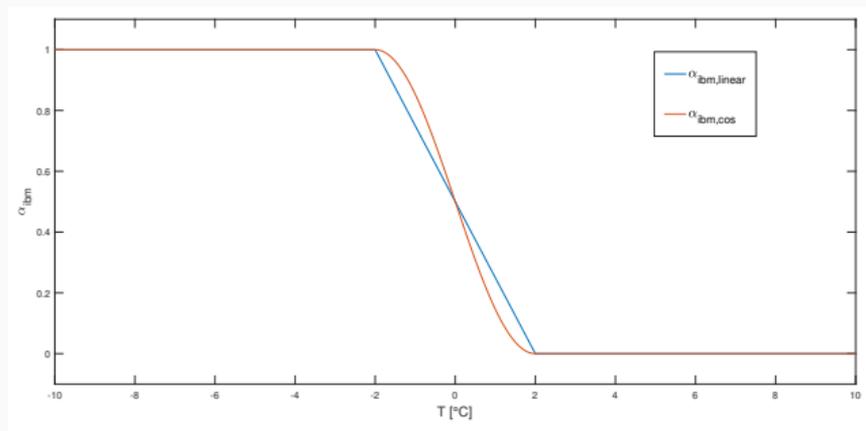
- Volume of Fluid formulation is employed
- Thermal and Immersed Boundary Method routine are supported

In the present work the objective is to couple the three of them and, in particular, to develop a thermal based IBM formulation

Solid function fraction

A solid function fraction has been defined as follows, representing the amount of ice for each cell:

$$\alpha_{ibm,lin} = \tau \cdot \frac{T_{max} - T}{T_{max} - T_{min}}$$
$$\alpha_{ibm,cos} = 0.5 \cdot \tau \cdot \left[\cos \frac{\pi \cdot (T - T_{min})}{T_{max} - T_{min}} + 1 \right]$$



$$\phi = (1 - \tau) \phi_{air} + \tau [(1 - \alpha_{ibm}) \phi_{liq} + \alpha_{ibm} \phi_{sol}]$$

Velocity calculation

$$\mathbf{v}_{liq} = \left(1 - \frac{\rho_{ice}}{\rho_{water}}\right) \mathbf{V}_{front}$$

Scalar transport equation:

$$\frac{\partial \alpha_{ibm}}{\partial t} + \mathbf{V}_{front} \cdot \nabla \alpha_{ibm} = 0$$

$$\mathbf{V}_{front} \cdot \mathbf{n} = \frac{-\frac{\partial \alpha_{ibm}}{\partial T} \frac{\partial T}{\partial t}}{\|\nabla \alpha_{ibm}\|}$$

$$n_i = \frac{\frac{\partial \alpha_{ibm}}{\partial x_i}}{\|\nabla \alpha_{ibm}\|}$$

Velocity imposition

$$\mathbf{f} = \alpha_{ibm} \frac{\mathbf{U} - \mathbf{U}^*}{\Delta t}$$

$$\begin{cases} U = 0 & \alpha_{ibm} \geq 0.95 \\ U = \mathbf{v}_{liq} & 0 < \alpha_{ibm} < 0.95 \end{cases}$$

Being \mathbf{U}^* a predictor velocity without considering the immersed object

Pressure correction

Jadim's SIMPLE algorithm is modified in order to take account of the calculated velocities

$$\begin{cases} H = c_{p,l}T & \text{Liquid} \\ H = c_{p,s}T + L & \text{Solid} \end{cases}$$

$$\frac{\partial \rho H}{\partial t} = \nabla \cdot (k \nabla T)$$

The source term method

$$\rho c_p \frac{\partial T}{\partial t} = \frac{\partial}{\partial x} \left(k \frac{\partial T}{\partial x} \right) - S$$

$$S = \frac{\partial \alpha_{IBM}}{\partial T} \frac{\partial T}{\partial t} \frac{[L + T(c_{p,s} - c_{p,l})]}{c_p}$$

The apparent heat capacity method

$$c_{app} = \frac{dH}{dT}$$

$$c_{app} = c_p + L \frac{d\alpha_{IBM}}{dT}$$

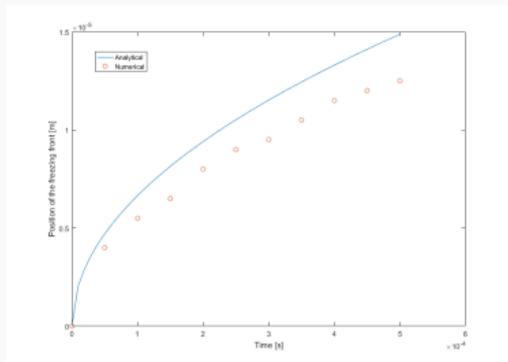
$$\rho c_{app} \frac{\partial T}{\partial t} = \nabla \cdot (k \nabla T)$$

1D problem and validation

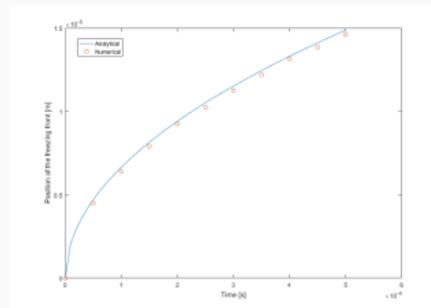
	$err_{T,max}$	$err_{T,avg}$	$err_{int,max}$	$err_{int,avg}$
Linear $[-2, 2]$	6.1%	5.7%	27%	17%
Linear $[-1, 1]$	4.3%	4.1%	14.2%	9.2%
Linear $[0, 1]$	5.2%	4.2%	4.7%	2.2%
Linear $[0, 0.1]$	2.8%	2%	3.5%	1%
Cosine $[-1, 1]$	5.2%	4.3%	12.2%	7.6%
Cosine $[0, 1]$	5.3%	4.1%	4.8%	2.3%

- For narrower solidification ranges, the results are more accurate
- The solidification front is well located if the inferior limit coincides to 0°C

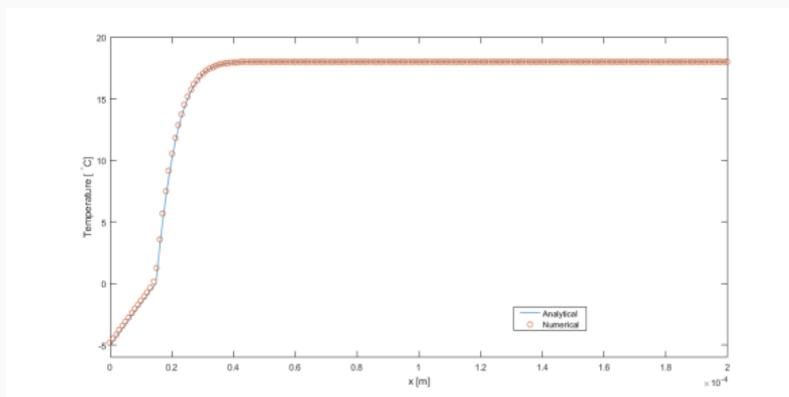
IBM functions, figures



Freezing front, cos $[-1, 1]$

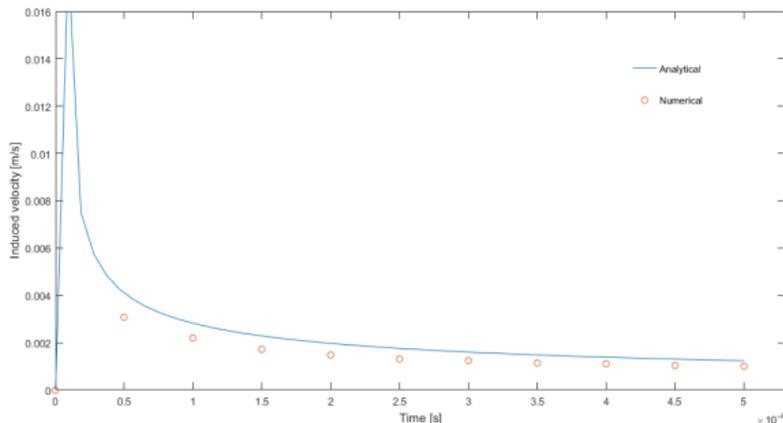


Freezing front, lin $[0, 0.1]$



	$err_{vel,max}$	$err_{vel,avg}$
Lin $[-1, 1]$	16.5%	8.1%
Lin $[0, 1]$	23.6%	8.7%
Lin $[0, 0.1]$	100%	53.8%
Cos $[-1, 1]$	13.7%	7%
Cos $[0, 1]$	23.6%	8.9%

- Velocity is generally underestimated
- The chosen range has to be wide enough to properly calculate the velocity



Grid convergence

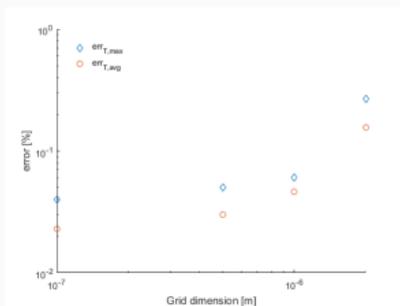


Figure 1: Temperature, $\cos[-1, 1]$

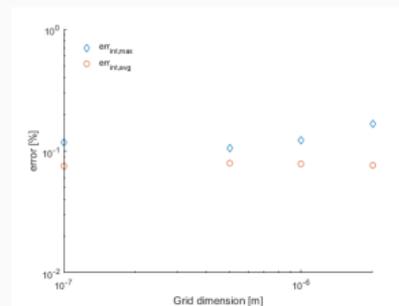


Figure 3: Interface position, $\cos[-1, 1]$

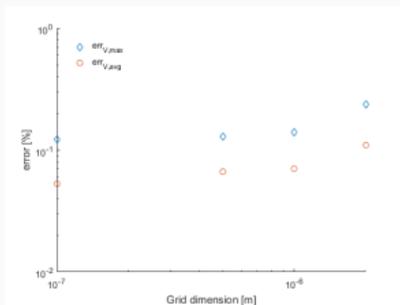


Figure 2: Velocity, $\cos[-1, 1]$

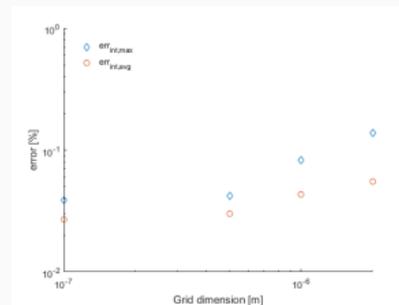


Figure 4: Interface position, $\text{lin}[0, 1]$

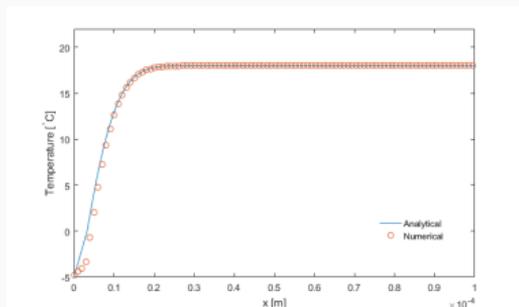


Figure 5: Apparent capacity method

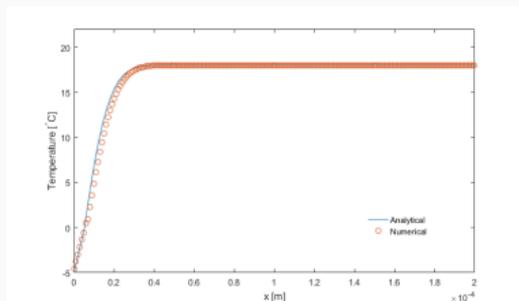
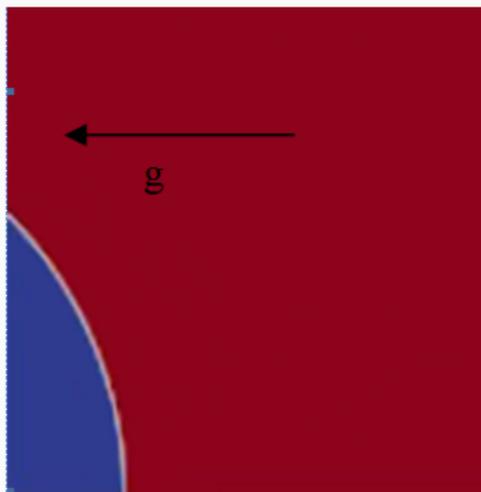


Figure 6: Source term method

- Average errors are comparable:
 $\sim 20\%$
- Source term method tends to become more accurate through time
- Apparent heat capacity worsens with time due to underestimation of the latent heat
- Source term method doesn't guarantee stability without additional loops

Simulations of the droplet

Parameters of the simulations



	$\alpha \left[\frac{m^2}{s} \right]$	$\rho \left[\frac{kg}{m^3} \right]$
Air	$2.166 \cdot 10^{-5}$	1.2
Water	$1.433 \cdot 10^{-7}$	1000
Ice	$1.176 \cdot 10^{-6}$	917

V	$1.35 \cdot 10^{-13} [m^3]$
R ₉₀	$4 \cdot 10^{-5} [m]$
dx	$10^{-6} [m]$
dt	$10^{-7} [s]$

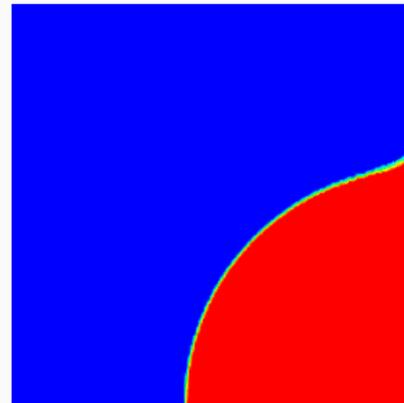
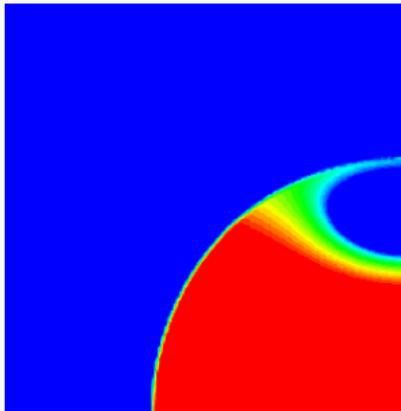
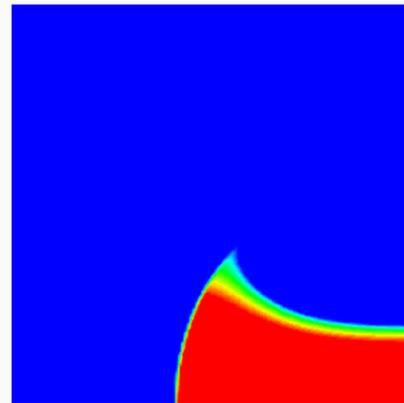
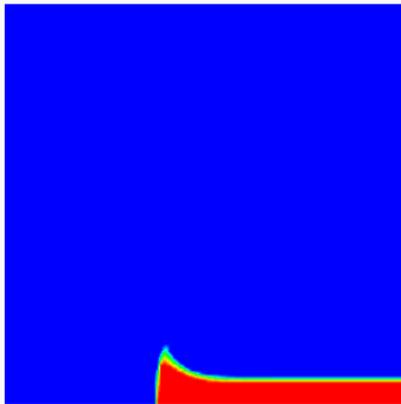
- West wall represents the cold plate and it is isothermal
- South is the symmetry axis
- North and east walls are adiabatic

$$T_i = 18^\circ C$$

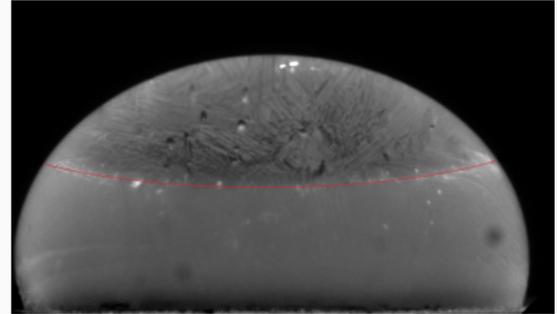
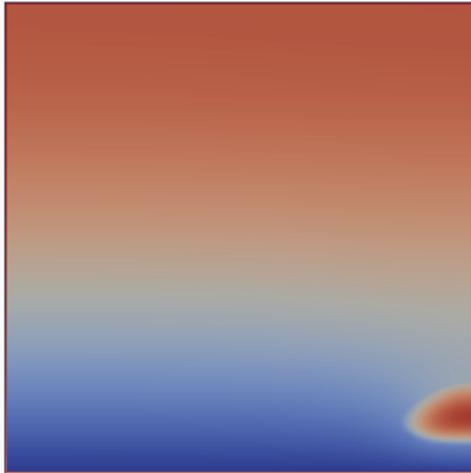
$$T_w = -5^\circ C$$

$$Bo = \frac{g \cdot \Delta\rho \cdot d^2}{\gamma} \ll 1$$

The solidification process (1)

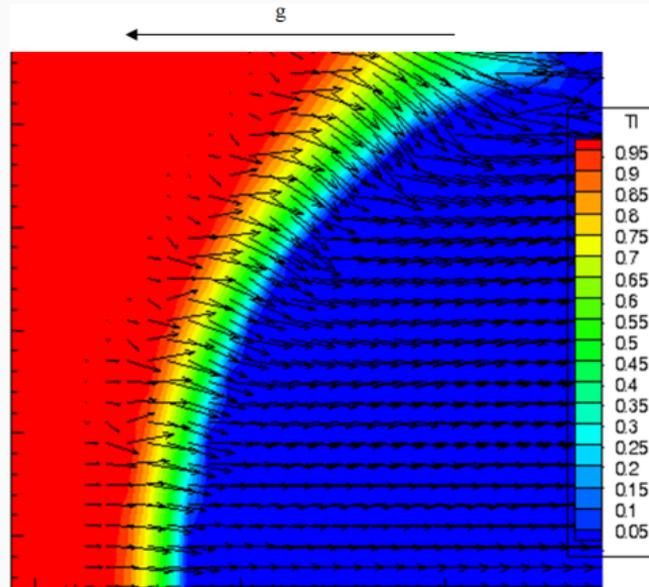


The solidification process (2)



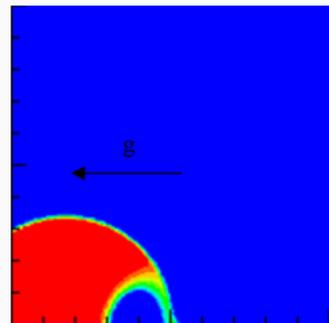
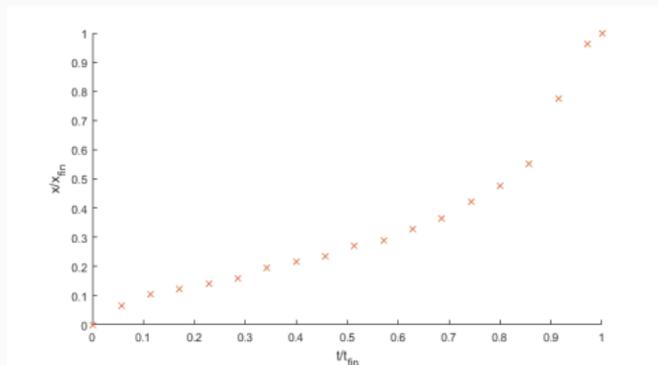
- Higher thermal diffusivity of the air causes the droplet outer layer to solidify
- Thermally treated as a mixture between ice and water
- Dynamically considered as liquid

Velocity field



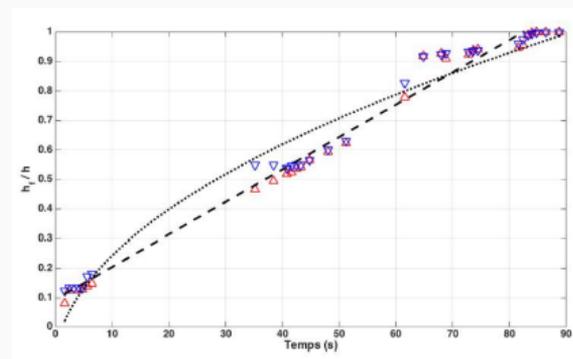
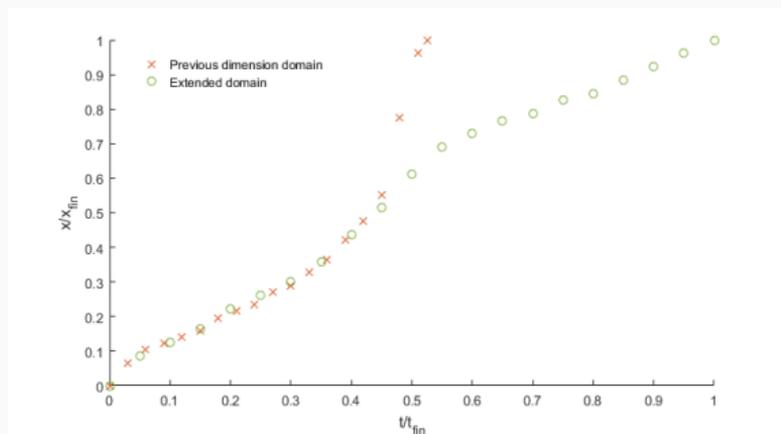
- Inside the solid velocity is zero
- Composition of V_x and V_y returns a vector perpendicular to the interface
- Velocity field in the water comes from the combination of incompressibility and the axis of symmetry

Evolution of the freezing front (1)



- Quasi-linear trend till the outer layer of ice is thin
- Acceleration due to the increased thermal diffusivity

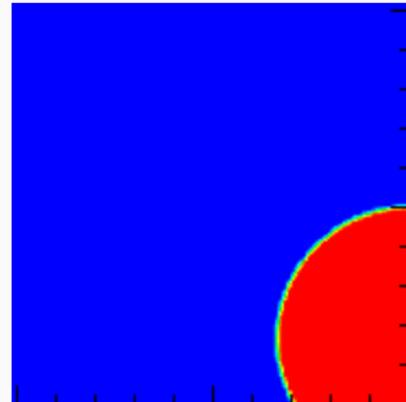
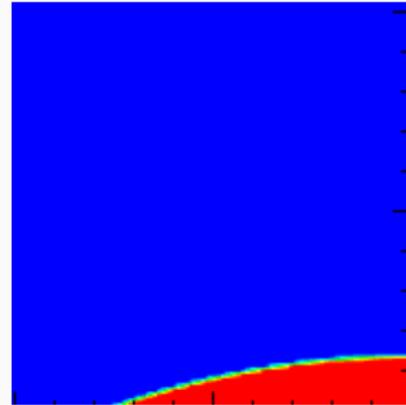
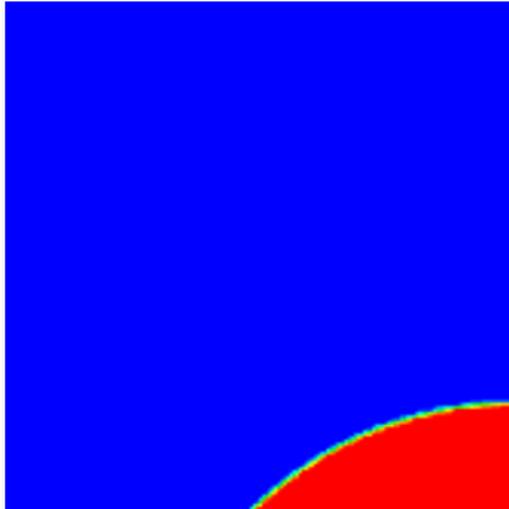
Evolution of the freezing front (2)



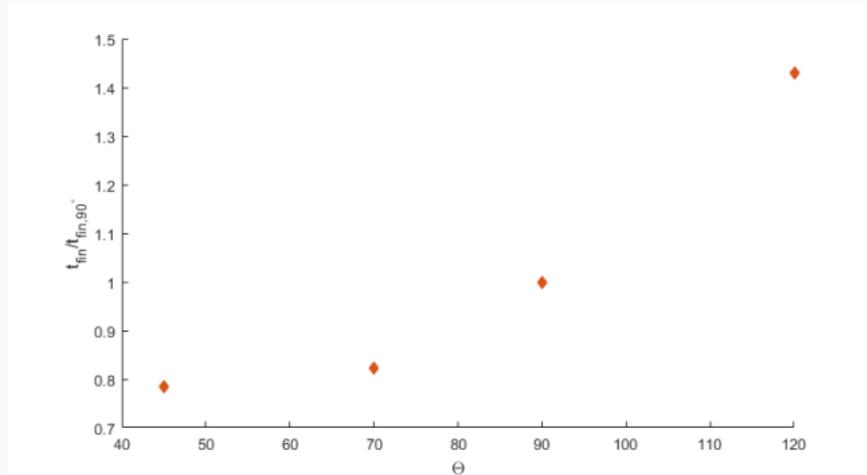
- Experimentally the trend seems to be linear differently from the Stefan problem
- An expanded domain guarantees a more accurate result, minimum size depends on the contact angle
- Numerical results confirm the global linear behaviour

Contact angle influence (1)

- Wall temperature
- Initial temperature
- Droplet's volume
- Mesh size

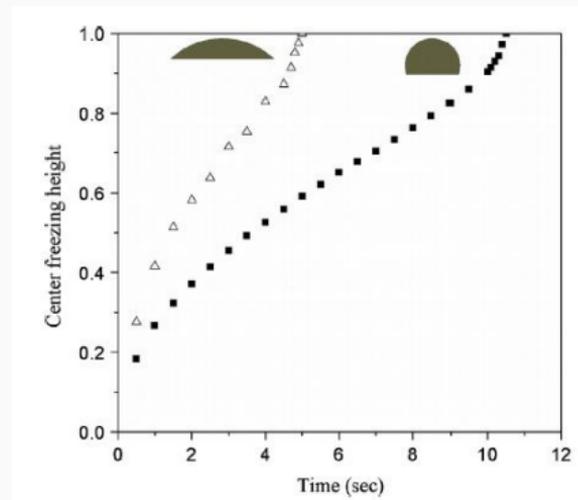
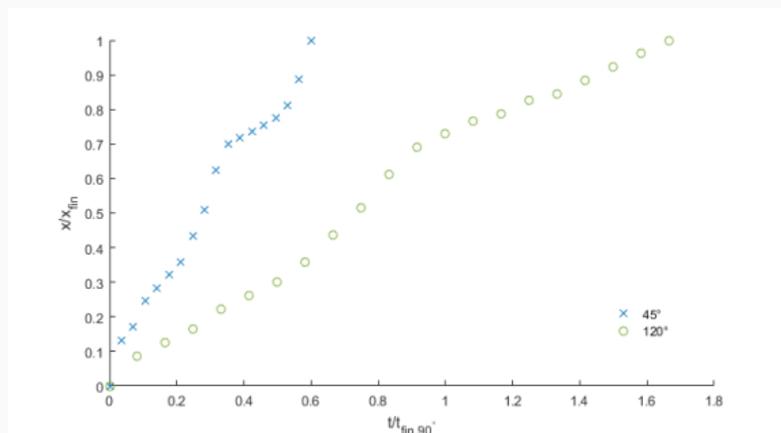


Contact angle influence (2)



- Hydrophobic surfaces tends to delay the ice accretion, commonly employed as constructive materials or coatings
- We observed no formation of the protrusion in correspondence of a threshold of about $\Theta \simeq 30^\circ$

Contact angle influence (3)

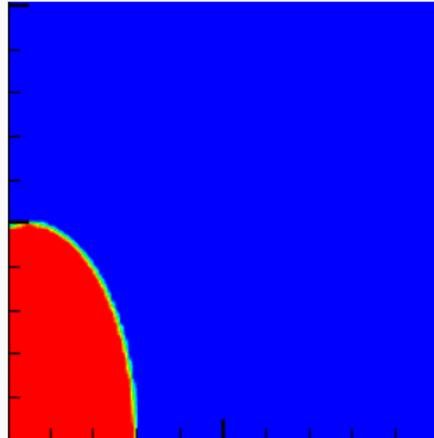


- Results similar to other numerical works
- Quasi-linear behaviour independent from the contact angle, the difference is the total solidification time

Elliptical droplet (1)

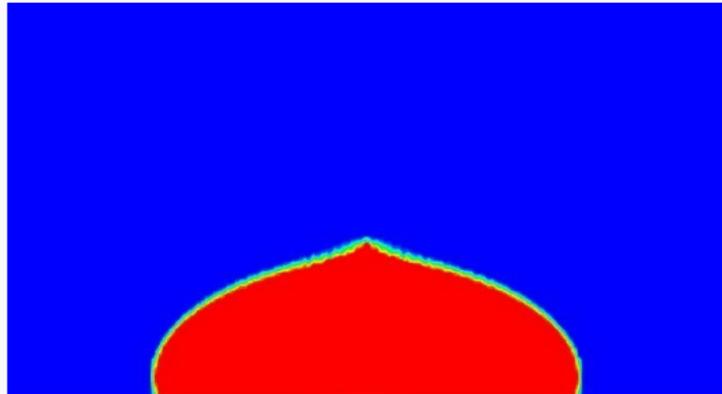
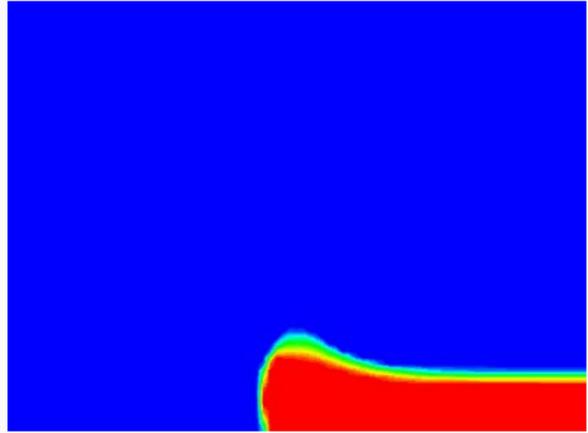
It is not a physical case \Rightarrow the droplet's volume and consequentially Bond number are too small to cause an elliptical shape

A qualitative study to investigate if new dynamics appear



Elliptical droplet (2)

- The freezing front shape resemble the spheric cap case and the experimental results
- The pointy protrusion continues to appear



Conclusions

Conclusions

- Successfully coupled VoF, thermics and IBM
- The characteristic pointy tip has been reproduced
- Evolution of the freezing front confirms experimental results over analytical ones
- Parametric study of the contact angle influence

Future developments

- Ameliorate the computation of the latent heat of solidification
- Tracking the freezing front for a better calculation of the velocity
- Experimentally confirm the influence of the contact angle

Thank you for your attention
